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# **REAERATION OF STREAMS AND RESERVOIRS ANALYSIS AND BIBLIOGRAPHY**

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Engineering and Research Center  
Bureau of Reclamation**

**December 1970**

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16. ABSTRACT  Bureau of Reclamation responsibility for maintaining or enhancing the water quality associated with its projects has resulted in a comprehensive program of research in water quality and pollution control. A literature search and state-of-the-art review to determine the need for future research in reaeration of streams and reservoirs revealed a large number of references concerning the application of aeration methods and equipment to waste treatment. Generally, the application of this technology to aeration of large volumes of water such as rivers and reservoirs remains to be developed, although several applicable references were found. Questions regarding atmospheric reaeration in streams remain unresolved. Research is also needed regarding the aeration capability of hydraulic structures and control devices, development of new methods and equipment, effects of dissolved air on cavitation, and comparative economics of various methods and equipment. Ecological effects of reaeration are being considered in a separate review.					
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ANALYSIS AND BIBLIOGRAPHY**

**by  
D. L. King**

**December 1970**

Hydraulics Branch  
Division of General Research  
Engineering and Research Center  
Denver, Colorado

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**UNITED STATES DEPARTMENT OF THE INTERIOR**

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**BUREAU OF RECLAMATION  
Ellis L. Armstrong  
Commissioner**

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## NOTATION

Dimensions of mathematical terms are given in general terms of mass-length-time (M-L-T). For example, concentrations are expressed in the form of  $M/L^3$ . This form corresponds to English system units of  $lb/ft^3$  or to Metric system units of  $mg/l$ . Similarly, the rate of mass transfer in general terms is expressed as  $M/L^2-T$ , corresponding to  $lb/ft^2-sec$  in English notation or  $g/m^2-sec$  in the Metric system.

## PURPOSE

The literature survey was conducted for the purpose of preparing a summary of the state-of-the-art for defining research needs in the field of reaeration of streams and reservoirs.

## CONCLUSIONS

The literature reflects a large amount of information on the waste treatment applications of reaeration. The use of diffusers and mechanical surface aerators is particularly well documented. Basic theories of mass transfer and bubble dynamics have also been widely investigated with emphasis on waste treatment.

Generally, the application of these theories and methods to large volumes of water such as rivers and reservoirs remains to be developed. Some work has been reported concerning the use of turbine injection, diffusers, and mechanical aerators for stream reaeration, and new devices such as the U-tube are being investigated; however, additional research is needed. The use of control devices, such as the Howell-Bunger valve, for reaeration, is in an early stage of investigation, and the reaeration capability of energy dissipators has had very little attention.

Reaeration of reservoirs has been primarily concerned with mixing by diffused air or pumping, with accompanying atmospheric reaeration at the water surface.

The effect of dissolved air on cavitation continues to be an area requiring further investigation.

Activity in mathematical simulation and prediction appears to be adequate. However, questions remain

concerning atmospheric reaeration in streams, particularly correlation with hydraulic parameters.

There is an apparent deficiency in the area of economic analysis and cost comparison of methods and devices for reaeration. The methods of defining efficiency need to be standardized.

These conclusions point to the difficulties facing designers of equipment for reaeration of streams and reservoirs. The research activity in this field has not been collected into a set of criteria for design purposes.

## APPLICATION

This report was prepared for the use of the Bureau of Reclamation in planning a program for research in reaeration. The bibliography provides references for use in the design and operation of reaeration equipment and for determining reaeration requirements.

## INTRODUCTION

The Bureau of Reclamation has responsibility for maintaining or enhancing the quality of water associated with its projects.

Because of this responsibility, the Bureau is engaged in a comprehensive program of research in water quality and pollution control. This program includes determination of methods and techniques for water-quality monitoring and control, studies of water-quality parameters in large and small impoundments, investigation of eutrophication problems, preimpoundment studies for estimating future reservoir water quality, prediction of reservoir temperatures, laboratory studies for selective withdrawal, determination of basinwide influences on water quality, establishment and review of standards and criteria, studies of irrigation return flow, and studies of the relationships among structures, reservoir site preparation, and water quality.

Reaeration of streams and reservoirs offers promise in improving water quality. Examples of this application would be reaeration of low-level releases from stratified reservoirs for protection of the stream fishery or in-stream aeration of a polluted river to increase the

capacity for assimilation of wastes. Techniques for reaeration of small streams and impoundments have been investigated and found to be applicable in varying degree. However, large streams and reservoirs introduce problems which do not allow immediate application of these techniques.

Reaeration has been used for many years in waste treatment, as in the activated sludge process. In-channel aeration for the recovery of badly polluted streams has received increasing attention.

Figure 1 shows the means by which oxygen enters or leaves a segment of a stream or reservoir. An easily defined contribution is through bulk flow; that is, the oxygen contained in the water entering and leaving the segment. Oxygen also enters the segment through precipitation which would also be considered as bulk flow. Other contributions are from chemicals, chemical reactions, and photosynthesis in plants. The most important natural addition of oxygen occurs through atmospheric aeration. Artificial oxygenation can be accomplished with air diffusers, mechanical aerators, or other devices.

In addition to bulk flow, oxygen leaves the system through decay of organic materials in the flow or on the bottom, plant respiration, and chemical reaction, such as nitrification (transformation of ammonia nitrogen to nitrates).

The earliest attempt to define the dissolved oxygen regime of a stream was made by Streeter and Phelps (S-37) with their oxygen sag equation:

$$\frac{dD}{dt} = K_1 L - K_2 D \quad (1)$$

where

- D = dissolved oxygen saturation deficit
- t = time
- L = biochemical oxygen demand (BOD)
- K<sub>1</sub> = decay (deoxygenation) rate constant
- K<sub>2</sub> = reoxygenation rate constant

The dissolved oxygen saturation deficit is defined as:

$$D = (C_s - C)$$

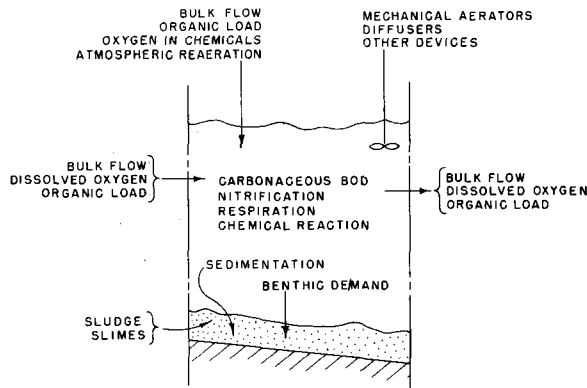


Figure 1. Oxygen balance in a finite element after Hann (H-3).

where

- C<sub>s</sub> = saturation concentration
- C = initial existing concentration

The oxygen-sag equation may be misapplied because:

- a. Deoxygenation and reoxygenation are not always first order reactions as shown in the equation.
- b. The equation is idealized in that other means of oxygen inflow and outflow are not included.
- c. Application to long stretches of the stream is not necessarily valid because of changing conditions and local variations.

An oxygen balance in a finite element, using the factors shown in Figure 1, more appropriately describes the actual physical situation. If the means of oxygen inflow or outflow can be described by differential equations, solution can be obtained by a method of finite differences. It is important to note, however, that Equation (1) is accurate under the conditions to which it is restricted.

## DISSOLVED OXYGEN REQUIREMENTS

Dissolved oxygen is required for the survival and growth of many aquatic organisms, including fish. Also, the absence of dissolved oxygen leads to



anaerobic decay of organic matter and results in undesirable esthetic qualities.

Federal recommendations for the levels of dissolved oxygen (C-22) for maintenance of fish and other aquatic life are quoted below:

“(1) For a diversified warm-water biota, including game fish, daily DO concentration should be above 5 mg/l, assuming that there are normal seasonal and daily variations above this concentration. Under extreme conditions, however, and with the same stipulation for seasonal and daily fluctuations, the DO may range between 5 mg/l and 4 mg/l for short periods of time, provided that the water quality is favorable in all other respects. In stratified eutrophic and dystrophic lakes, the DO requirements may not apply to the hypolimnion. In shallow unstratified lakes, they should apply to the entire circulating water mass.

“These requirements should apply to all waters except administratively established mixing zones. In lakes, such mixing zones must be restricted so as to limit the effect on the biota. In streams, there must be no blocks to migration and there must be adequate and safe passageways for migrating forms. These zones of passage must be extensive enough so that the majority of plankton and other drifting organisms are protected (see section on zones of passage).

“(2) For the cold water biota, it is desirable that DO concentrations be at or near saturation. This is especially important in spawning areas where DO levels must not be below 7 mg/l at any time. For good growth and the general well-being of trout, salmon, and other species of the biota, DO concentrations should not be below 6 mg/l. Under extreme conditions they may range between 6 and 5 mg/l for short periods provided that the water quality is favorable and normal daily and seasonal fluctuations occur. In large streams that have some stratification or that serve principally as migratory routes, DO levels may be as low as 5 mg/l for periods up to 6 hours, but should never be below 4 mg/l at any time or place.

“(3) DO levels in the hypolimnion of oligotrophic small inland lakes and in large lakes should not be

lowered below 6 mg/l at any time due to the addition of oxygen-demanding wastes or other materials.”

## OXIDATION

As discussed earlier, the dissolved oxygen regime of a stream is expressed by the Streeter-Phelps oxygen sag equation:

$$\frac{dD}{dt} = K_1 L - K_2 D \quad (1)$$

In addition to bulk flow, the major depletion of oxygen occurs by decay of organic matter (BOD). Carbonaceous, or first-stage BOD is described by:

$$\frac{dL}{dt} = -K_1 L \quad (1a)$$

The solution to this equation is given by:

$$L = L_a e^{-K_1 t} \quad (1b)$$

where  $L_a$  = the initial BOD at the start of the decay process. This decay can occur in the flow or on the bottom. Oxygen demand also occurs by nitrification (C-26, S-32, S-33, W-9). The nitrification stage sometimes occurs after the carbonaceous stage is completed and can be very significant, particularly in reservoirs. Streeter (S-34, S-35) discussed this two-stage oxidation in detail. It must be emphasized that the oxidation process is complex and variable from one case to another. Determination of oxygen demand in streams and reservoirs should be attempted only with a complete understanding of the processes involved.

Other chemical reactions result in lesser oxygen depletion.

Krenkel, et al (K-26) discuss the effect of reservoirs on the removal of BOD by biological oxidation. Reduced velocity causes oxygen demand to take place closer to the point of waste discharge. Reservoirs can be advantageous by providing large volumes of water for dilution of wastes. If the reservoir is stratified,

however, wastes can be confined to the hypolimnion and result in depletion of DO in that zone. DO depletion in the hypolimnion can also be caused by decay of sludge or other organic materials which have settled to the bottom of the reservoir. Settling of dead algae from the surface is a common example of this. If stratification persists for long periods of time, no atmospheric reaeration occurs, and DO can drop to zero in the hypolimnion. Therefore, low-level releases from a reservoir might have a desirable temperature, but be completely unacceptable in terms of DO.

Low DO also causes iron and manganese to return from the solid precipitated form back into solution. This condition can cause taste and odor problems in municipal water supplies.

Krenkel, et al discuss the variation of the decay rate constant with bacteria concentration, waste concentration, turbulent mixing, and temperature.

Variation of the decay rate constant  $K_1$  with temperature is usually determined by the relationship:

$$K_1(T) = K_1(20) \theta^{(T-20)} \tag{2}$$

where

- $K_1(T)$  = rate constant at  $T^{\circ}C$
- $K_1(20)$  = rate constant at  $20^{\circ}C$
- $\theta$  = a constant, usually 1.047

Reference (K-26) includes a discussion of variation of  $\theta$ .

Velz (V-7) states that BOD effects of bottom deposits may become acute where reservoir inflow velocities are less than 0.6 fps. Sludge deposits were found to return to suspension for velocities above 1.0 to 1.5 fps. The nature of the bottom material and currents within a given reservoir will, or course, determine the specific considerations for that reservoir.

Krenkel, et al (K-26) explain that reservoirs usually show improvement in water quality as the bottom deposits are oxidized or leached into solution and discharged. This applies particularly to debris which exists at the initial filling of the reservoir. The paper includes a tabulation of the oxygen demand of various types of soils and litter.

## REAERATION

### Basic Theories of Reaeration

Fick's first law of diffusion is expressed in vector notation as:

$$\vec{n}_A = W_A(\vec{n}_A + \vec{n}_B) - \rho D_{AB} \nabla W_A \tag{3}$$

where

- A = gas
- B = liquid
- $\vec{n}_A$  = mass flux of A,  $M/L^2T$
- $\vec{n}_B$  = mass flux of B,  $M/L^2T$
- $W_A$  =  $\rho_A/\rho$  mass fraction of A, dimensionless
- $\rho_A$  = mass density of A,  $M/L^3$
- $\rho_B$  = mass density of B,  $M/L^3$
- $\rho$  =  $\rho_A + \rho_B$  = mass density of solution,  $M/L^3$
- $\nabla W_A$  = mass density gradient,  $L^{-1}$
- $D_{AB}$  = mass diffusivity of gas into liquid,  $L^2/T$

The first term on the right side of the equation represents transfer by bulk flow while the second term represents transfer by molecular diffusion. Therefore, mass transfer by molecular diffusion (assuming a still liquid) is represented by:

$$\vec{n}_A = -\rho D_{AB} \nabla W_A \tag{4}$$

Considering the x-direction only, and changing to scalar notation, an alternate form is:

$$\frac{\partial m}{\partial t} = -Dm \frac{\partial c}{\partial x} \tag{5}$$

where

- $\frac{\partial m}{\partial t}$  = rate of mass transfer per unit area,  $M/L^2T$
- $Dm$  = molecular diffusivity,  $L^2T$
- $\frac{\partial c}{\partial x}$  = concentration gradient,  $M/L^4$

Equation (5) describes steady-state transfer. If the concentration varies with time as well as distance:

$$\frac{\partial c}{\partial t} = D_m \frac{\partial^2 c}{\partial x^2} \quad (6)$$

which is a form of Fick's second law of diffusion. A solution to this equation was found by Stefan (S-28, S-29) in 1878 and later applied by Phelps. The solution is:

$$C_t = C_s - 0.811(C_s - C_o)(e^{-K_d t} + \frac{1}{9}e^{-9K_d t} + \frac{1}{25}e^{-25K_d t} + \dots) \quad (7)$$

where

$$K_d = \frac{2 D_m t}{4 h^2}$$

h = depth of water  
 $D_m$  = molecular diffusivity  
 $C_t$  = concentration at time t  
 $C_s$  = saturation concentration  
 $C_o$  = initial concentration, t = 0

The molecular diffusivity of oxygen into water has been estimated (K-3) to be  $2.1 \text{ cm}^2/\text{sec}$  at  $20^\circ \text{C}$ .

The dissolved oxygen saturation deficit, D, is determined in aeration problems by the difference between the initial existing concentration,  $C_o$ , and the concentration at saturation,  $C_s$ . The saturation concentration depends upon the solubility of air or oxygen in water, which in turn depends upon temperature, pressure, and salinity. For example, with zero salinity, Figure 2, the solubility  $C_s$  varies from about 14.6 mg/l at  $0^\circ \text{C}$  to about 7.5 mg/l at  $30^\circ \text{C}$ , at atmospheric pressure. Phelps suggests a reduction in solubility of 10 percent for each 10,000 mg/l salinity (as chlorides). The saturation value increases with pressure.

As shown in Equation (1), the rate at which oxygen is absorbed is expressed as being directly proportional to the saturation deficit:

$$\frac{dD}{dt} = -K_2 D \quad (8)$$

This equation can be integrated to give a solution in the form:

$$\frac{D}{D_o} = e^{-K_2 t} \quad (9)$$

where  $D_o$  is the initial deficit.

An alternative form is:

$$\frac{D}{D_o} = 10^{-k_2 t} \quad (10)$$

where

$$k_2 = K_2 / 2.30$$

Some references fail to show this distinction in the use of  $K_2$  and  $k_2$ .

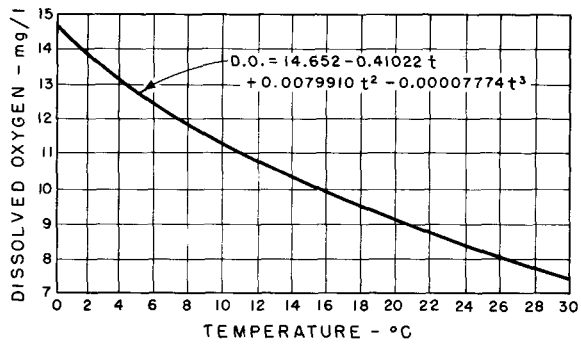


Figure 2. Experimentally determined and computed dissolved oxygen saturation values from Reference C-20

Evaluation of  $K_2$  is the key to the development of an accurate description for the reaeration mechanism. Several theories have been proposed to provide an analytical basis for determination of  $K_2$ . Whitman (W-14), and Lewis and Whitman (L-11), in 1923 and 1924, presented the two-film theory. This theory makes four major statements:

1. Laminar layers of gas and liquid at the interface control the transfer process.
2. The laminar liquid film at the water surface controls the rate of oxygen transfer through the surface.

3. The film is saturated with oxygen at the surface.

4. The water is well mixed so that the concentration is uniform in the body below the laminar film.

Thus, a steep concentration gradient exists in the film and oxygen transfer takes place by molecular diffusion according to Fick's Law (Equation (5)), which becomes:

$$q = \frac{-A D_m D}{b} \quad (11)$$

where

- q = rate of oxygen transfer, M/T
- A = surface area, L<sup>2</sup>
- D<sub>m</sub> = molecular diffusion coefficient, L<sup>2</sup>/T
- D = saturation deficit, M/L<sup>3</sup>
- b = stagnant film thickness, L

A liquid film coefficient, K<sub>L</sub>, is introduced as a correlary to a rate constant, giving:

$$q = -AK_L D \quad (12)$$

where

$$K_L = \frac{D_m}{b}$$

The film theory has not been generally accepted because the assumption of a laminar film is not physically realistic. It must also be noted that the film thickness *b* has never been measured; therefore, analytical evaluation of K<sub>L</sub> is not possible.

The term K<sub>L</sub>*a* also appears in the literature. Dividing both sides of Equation (12) by the volume *V* expresses the rate of change in concentration:

$$\frac{q}{V} = -\frac{A}{V} K_L D \text{ or } \frac{dc}{dt} = -K_L a D \quad (13)$$

where

$$K_L a = K_L \frac{A}{V}$$

Objections to the film theory resulted in several alternatives being offered. Higbie (H-10) proposed his film penetration theory, which assumes that the transfer process takes place through alternate cycles of gas absorption and mixing. The water body is assumed

to be stagnant for a short period during which oxygen is absorbed and downward molecular diffusion occurs. Then, the water is completely mixed and the cycle begins again. This theory led to an alternate expression for K<sub>L</sub>:

$$K_L = 2\sqrt{\frac{D_m}{\pi t'}} \quad (14)$$

where *t'* is the time required to complete one cycle of absorption and mixing. The penetration theory was the first to recognize the importance of turbulent mixing in renewing the unsaturated water exposed to the free surface. From a physical view, however, the assumption of alternate periods of stagnation and mixing is obviously unrealistic. Also, the penetration theory still contains the objectionable assumption of a surface film.

Danckwerts (D-2) extended the penetration theory by stressing the idea of surface renewal. He questioned the film concept and suggested a statistical distribution for mixing of individual elements. This approach seems more realistic, in view of the physical structure of turbulence.

The statistical distribution is expressed as:

$$f(t) = re^{-rt} \quad (15)$$

where *r* is a rate of surface renewal, expressed as a fraction. Therefore, *r* is analagous to the reciprocal of *t'* in Equation (14). Danckwerts proposal thus results in:

$$K_L = \sqrt{D_m r} \quad (16)$$

Dobbins (D-11) combined the film theory with the surface renewal theory by assuming continuous mixing below the film along with continuous renewal of the surface film and molecular diffusion within the film. Using Danckwerts' statistical distribution and a film thickness *b*, Dobbins derived:

$$K_L = \sqrt{D_m r} \coth \sqrt{\frac{rb^2}{D_m}} \quad (17)$$

Note that as *r* approaches zero, K<sub>L</sub> approaches that defined by the surface renewal theory: i.e.

$$K_L \rightarrow \sqrt{\frac{D_m^2}{rb^2}} \rightarrow \frac{D_m}{b}$$

Also, as  $r$  approaches a large number,  $K_L$  approaches that defined by the surface renewal theory; i.e.,

$$K_L \rightarrow \sqrt{Dmr}.$$

O'Connor and Dobbins (O-2) determined that Equation (17) would be identical to Equation (16) for values of  $r$ ,  $b$ , and  $Dm$  which typify natural streams. They further postulated that streams had either nonisotropic turbulence or isotropic turbulence, depending on whether Chezy's  $C$  was less than or greater than 17, respectively. Many investigators have recognized that this appears to be a rather arbitrary way of defining isotropic turbulence. Actually, O'Connor and Dobbins, by their definition, found that most streams which they analyzed had isotropic turbulence. To test their concept of surface renewal, they performed laboratory experiments using an oscillating grid to produce turbulence. The results indicated a good correlation between the grid oscillation frequency and the observed  $k_2$ .

This theoretical and experimental work led to the expression:

$$k_2 = \frac{(Dm \bar{u})^{1/2}}{2.31 H^{3/2}} \quad (18)$$

for isotropic turbulence and

$$k_2 = \frac{480 Dm^{1/2} S_e^{1/4}}{H^{5/4}} \quad (19)$$

for nonisotropic turbulence.

In these equations:

$\bar{u}$  = average flow velocity  
 $H$  = average flow depth  
 $S_e$  = energy gradient

As mentioned above, most streams were found to conform to Equation (18). The measurements were made on reaches selected to minimize effects of bottom sludge deposits and algae. As much as 50 percent variation between theoretical values of  $k_2$  and those determined by the field measurements was noted.

### Empirical Studies

The foundation for empirical evaluation of  $k_2$  was the work of Streeter and Phelps (S-37) on the Ohio River.

Their oxygen sag equation was referred to earlier as Equation (1). By applying this equation, they indirectly measured values of  $k_2$ . Streeter and Phelps correctly hypothesized that the  $k_2$  values should be related to temperature, depth, and turbulence in the stream. Assuming the temperature to be constant, they reasoned, with the aid of the solution to Fick's second law (Equation (7)), that  $k_2$  should be approximately proportional to the inverse square of the depth. Also, they felt that the remaining factor, turbulence, should be directly proportional to a power function of the flow velocity. They thus derived the empirical relationship:

$$k_2 = \frac{Cv^n}{H^2} \quad (20)$$

where  $C$  and  $n$  are constants that must be determined. The Ohio River measurements of Streeter and Phelps resulted in  $n$  values ranging from 0.57 to 5.40 and corresponding  $C$  values from 0.23 to 131. The need for caution in general application of Equation (20) is obvious.

Churchill, et al (C-12) used a strictly empirical approach to develop the relationship:

$$k_2(20) = 5.026 \bar{u}^{0.969} H^{-1.673} \quad (21)$$

where

$k_2(20)$  = reaeration coefficient at 20° C  
 $\bar{u}$  = average velocity, fps  
 $H$  = mean depth of flow, ft

Multiple regression analysis was used with 509 sets of data to develop Equation (21), which is applicable to unpolluted streams.

This data collection program was accomplished with great care. The studies were conducted in streams below impoundments for which releases were low in dissolved oxygen and BOD. The reaches were chosen to have relative uniform hydraulic parameters of slope, depth, and shape. Generally, Churchill, et al attempted to eliminate those factors which tend to mask the true value of  $k_2$ . These data are generally accepted to be the most reliable available at the present time.

Owens, et al (O-9) combined the data of Churchill, et al (C-12) and Gameson, et al (G-2), and by regression analysis developed the equation:

$$k_2(20) = 9.41 \bar{u}^{0.67} H^{-1.85} \quad (22)$$

for velocities of 0.1 to 5.0 fps and depths of 0.4 to 11 ft. Using their own data for fast-flowing, shallow streams, they obtained the equation:

$$k_2(20) = 10.1 \bar{u}^{0.73} H^{-1.75} \quad (23)$$

which gives a  $k_2$  considerable higher than determined by data of Churchill, et al, Equation (21).

The experimental procedure and interference by bottom oxygen demand and plant photosynthesis make the results rather speculative, even though correction factors were applied. The restriction to fast-flowing, shallow streams is also an important limitation, even if the relationship could be accepted as valid.

Isaacs and Gaudy (I-11) used a rectangular laboratory flume to develop the expression:

$$k_2 = 3.053 \bar{u} H^{-1.5} \quad (24)$$

The similarity of these empirical relationships with that originally proposed by Streeter and Phelps should be noted.

Much time and effort has been devoted to attempts to relate the reaeration coefficient  $k_2$  to the hydraulic parameters of velocity and depth. Little progress has been made, for the following reasons:

1. Average values of velocity and depth are poor measures of flow conditions in a stream. Churchill, et al, for example, cautioned against applying their results to reaches with white water.
2. Even if these average parameters were acceptable correlations, they would be extremely difficult to measure accurately in the field.
3. Other effects, such as BOD, cannot be isolated when analyzing relatively long reaches.

Intuitively, the reaeration rate should be related to some measure of turbulence, as indicated in several of the investigations described above. Since turbulence is difficult to measure directly in the field, some investigators have attempted to relate  $k_2$  to some indirect indicator of turbulence, such as eddy size or the rate of energy dissipation.

Krenkel and Orlob (K-23) applied kinetic gas theory to explain the transfer process. The change of reaction rate with temperature is given by:

$$k = A'e^{-\frac{E_a}{RT}} \quad (25)$$

where

- $k$  = the reaction rate
- $E_a$  = energy required by a molecule to be included in a reaction
- $R$  = the universal gas constant
- $T$  = absolute temperature
- $A$  = collision factor (analogous to a frequency)

Krenkel and Orlob reasoned that the movement of molecules from one equilibrium position to another in turbulent shear flow is analogous to the movement of molecules over a barrier of potential energy, for which a certain activation energy is required. Furthermore, they argued that some internal flow mechanism such as turbulence was required to sustain the absorption process. The longitudinal mixing coefficient was chosen as being the most appropriate. This coefficient was evaluated in the laboratory experiments by measuring the dispersion of an injected tracer. Correlation of this parameter with oxygen absorption measured in the laboratory flume gave:

$$k = 1.418e^{-\frac{E_a}{RT}} \frac{D_L}{h^2} - 0.0069 \quad (26)$$

where

- $D_L$  = longitudinal mixing coefficient
- $h$  = depth of flow

$D_L/h^2$  is proportional to the frequency at which gas molecules collide with the surface layers, and can be considered as a surface renewal rate.

Harleman and Holley (H-4) questioned the use of the longitudinal mixing coefficient as a measure of turbulence, explaining that the mechanism is one of dispersion caused by convective effects and is not, therefore, representative of turbulence. They suggested that the correlation was actually between  $k_2$  and the average vertical eddy diffusivity.

Krenkel and Orlob also found a direct relationship between  $k_2$  and the rate of energy dissipation in their laboratory flume. This relationship is:

$$k_2' = (1.141 \times 10^{-4}) E^{0.408} h^{-0.660} \quad (27)$$

where

$$\begin{aligned} k_2' &= k_2 \text{ corrected to } 20^\circ \text{ C} \\ E &= \text{rate of energy dissipation per unit mass} \\ h &= \text{flow depth} \end{aligned}$$

In open channel flow:

$$E = \bar{u} Se g \quad (28)$$

where

$$\begin{aligned} \bar{u} &= \text{mean flow velocity} \\ Se &= \text{energy gradient} \\ g &= \text{gravity} \end{aligned}$$

The correlation between  $k_2$  and  $E$  appears to be a very valuable result of the work, even though it was not given primary emphasis in the paper. However, in defining  $E$ , the difficulty remains in measurement of  $\bar{u}$ .

Krenkel and Orlob also suggest that the absorption rate of some gas should be in known proportion to that of another gas. In cases where the absorption rate of oxygen might be affected by BOD, for example, some other gas could be used to indirectly measure the oxygen absorption rate. The possible use of radioactive gases was mentioned.

Tsivoglou (T-28) describes such a method for direct measurement of the reaeration capacity of a stream. The method uses radioactive gas tracers to determine both dispersion and gas transfer. This represents the first known attempt to measure  $k_2$  directly. All previous work has involved an indirect evaluation of  $k_2$  through computation based on an oxygen-sag curve, even though the value thus obtained has been referred to as being "observed." The tracer method was developed in the laboratory and demonstrated in full-scale field studies.

Tsivoglou stresses that the tracer method should be considered as a primary standard, to which all the empirical results described earlier should be compared.

The O'Connor-Dobbins equation and the equation of Churchill, et al, were found to give approximate predictions for the Jackson River in Virginia. Tsivoglou states that comparisons of this type must be made with caution, because of errors in determining hydraulic parameters of the stream. More cross sections are

necessary for accurate computations than are usually practical from a cost standpoint.

*Effect of temperature.*—The most commonly used description of the effect of temperature on  $k_2$  was given by Streeter and Phelps (S-37):

$$k_2(T) = k_2(20) 1.047^{(T-20)} \quad (29)$$

where

$$\begin{aligned} k_2(T) &= \text{reaeration coefficient at } T^\circ \text{ C} \\ k_2(20) &= \text{reaeration coefficient at } 20^\circ \text{ C} \end{aligned}$$

Krenkel, et al (K-26) summarize the work of other investigators. They state that O'Connor and Dobbins (O-2) and Krenkel and Orlob (K-23) predict a coefficient of 1.016. However, this value is incorrect and has apparently been confused with the correction coefficient for surface transfer as reported by Streeter, Wright, and Kehr (S-35).

Dobbins (D-11) maintains that the coefficient should be variable. Tsivoglou (T-28) found the relationship:

$$\frac{k_2(T_2)}{k_2(T_1)} = \theta^{(T_2-T_1)} \quad (30)$$

where  $\theta$  was  $1.022 \pm 0.003$ . Churchill, et al (C-12) found that  $\theta = 1.024$ , based on a large number of measurements.

A relationship in the form of Equation (20) should generally apply to evaluation of  $k_2$  for open structures and jets. However, where high velocities or severe surface turbulence occur, atmospheric reaeration is higher than that predicted by any of the empirical equations. Very little work has been done in this area. Tsivoglou's tracer method might be appropriate in this case.

This review of the state-of-the-art, with respect to natural reaeration of streams, indicates that attempts are being continued to better define correlation with hydraulic parameters. Empirically derived equations, most in the basic form of Streeter and Phelps' original work, continue to be used for lack of something better. Tsivoglou's tracer method for direct measurement of  $k_2$  is a promising development, but remains restricted

to in situ measurements. It is not yet suitable for prediction, because of the usual barriers in relating  $k_2$  to hydraulic parameters.

It seems to the writer that correlation with some measure of energy dissipation is the only rational approach. Energy dissipated is the only means of summarizing activity within a finite segment of the stream. However, it is not difficult to imagine possible differences in stream segments with similar energy dissipation (such as a tranquil stream segment with a waterfall versus a segment with rapids).

### Photosynthesis

Photosynthesis is the process by which carbohydrates are formed from water and carbon dioxide by chlorophyll in living plants. The reaction results in the release of oxygen.

Krenkel, et al (K-26) discuss the importance of photosynthesis as an oxygen source in reservoirs and summarize the thinking of several investigators. Experience has shown that the relative contribution of photosynthesis has ranged from unimportant to very important. Photosynthetic oxygen should be considered in the oxygen balance but should not be depended upon for waste assimilation. Knowledge in this subject has not advanced sufficiently to allow satisfactory application in practice. Hull (H-18, H-19, H-20) has published several papers on this subject. Other references include Edwards (E-5), Ignjatovic (I-2), Mackenthun (M-1), Verduin (V-8), and Winberg and Sivko (W-21).

### Artificial Reaeration

Thackston and Speece (T-15) report that when mechanical devices are used for stream aeration, a level of 40 percent of saturation prior to reaeration is often considered as the upper limit for economical aeration. Aeration facilities should generally be located at the low point on the oxygen sag curve. Site choice is also influenced by the location of existing facilities (such as those with head loss), power availability, accessibility, and availability of personnel for operation and maintenance (T-15).

The break-even point of oxygen deficit versus cost of artificial reaeration depends on the characteristics of the particular device. The statement of 40-percent saturation may apply to many devices. However, a more appropriate general statement might be simply that efficiency of reaeration devices is directly proportional to the oxygen deficit, just as in natural reaeration.

*Cascades.*—Several British researchers (B-5) have investigated atmospheric reaeration at weirs. Data from four weir systems resulted in the empirical equation:

$$r = 1 + 0.11 ab (1 + 0.046 T) h \quad (31)$$

where

- $r$  = ratio of upstream saturation deficit to downstream saturation deficit
- $a$  = coefficient for water quality (1.25 for slightly polluted water, 1.0 for moderate pollution, and 0.8 for sewage effluent)
- $b$  = 1 for a free weir, 1.3 for the examined step weirs
- $T$  = water temperature, °C
- $h$  = height of free fall, ft

The equation was partially verified for flows of 1 to 500 million gallons per day (mgd) (1.55 to 774 cfs). The equation also applies to loss of oxygen from supersaturated water. The authors state that most of the oxygen uptake resulted from splashing at the base of a free fall. Therefore, efficiency would be expected to increase with the number of steps, as indicated by the value of  $b$ . This is conjecture, although not entirely without basis. The phenomenon is likely a combination of insufflation, splashing, and turbulence (conjecture by the writer).

In an earlier reference, Gameson (G-6) presents a somewhat simpler relationship:

$$r = 1 + abh/2 \quad (32)$$

where the parameters are as defined above, except that  $h$  is measured in meters. The effect of water temperature is not considered.

Very recently, Huckabay and Keller (H-16) have described a "cascade board." The development of this device was partially stimulated by Gameson's finding that the efficiency of aeration at weirs was directly related to the number of steps. The experimental apparatus consisted of a variable slope board covered with corrugated metal, with the corrugations transverse to the direction of flow. Tap water was used for the tests. Flow rate varied from 0.02 to 0.08 mgd/ft of width (about 0.03 to 0.12 cfs/ft).

The mass transfer coefficient  $K_L a$  was expressed in terms of a "penetration factor," which in turn was related to a modified Reynolds number and the Schmidt number. The modified Reynolds number included flow rate, board length and inclination, and



kinematic viscosity. The Schmidt number consisted of kinematic viscosity, density, and molecular diffusivity.

The authors conclude that the "cascade board" appears to be a promising aeration device. However, it is very difficult to extract information concerning actual mass transfer rates or coefficients from the paper. They state that additional investigations are being planned.

The writer suggests that these preliminary results should not be directly applied to aeration of large discharges, particularly in view of the very small discharges tested.

Aeration at weirs is also discussed by Albrecht (A-3, A-4), Grindrod (G-17), Manzack (M-5), Scott and Wisniewski (S-5), and Thackston and Speece (T-15).

Weirs as aeration devices have the advantages of being relatively maintenance free and requiring no direct energy expenditure. Where "free" head is available, weirs can be used very beneficially. However, if the head determines power loss or pumping requirements, cost of operation must be determined on that basis. Possible disadvantages of weir aeration systems are high capital cost, particularly for large structures, and low transfer efficiency.

*Valves.*—The Tennessee Valley Authority (TVA) (E-7) has evaluated the fixed-cone (Howell-Bunger) valve for aerating reservoir discharges. Tests were conducted with discharge either to a partially enclosed jet containment structure or to a tailwater pool. Aeration efficiency was found to be related to the discharge velocity. Jet thickness had little effect in the range covered by the tests. At discharge velocities less than 30 fps the discharge to the tailwater pool was more efficient than the confined discharge. For velocities above 30 fps either condition resulted in an oxygen increase greater than 80 percent of the initial deficit. The data show that the initial deficit had a noticeable, but ill-defined effect on the efficiency.

To the writer's knowledge, other control devices such as hollow-jet valves or slide gates have not been similarly evaluated for use in reaeration, even though they would probably have lower efficiency than the fixed-cone valve because of jet configurations which would result in less air-water contact. However, the reaeration effect might finally be determined by the design of the containment structure, when such a structure is used, or other appurtenances. The TVA work did not separate oxygen uptake by the jet from that in the catchment structure or tailwater pool. This would be useful information, if sampling methods could be devised.

The amount of DO increase in free chutes and tunnels and in energy dissipators such as stilling basins, baffled drops, and flip buckets also needs to be determined. Possible reaeration benefits of hydraulic devices and structures which are normally a part of the project plan should not be overlooked. In some cases departures from usual design practice may be required to increase the reaeration benefit.

*Diffusers.*—Using the penetration theory, gas absorption from rising bubbles can be expressed by (B-19):

$$\frac{dm}{dt} = \sqrt{\frac{4 D_m}{\pi \text{texp}}} C_s \quad (33)$$

where

$$\begin{aligned} \frac{dm}{dt} &= \text{average rate of mass transfer, } M/L^2T \\ D_m &= \text{molecular diffusivity, } L^2/T \\ \text{texp} &= \text{exposure time of bubble (time required for liquid to pass one bubble diameter), } T \\ C_s &= \text{solubility of the gas in the liquid, } M/L^3 \end{aligned}$$

This theory assumes the liquid at the bubble surface to be at zero concentration of dissolved oxygen, and that no surface active agents are present.

This equation can also be expressed as:

$$\frac{dm}{dt} = \sqrt{\frac{4 D_m v_t}{\pi D'}} C_s \quad (34)$$

where

$$\begin{aligned} v_t &= \text{terminal velocity of the bubble, } L/T \\ D' &= \text{bubble diameter, } L \end{aligned}$$

Thus:

$$K_L = \sqrt{\frac{4 D_m v_t}{\pi D'}} \quad (35)$$

The bubble terminal velocity is given by:

$$v_t^2 = 4/3 \frac{gD'}{f} \left( \frac{\gamma - \gamma_a}{\gamma} \right) \quad (36)$$

where

- $g$  = gravity,  $L/T^2$
- $f$  = friction factor (drag coefficient), dimensionless
- $\gamma$  = specific weight of water,  $M/L^3$
- $\gamma_a$  = specific weight of air,  $M/L^3$

However,  $\left(\frac{\gamma - \gamma_a}{\gamma}\right) \approx 1.$

Therefore,

$$v_t^2 = 4/3 \frac{gD'}{f} \quad (37)$$

can be used.

The friction factor is dependent upon the Reynolds number:

$$Re = \frac{v_t D'}{\nu}$$

where  $\nu$  = kinematic viscosity,  $L^2/T$ .

A diagram of  $f$  versus  $Re$  for spheres is used for a trial-and-error solution.

For example, assume a 1/4-inch bubble and  $f = 0.44$  as a first trial.

From Equation (37):

$$v_t^2 = \frac{4/3(32.2)(1/48)}{0.44}$$

$$v_t = 1.43 \text{ fps}$$

From Equation (38):

$$Re = \frac{1.43(1/48)}{(1.664 \times 10^{-5})} = 1,700$$

From the  $f$ - $Re$  diagram,  $f \approx 0.44$ .

Therefore, the first trial is correct and  $v_t = 1.43$  fps.

From boundary layer theory, the transfer efficiency of a bubble diffuser can be expressed in terms of the

overall transfer coefficient or liquid film coefficient:

$$K_L = \frac{D_m}{D'} [2 + 0.664 (Re)^{1/2} (Sc)^{1/3}] \quad (39)$$

(after B-19)

where

- $D_m$  = molecular diffusivity,  $L^2/T$
- $D'$  = bubble diameter,  $L$
- $Re$  = Reynolds number
- $Sc$  =  $\nu/D_m$ , Schmidt number

This relationship is more complex than Equation (35), which does not account for viscous effects.

Johnson, et al (J-8) measured absorption rates of carbon dioxide, ethylene, and butene from single rising bubbles in a water column to determine the relationship:

$$Sh = 1.13 Pe^{1/2} \left( \frac{d_e}{0.45 + 0.2 d_e} \right)^{1/2} \quad (40)$$

where

$$Sh = \text{Sherwood number, } \frac{K_L d_e}{D_m}$$

- $d_e$  = equivalent bubble diameter,  $L$
- $D_m$  = molecular diffusivity,  $L^2/T$

$$Pe = \text{Peclet number, } \frac{v d_e}{D_m}$$

$$v = \text{stream velocity or bubble velocity, } L/T$$

which conformed quite closely to a theoretically derived equation.

An alternate form is:

$$K_L = 1.13 \left( \frac{D_m v}{0.45 + 0.2 d_e} \right)^{1/2} \quad (41)$$

These equations apply for Reynold's numbers between 500 and 20,000. The bubbles were oblate spheroids, ellipsoids, or spherical caps, depending on the equivalent diameter, which ranged from 0.4 to 2.0 cm. Equation (41) applies to equivalent diameters of 0.6 to 4.0 cm. This result can be compared with the

theoretical  $K_L$  for spherical bubbles from Equation (35):

$$K_L = \left( \frac{4 D_m v}{\pi d_e} \right)^{1/2} \quad (42)$$

with appropriate changes in notation, and with Equation (39). The writer suggests that Equation (41) be used. The limitation to spherical bubbles in the other cases is not practical.

The ratio of oxygen transferred from a bubble to the volume of oxygen contained in the bubble determines the transfer efficiency.

Similarly, the efficiency of a diffuser system is determined by the ratio of oxygen transferred to oxygen supplied:

$$E = \frac{TR}{SR} \times 100 \quad (43)$$

where

$E$  = efficiency, percent  
 $TR$  = oxygen transfer rate, M/T  
 $SR$  = oxygen supply rate, M/T

Eckenfelder (E-1) summarizes the work of several other investigators and presents the relationship:

$$K_L = C \frac{D_m Re Sc^{1/2}}{D' H^{1/3}} \quad (44)$$

where  $C$  is an empirical constant,

$H$  is the tank depth.

This equation is similar to those presented previously, with the exception of the inclusion of tank depth. It also must be noted that Equation (44) holds only for the narrow range of Reynolds numbers of 50 to 500.

Eckenfelder also formulates an overall mass transfer coefficient for evaluating performance of a commercial diffuser:

$$K_L a = \frac{c G_s^{(1-n)} H^{2/3}}{V} \quad (45)$$

where

$K_L$  = liquid film coefficient,  $\text{min}^{-1}$   
 $a$  = ratio of total bubble surface area to liquid volume,  $A/V$ ,  $\text{ft}^{-1}$   
 $c$  = a constant  
 $G_s$  = airflow, SCFM (at standard temperature and pressure)  
 $V$  = tank volume,  $\text{ft}^3$   
 $(1-n)$  = variable exponent which is a function of bubble size  
 $H$  = tank depth, ft

The exponent of  $H$  has actually been found to vary from 0.45 to 0.77 depending on the type of diffuser and the particular application. The exponent  $(1-n)$  might vary from 0.8 to 1.4, with higher values for smaller bubbles and correspondingly greater transfer rates.

Eckenfelder also summarizes the velocity and shape characteristics of air bubbles in water as they vary with the Reynolds number of the bubble. At  $Re < 300$ , the bubbles are rigid spheres which rise either in a rectilinear or a helical motion. For  $Re = 300 - 4,000$ , the bubbles are ellipsoidal in shape and rise with a rectilinear, rocking motion. The bubbles are shaped as spherical caps for  $Re > 4,000$ .

Tyler (T-34) produced one of the early proposals for the use of diffusers for supplemental reaeration of streams. He reported an average efficiency of about 7 percent, using carborundum plates and porous tubes under 12 feet of water.

Experience with diffusers in waste treatment is well documented. Reference (T-3) contains an excellent summary of diffuser types, design, and economics as applied to waste treatment.

Diffusers are classified (T-3) as porous or nonporous. Porous diffusers consist of plates or tubes, usually formed with a ceramic of silicon dioxide or aluminum oxide held in a porous mass with a ceramic binder. Porous diffusers may also consist of nonceramic plastic-wrapped tubes or plastic-cloth tubes.

Nonporous diffusers exist in several types. The nozzle and orifice types are made of metal or plastic with larger openings (and larger bubbles) than the porous diffusers. The valve type has a disk or valve which closes when the air supply is cut off. The valve type produces large bubbles. The shear type has a square

shape and an open top through which water enters, thus "shearing" the bubbles into smaller sizes. The water jet type consists of a system of nozzles which entrain air supplied to one side of the nozzle. For temporary use or in unusual circumstances, perforated or slotted pipes are used. This type is usually used only in shallow water, has a low efficiency, and tends to clog and corrode readily.

Plain jets (Sparjers) are often referred to in the literature. Reference (T-3) describes the Sparjer as a controlled air-release device which utilizes a cluster of four high-velocity short-tube orifices to disperse the air in a controlled pattern. The bubbles break into smaller bubbles a short distance above the device. Orifice sizes vary from 1/8 to 5/16 inch, depending on the application.

Diffuser efficiencies as high as 17.5 percent have been measured in aeration tanks. However, this efficiency seems unusually high, in light of many other references which indicate efficiencies ranging from 2 to 8 percent. Oxygen transfer was found to increase with depth. This is due to the increase in the saturation concentration caused by an increase in pressure. The oxygen saturation deficit is larger, and oxygen transfer occurs at a faster rate.

Fischerstrom (F-5) suggests the use of diffusers close to the surface with introduction of relatively large quantities of air. Several examples of the application of this method in Sweden are described. The method is based on the idea that although transfer efficiency is reduced by introducing air at shallow depths, more air can be supplied for the same amount of power required for deeper diffusers.

The number of diffusers required for a given application depends upon the recommended flow rate per diffuser, which usually varies between 4 and 15 cfm/diffuser (0.1 to 0.4 cu m/min). Diffuser spacing should be 6 to 24 inches. Clogging of diffusers can be eliminated by adequate filtering of the air supply.

Installation of a diffused air system requires blowers and housing, air piping and headers, diffusers and supports. Annual operating expense consists of power cost and equipment maintenance. Clogging is the most serious maintenance problem (T-4). Reference (T-4) includes aids for economic analysis.

Palladino (P-1) used drilled pipe diffusers under 4 to 5 feet of water and attained an efficiency of only 1.7 percent.

Wisniewski (W-23) reports the use of a bed of diffuser plates on the Flambeau River in Wisconsin, with efficiencies of 6 to 8 percent.

As mentioned earlier, the efficiency depends on the initial level of DO below the saturation level.

Diffusers have been widely accepted as aeration devices and may have application to specific problems of reaeration of streams and reservoirs. However, the writer feels that because of the usual low efficiencies, high initial cost, and possible maintenance problems, alternate devices should be considered. It is the writer's opinion that diffusers probably have an advantage when used in reservoirs, both for direct aeration and mixing. However, their use in streams might be questionable.

*Mechanical aerators.*—Mechanical aerators accomplish reaeration at the water surface and also often meet mixing requirements in waste treatment practice. Reference (T-3) contains an excellent description of mechanical aerators, including photographs.

Mechanical aerators can transfer oxygen by surface renewal and interchange (surface aerators) or by dispersing compressed air fed below the surface to a rotating agitator or turbine (turbine aerators).

The updraft-type surface aerator lifts large volumes of liquid above the surface for exposure to the atmosphere. The plate-updraft type produces a high level of surface turbulence. The turbine-updraft type (or combination type) consists of a turbine with a pipe or sparge ring discharging air below the rotating blades.

In the downdraft type, air is supplied by the negative head produced by the rotor. External blowers or compressors are not required.

The brush-type surface aerator consists of a horizontal revolving shaft with combs, blades, etc., extending below the water surface.

The efficiency of a mechanical aerator is expressed as:

$$N = \frac{K_L a D W}{P} \quad (46)$$

where

N = efficiency, lb (or g)/hp-hr  
 $K_L a$  = overall transfer coefficient,  $T^{-1}$

D = oxygen deficit, M/L<sup>3</sup>,  
W = capacity of system, L<sup>3</sup>  
P = brake horsepower, hp

The numerator of Equation (46) can be measured in the field as a single quantity, the weight of oxygen transferred per unit time.

Burns, et al (B-33) describe the use of a plate-updraft-type surface aerator placed at the location of minimum DO in a stream. With an initial DO deficit of 100 percent, an efficiency of 2.15 lb/hp-hr (1.61 lb/kwhr) was obtained. A discussion of the paper describes German use of floating aerators for which an efficiency of 1.75 lb/kwhr (2.34 lb/hp-hr) was obtained at 50 percent DO deficit.

Downing, et al (D-15) describe tests of two types of mechanical aerators of British manufacture (Searle aerator and Simplex cone). Effects of temperature, immersion depth, and surface-active agents were determined. Maximum efficiencies for the two types were about 1,450 g/kwhr, or approximately 3.2 lb/kwhr, based on total power consumption. The tests were conducted in full-scale laboratory apparatus with 100 percent DO deficit. The paper also discusses the Kessener brush aerator and the Sheffield system of rotating paddles; however, no efficiency data are given.

Thackston and Speece (T-15) discuss a floating aerator with two 10-foot-diameter rotating turbines in vertical draft tubes. Low-lift, high-capacity pumps throw the water into the air from the periphery of the turbines (updraft type). The aerators were used in a canal and efficiencies were 1.3 lb/hp-hr (1.0 lb/kwhr) for flows less than 3,000 cfs and 3.4 lb/hp-hr (2.5 lb/kwhr) for flows greater than 4,400 cfs. Initial DO level was not stated.

In the writer's opinion, mechanical aerators have definite application to stream reaeration, except where they might present hazards to recreation or navigation. In some locations, noise of operation might also be objectionable. Initial cost of the equipment is high. However, a wide variety of types is available. Application to reservoir reaeration is doubtful. The epilimnion is usually well mixed and relatively high in dissolved oxygen. The mixing effect of the mechanical aerators would not, in most cases, extend into the deeper layers of the reservoir.

**Turbine injection.**—Where power turbines are set above tailwater level, which is usually the case, the vacuum produced in the draft tube can be used to draw air from the atmosphere. Vents can be designed to open

automatically, can be permanently open, or can be valved for closer control. Another method is to introduce compressed air either above or below the turbine runner. This approach is necessary whenever a natural draft due to vacuum does not exist. Many hydroplants include provisions for injection of air for the purposes of cavitation suppression or control of draft tube surging (D-21). Therefore, the mechanics of venting, etc., are well known. However, in most cases the increase in DO downstream has been an incidental and unmeasured benefit.

Wagner (W-1, W-2, W-3, W-4) describes early studies in turbine aeration and gives the first detailed discussion of operation, including cost and efficiency.

The most extensive and well documented experience in turbine aeration is in Wisconsin (S-5, S-6, W-16, W-17, W-19, W-23). However, this experience is limited to installations with heads of 8 to 21 feet.

Scott, et al (S-6) describe the results of turbine venting at Pixley Dam on the Flambeau River in Wisconsin. The turbines are the double-runner horizontal type. Air was injected in the annular space between the runner ring and the cone-shaped part of the draft chest which surrounds the runner ring. According to the authors, air injection resulted in a power loss because of reduction in discharge through the turbine. Reaeration efficiencies are stated in terms of this power loss. The maximum DO gain at Pixley Dam was 4.87 lb/kwhr. 37.3 percent of the supplied oxygen was absorbed.

Power loss is usually determined by reading power gages in the powerhouse. Scott and Wisniewski (S-5) discuss the determination of true power loss. They state that, although the power output is reduced, water is also saved for later generation because of reduced discharge, thus partially offsetting the cost of the immediate power loss. This statement should not be accepted without reservation. It seems incorrect to attempt to justify a reduction in efficiency in this way.

Wisniewski (W-23) reviews the status of stream aeration on three Wisconsin rivers as of 1965. The paper gives an evaluation of capital and operating costs for turbine aeration and suggests that a power loss of about 5 percent should be expected for low-head dams (15 to 25 feet), with less power loss expected for high dams (over 100 feet). As of 1961, 18 dams included turbine aeration. The range of efficiencies was 1.82 to 5.43 lb/kwhr in terms of power loss.

Palladino (P-1) evaluates turbine venting for reaeration of the Kalamazoo River in Michigan. The venting

added 2 lb/kwhr, with initial DO less than 1 mg/l. Actual addition of oxygen was 0.5 mg/l. Noise in the vent indicated undersizing.

Lee (L-9), in a discussion of Wisniewski's paper, describes aeration experiments with Francis turbines at the Wylie Station plant on the Catawba River in South Carolina. He stresses the importance of turbine characteristics, load, wheel setting elevation with respect to tailwater elevation, vacuum breaker arrangement, and draft tube dimensions and shape with regard to the reaeration effectiveness. Bureau of Reclamation experience with draft tube air injection for control of cavitation and surging in high-head installations has shown an increased efficiency. The slight reduction in discharge is more than offset by the effects of smoother operation. Under these circumstances, draft tube aeration could be considered to be a cost-free benefit.

The possibility of using the draft tubes of dormant turbines for reaeration has been considered, with specific reference to equipment which is no longer used because of age. A logical extension to this idea would be the use of turbines for reaeration during offpeak periods. Reaeration benefits would have to be balanced against cost of water loss.

Since most Bureau of Reclamation projects include hydraulic turbines, the writer feels that this method of reaeration should be carefully considered. However, considerable research will be required. The literature, including the references discussed above, does not provide a clear understanding of the advantages and disadvantages of turbine injection, particularly for high-head installations. Also, experience in turbine venting has not been widely published in comparison with diffusers and mechanical aerators. This is probably because of the wide application of the latter methods to waste treatment.

**Hydraulic guns.**—The "Aero-hydraulic gun" is described by Bryan (B-27). The device consists primarily of a vertical pipe, 6 inches to 3-1/2 feet in diameter, into which large bubbles are introduced intermittently and automatically. The bubble completely fills the pipe and discharges water from the top of the pipe as new water is drawn through ports near the bottom of the pipe. The device was first used in ice-prevention and local wave control and in aerobic sewage treatment. Aeration occurs through generation of high-velocity surface currents, transfer from the bubbles, and generation of a surface boil. The design is optimized according to the nature of the requirement. Efficiency with an initial zero DO at 20° C is

approximately 1.6 lb/brake hp at an aeration capacity of 1 lb/hr (1.2 lb/kwhr), depending upon the details of the design and the primary purpose of the installation. The primary effect of the device is in mixing the water body in which it is placed. It is a relatively low-efficiency aerator and thus has questionable value as an instream device.

**U-tubes.**—The development of the U-tube device in the Netherlands was reported by Bruijn and Tuinzaad (B-28) in 1958. Further work has been carried out recently by Speece and reported by Speece and others (S-21, S-23, S-24, S-25, S-26). As the name implies, the device is shaped like a U-tube, in which the water flows downward from the entering channel then upward into the exit channel. The two legs can be formed by placing a vertical baffle in a trench.

The main advantages of the U-tube device are:

1. A high rate of bubble surface renewal resulting from turbulence caused by the buoyant force of the bubble.
2. Longer bubble contact time in the downward leg because of downward flow counteracting the buoyancy of the bubbles.
3. Bubble pressurization with increased saturation concentration, resulting from hydrostatic head.

Air is introduced at the top of the downward leg by a natural drop such as a weir, by a constriction in the flow passage, or by injection from a diffuser. Where head loss can be tolerated, natural entrainment is, of course, preferable.

Speece, et al (S-25) describe small-scale experimental studies. Effects of air-water ratio, velocity, depth, injection depth, bubble size, and internal flow constrictions were evaluated. The pilot system was made of 4-inch-diameter pipe. The study showed that water with initial DO of zero could be completely saturated with one pass through a 40-foot-deep U-tube with air injection of 20 percent of the water volume. The paper states that the transfer economy and capital cost of the U-tube are competitive with conventional aeration systems, which are economical only when reaerating waters with low initial DO. The design of U-tube aeration systems has been discussed in a recent paper by Speece and Orosco (S-26). A design example is given, which includes a cost analysis. The U-tube is considered by the authors to be the best device available for saturating a flow with oxygen, but not necessarily advantageous over mechanical surface aerators when producing 40 to 50 percent saturation.

The writer feels that this device shows promise for application to Bureau of Reclamation problems. However, the U-tube has not yet been used for aeration of large open-channel flows. Therefore, application of the results of the small-scale studies reported in the literature may or may not be appropriate. Consideration should also be given to possible plugging of the device with coarse sediment, weeds, or ice.

*Venturi tubes.*—Bayley and Wyatt (B-8) describe an experimental study in which air was injected at the 3/4-inch-diameter throat of a Venturi section in a 1-1/2-inch-diameter pipe. Oxygen absorption was measured at various airflow rates, for several water discharge rates. DO was zero at the start of each test. Air was admitted naturally as the result of the vacuum at the throat.

The increase in DO varied directly with the ratio of air to water in the system. The presence of air in the Venturi caused an increase in head loss, as compared to the loss with no air present. The loss also increased with increased velocity. The study did not separate these effects.

The maximum transfer efficiency obtained was 850 g/kwhr of energy loss (1.9 lb/kwhr). The maximum efficiency occurred only when the DO absorbed was less than 0.5 ppm. For higher absorptions (and higher velocities) efficiency was reduced because of increased head loss. The paper states that some reduction in efficiency resulted from small bubbles coalescing into large bubbles in the main pipe, thus reducing the bubble surface area.

Additional experiments were performed in which the flow was discharged directly into a tank. The bubbles were thus allowed to rise from the exit of the pipe to the water surface. A maximum efficiency of 1,150 g/kwhr (2.5 lb/kwhr) was obtained with this method.

Addition of detergents resulted in a substantial increase in efficiency, which is in contrast to observations made on diffused air systems. The authors speculate that this is due to an increase in the interfacial area of the rising bubbles, but do not give any confirmation.

More recent experiments were performed by Jackson and Collins (J-2) on two different scales of a Venturi aerator.

The writer feels that this method would be useful only in reaeration of relatively small discharges and volumes, as in waste treatment.

*Pressure injection.*—Thackston and Speece (T-15) review a method in which a small amount of the total water volume is supersaturated with air, under pressure, then released into the main flow. Air comes out of solution and reaerates the rest of the flow. No efficiencies were given.

*Miscellaneous methods.*—Thackston and Speece (T-16) report the use of a siphon which supplies spray nozzles downstream from a dam. Actual amounts of the DO increase were not given. Bulicek (B-30) describes an unsuccessful attempt to save fish by aerating a stream with paddle wheel steamers.

*Hypolimnion reaeration.*—Situations occur in which it is desirable to reaerate the bottom waters of a lake or reservoir without destroying the stratification by mixing. For example, where downstream releases are used for drinking water or maintenance of certain fish life, it is beneficial to release cold water. One obvious way to fill these needs is to selectively withdraw cold water from the reservoir, then reaerate the stream. The devices described thus far generally apply to this approach. Bernhardt (B-15) proposed a method by which reaeration of the hypolimnion could be accomplished within the reservoir without destruction of the thermocline and epilimnion. Efficiency was determined to be 2.1 lb/kwhr. The corresponding transfer efficiency was 50 percent, based on measurement of the oxygen content of the rising bubbles.

The system includes an open-ended vertical pipe which extends from near the bottom of the reservoir to above the water surface. Air is introduced through a diffuser at the bottom of the pipe. Four distribution pipes, branching from the vertical pipe, are located just below the thermocline. The rising air causes the water within the pipe to rise, then flow outward through the distribution pipe. The vertical pipe extends far enough above the surface so that water is unable to overflow at the top.

Bernhardt's paper also includes a short summary table of reoxygenation capacity for several reservoir aeration systems. A condensed version of this table is given below:

Table 1

EFFICIENCIES OF SEVERAL REAERATION DEVICES	
Method	Efficiency (lb/kwhr)
Diffused air, mixing	*0.3-4.3
Mechanical turbine aerators	1.3-5.6
Mechanical pump, mixing	1.0
Aerohydraulic gun	1.4
Hypolimnion aeration and mixing	2.1

\*Transport of water to surface allows atmospheric reaeration in addition to oxygen transfer from bubbles.

*Reaeration by reservoir mixing.*—Improvement of reservoir water quality by artificial destratification, using either compressed air or mechanical pumping, has been described by Symons, et al (S-42—S-49). Before using this approach, the necessity and desirability of destratification must first be determined. In many cases, stratification may be determined to be beneficial; for example, in controlling the temperature of downstream releases. Also, the work described has been limited to relatively small impoundments (less than about 5,000 acre-feet). Energy requirements for mixing large reservoirs might be prohibitive. However, mixing of selected zones of reservoirs might prove to be economically feasible.

A recent paper by Symons, Carswell, and Robeck (S-49) describes test destratification of reservoirs up to 2,900-acre-foot volume using either mechanical or diffused air pumping. Results from one test showed reoxygenation efficiencies of 0.7 lb/kwhr for mechanical pumping and 1.7 lb/kwhr for diffused air pumping.

#### Reaeration with Molecular Oxygen

Molecular oxygen has a solubility in water approximately five times greater than oxygen in equilibrium with air. Therefore, correspondingly smaller amounts of molecular oxygen are required for reaeration. However, molecular (or tonnage) oxygen must be manufactured, and the advantage of less quantity might be offset by higher unit cost. Where dissolved nitrogen might have adverse effects on fish, use of molecular oxygen instead of air should be given special consideration.

Amberg, et al (A-7, A-8, A-9) discuss injection of molecular oxygen into a Pelton turbine. Separate runs were made using air or molecular oxygen. A single vent was placed directly above the runner blade, or a sparge ring above the runner blade was used.

The average results were as follows:

Single vent, air: Initial DO = 8.9 ppm  
Added 0.529 lb oxygen/kwhr  
(0.71 lb/hp-hr) of power loss

Single vent, oxygen: Initial DO = 7.2 ppm  
Added 13.9 lb/kwhr  
(18.6 lb/hp-hr)

Sparge ring, oxygen: Initial DO = 7.8 ppm  
Result not clear

Turbine vibration was noted with the single vent, but not with the sparge ring.

Speece (S-22) discusses several sources of information which indicate absorption efficiencies ranging from 14 to 55 percent for various methods. He suggests that the cost of molecular oxygen depends upon the quantity used and whether the demand is seasonal or continual.

The cost for large quantities used throughout the year is estimated at \$7-8/ton. For a 3-month-per-year operation, the cost might be \$20-60/ton, with the cost proportional to the amount used. About 350 kwhr of power are required to produce 1 ton of oxygen. Speece states that for a year-around usage of 20 tons or more of oxygen per day, it would be economical to place an oxygen plant on the site of use. This reference reviews several theories of oxygen transfer and discusses several methods of introducing pure oxygen to water, including a downflow bubble contact system and injection into penstocks.

With injection into penstocks, the initial bubbles should be sized so that oxygen transfer can be essentially complete before reaching the turbine. Free bubbles can have an adverse effect on turbine operation.

Injection of molecular oxygen bubbles from a diffuser at the bottom of a reservoir has been suggested. The bubbles would be sized so that most of the oxygen transfer would be accomplished within the hypolimnion. Thus, the stratification would not be disturbed.



Use of liquid oxygen (LOX) is being investigated, but has not yet been reported.

Investigations of the use of molecular oxygen for reaeration are relatively recent. This technique should, in the writer's opinion, be investigated thoroughly for possible application to Bureau of Reclamation problems.

#### Overall Comparison of Artificial Reaeration Methods

Efficiencies of several reaeration devices were compared in Table 1. Table 2 summarizes efficiencies (in lb oxygen/kwhr), advantages and disadvantages of the various devices and methods which have been discussed. Obviously, it is difficult or impossible to make an evaluation on the basis of efficiencies alone. The efficiency is strongly dependent upon the initial DO deficit which is not always stated in the references. Also, Table 2 shows that the ranges of efficiencies are quite similar for the various methods.

Therefore, choices must be made on the basis of other factors such as the required application, the advantages and disadvantages of use, first cost, and maintenance cost. Relative costs are indicated under advantages and disadvantages for some of the methods listed in Table 2.

Thackston and Speece (T-15) present a limited comparison of annual costs of reaeration by diffusers, turbine injection, cascade aeration, and mechanical surface aerators. This comparison is given in Table 3.

The cost of turbine aeration assumes an efficiency of 3.5 lb/kwhr and a power value of 1 cent/kwhr. The capital costs for all methods are converted to annual costs by using a 5-percent interest rate and 20-year life. The sources of data are given in (T-15).

Imhoff (I-5) reports the comparative costs of three alternative methods applied to the Ruhr River in Germany:

Mechanical aeration	0.81 DM* for removal of organic pollution of one population equivalent
Turbine aeration	0.22 DM per population equivalent
Treatment plant expansion	4.0 DM per population equivalent

\*German currency 4 DM  $\approx$  \$1.00 U.S.

Mechanical aeration was found to be 3.7 times more costly than turbine aeration (Table 3 shows a factor of 3.1). The marked advantage of instream aeration over treatment plant expansion in this case should be noted.

Krenkel, as part of unpublished seminar notes on reaeration, has provided a summary of costs of aeration systems determined by Bernhardt. This summary is reproduced in Table 4.

Table 4 shows that cascades (constructed only for the reaeration benefit) are not as competitive as suggested by Table 3, due to their relatively low oxygenation capacity. The cascade listed in Table 4 also had a relatively very low first cost. Both Tables 3 and 4 show that turbine aeration is very competitive. Bernhardt's hypolimnion aeration method is the next most competitive of the methods listed in Table 4, followed by floating aerators, U-tubes, turbo oxyders, cascades, and diffusers.

Whipple and Coughlin (W-11), in a recent paper, describe tests on the Passaic River, New Jersey, conducted for the purpose of comparing costs of mechanical aerators and diffusers. The efficiency of the mechanical aerator varied from approximately 2.0 to 3.0 lb/hp-hr (2.7 to 4.0 lb/kwhr), increasing with an increase in stream discharge. The transfer rates of the diffusers were about two-thirds those of the mechanical aerators under comparable conditions. Table 4 indicates similar results.

Complete cost analyses were made for multiple unit installations of either mechanical aerators or diffusers. The total annual costs showed that the mechanical aerators had a marked advantage.

The paper also includes a brief discussion of the possible environmental effects of aeration installations.

#### Other Applications of Reaeration Methods

*Cavitation control.*—In 1963 Robertson (R-9) suggested that the effect of gas or air content on cavitation was the least understood of any of the scaling factors in cavitation testing. There is little evidence that the situation has changed since that time. Robertson's discussion includes the "pseudo-cavitation" which can occur above vapor pressure due to the release of dissolved gases at low pressures.

It is generally accepted that true cavitation results from the growth and collapse of gas nuclei other than free bubbles. The necessary nuclei are believed to originate

Table 2

## OVERALL COMPARISON OF REAERATION METHODS

Device	Efficiency	Advantages	Disadvantages
Diffusers (including reservoir mixing)	2-8 percent (Est. 1-3 lb/kwhr)	Many types available.	Clogging. Requires filtering of air. Relatively low transfer efficiency. High first cost.
Mechanical aerators	2-5 lb/kwhr	Many types available. Natural or forced-air admission. Valves, piping, blowers, etc., are not required.	Swimming hazard. Obstructs channel. High first cost.
Turbine injection	2-6 lb/kwhr (with admission by natural draft)	Natural or forced-air admission. Large discharges. Low first cost, low maintenance cost.	Possible power loss and adverse effects on turbine performance. Restricted to sites with hydroplants.
Venturi tubes	2-3 lb/kwhr	Natural or forced-air admission.	Head loss. Small discharges.
Cascades	Determined from empirical formula (Low, see Table 4).	Maintenance free. Often associated with energy dissipation. Large discharges. No auxiliary equipment required.	Head loss may not be allowable. High first cost. Low transfer efficiency.
U-tubes	1-5 lb/kwhr	Natural or forced air admission. Low maintenance cost. High surface transfer, longer contact time, increased deficit due to pressurization. Can be used in channel.	Not yet proven for large discharges. Possible plugging with debris or ice.
Hydraulic guns	≈2 lb/kwhr	Efficient mixing, high surface currents, surface boil.	Primarily for mixing. Large bubble size, low transfer efficiency.
Pressure injection	No data available.		Small volumes
Fixed-cone valves	No power use or loss is involved.	Associated with required energy dissipation. Large volumes. No auxiliary equipment required.	Requires reservoir releases, which may not be possible.
Mechanical pump mixing	< 1 lb/kwhr	Simple equipment. Minimal maintenance.	Primarily for mixing. Low transfer efficiency. Verified only for relatively small volumes.
Hypolimnion reaeration and mixing	> 2 lb/kwhr	Allows stratification to remain undisturbed.	Relatively low transfer efficiency.
Molecular oxygen	14-55 percent	Can be used with various types of contact devices. High transfer efficiency. No dissolved nitrogen.	High cost of molecular oxygen.

Table 3

[From Ref (T-15)]

## ANNUAL COSTS OF REAERATION\*

Type of cost	Cost for diffused-air aeration (\$)	Cost for turbine aeration (\$)	Cost for cascade aeration (\$)	Cost for mechanical aeration (\$)
Capital cost	39,000	3,000	30,000	50,000
Per year	3,130	240	2,400	4,000
Annual operating cost	5,150	2,570	—	4,500
TOTAL	8,280	2,810	2,400	8,500

\* Conditions for computation are: 10,000 lb oxygen/day/1,000 cfs (16 kg/day/100 cu m/sec) or 1.86 mg/l, for 90 days.

Table 4

COSTS OF APPLIED AERATION SYSTEMS								
	Cascade (weir)	Air hoses (diffusers) Baldeney	Air pipes (diffusers) Lippe	Reservoir circulation	U-tube aerator	Turbine injection system Baldeney	Floating aerator	Turbo oxyder
Oxygenation capacity* (kg/hr)	0.88	28	22	16	4.1	120	41	13
Capital costs (DM) <sup>1</sup>	5,000	66,000	110,000	15,000	16,000	34,000	95,000	44,000
(year of construction)	(1965)	(1965)	(1965)	(1964)	(1958)	(1967)	(1965)	(1967)
Relative capital costs* (DM/kg O <sub>2</sub> /hr)	5,700	2,360	5,000	940	4,000	283	2,300	3,280
Energy consumption* (kwhr/kg O <sub>2</sub> )	0.85 (gravity flow)	***6.60	3.45	2.40	0.67 (gravity flow)	0.98	1.52	2.0
Total costs** (DM/kg O <sub>2</sub> )	0.87 (gravity flow)	0.99	1.05	0.37	0.62 (gravity flow)	0.14	0.51	0.65
Reference	Bock and Schmidt <sup>2</sup> 1965	Imhoff 1968 (I-5)	Londong 1967 (L-16)	Bernhardt 1963 and 1967 (B-15)	Bruijn and Tuinzaad 1958 (B-28)	Imhoff 1968 (I-5)	Imhoff 1968 (I-5)	—

<sup>1</sup>4DM ≈ \$1.00.<sup>2</sup>Exact reference unknown.

\*With 50 percent DO deficit.

\*\*With 50 percent DO deficit, operating 30 days per year, 10-year life, and 0.10 DM/kwhr.

\*\*\*Due to local conditions compressed air with 4.5 kg/cm<sup>2</sup> is used.

in cracks and crevices of construction materials, as explained by Johnson (J-9).

Tullis and Skinner (T-31), in a discussion of cavitation in valves, suggest three possible solutions for controlling cavitation:

1. Eliminating the nuclei or reducing their size.
2. Eliminating the pressure recovery which causes collapse of the cavities.
3. Eliminating the low-pressure zones in which the nuclei grow into vapor cavities.

The third solution is practical and has been used extensively for controlling cavitation in gates and valves, on turbine runners, and in high-velocity chutes and free tunnels. Cavitation is controlled by placing air in the low-pressure zone to raise the pressure above that required for growth of the cavities. Also, cavitation damage is reduced in the pressure recovery zone because of the presence of free air to cushion the effects of cavity collapse.

The preceding discussion leads to the conclusion that dissolved air has no effect on either cavitation or cavitation damage. However, it seems to the writer that the presence of dissolved air could lead to the presence of free air because of dissolution in low-pressure areas of the flow, as in "pseudo-cavitation." Whether this free air would provide protection is not clear. Therefore, it could be concluded that the amount of dissolved air and the conditions in which it exists would determine whether it would be beneficial or deleterious.

Dijkman and Vrengdenhil (D-9) studied the effect of dissolved gas on water-column separation. They assumed that the gas comes out of solution and collects in a single cavity at the top of the pipeline. Upon an increase in pressure, that cavity compresses or collapses. Their mathematical analysis predicts that, in the presence of dissolved gas, the pressure rise after compression of the cavity is lower than that for water without dissolved gas.

Panaioti (P-2), in experiments on a cylindrical profile for application to problems of cavitation in pumps, found that variations in gas content of the water had no practical effect on cavitation.

*Velocity and discharge control.*—Reference (T-3) describes the use of a diffused air curtain for controlling the velocity of flow leaving a treatment

plant grit removal chamber. Such an arrangement can have the dual purpose of reaeration and discharge control.

*Removal of suspended matter.*—Diffused air is used in sewage treatment for the removal of grit (A-2). The air is used to scour organic material from the grit, thus allowing the heavier grit to sink to the floor of the basin for removal. Also, a flotation process is used in which minute air bubbles are used to float suspended solids to the surface (E-10). The liquid is first supersaturated with air, then the pressure is reduced to produce the required small bubbles of free air. A similar process might have application in hydraulic engineering for removal of suspended sediments or other undesirable materials (S-11, S-12).

*Fish control.*—Curtains of diffused air have been used for controlling the movement of fish in the vicinity of separation facilities and fish ladders.

*Ice control.*—Diffused air has been used for some time to prevent ice formation in reservoirs (H-9, L-1, S-17). This is essentially a mixing application, in which warmer water is circulated from the bottom of a body of water to the surface during subfreezing air temperatures.

*Control of surface pollutants.*—The use of air curtains has been proposed for use in blocking the movement of surface pollutants, such as oil slicks (G-10).

*Evaporation control.*—Streif (S-37) proposed using compressed air to bring cold reservoir bottom waters to the surface, thus reducing evaporation losses. A measurable reduction in evaporation is reported by Koberg (K-18).

## INSTRUMENTATION

The Winkler method (-2, H-21) is commonly used for laboratory analysis of dissolved oxygen. Within the past several years, electronic instrumentation has become available for this purpose. As pointed out by Wood (W-25), sensors have the advantages of (1) elimination of preparation and standardization of reagent solution, (2) reduced analysis time, (3) a less tedious method, and (4) excellent correlation with the Winkler method. A wide variety of sensors is available from a number of manufacturers. However, the reader should be cautioned that experience to date has shown that electronic equipment may not maintain calibration over a period of a few days.

## RESEARCH NEEDS

### Reported Research

The review has indicated considerable past research activity in:

- Natural reaeration in streams, reservoirs, and estuaries, including dispersion in streams
- Oxygen depletion by organic decay and nitrification
- Design and performance of diffusers and mechanical aerators for waste treatment applications
- Bubble dynamics
- Mathematical simulation of reaeration and oxygen depletion

Some research has been done concerning:

- Use of diffusers, mechanical aerators, and other devices for reaerating large volumes of water such as for in-stream reaeration and reservoir reaeration and mixing
- Use of molecular oxygen
- Comparative costs of reaeration methods and devices
- Reaeration efficiency of turbine injection
- Effects of air injection on turbine performance
- Air injection for cavitation control, velocity and discharge control, removal of suspended matter, and other miscellaneous applications
- Evaluation of outlet control valves for reaeration capability
- Reoxygenation by photosynthesis
- Reaeration at cascades
- Use of radioactive tracers in field studies
- Development of instrumentation
- Development of U-tube aeration
- Turbulent mixing in surface aeration

### Current Research Activity

Research, as yet unreported, is currently underway in several areas including:

- Natural stream reaeration
- Reaeration by photosynthesis
- Mathematical simulation
- Induced mixing by air
- Field evaluations of reaeration
- Use of molecular oxygen, including liquid oxygen
- Oxygen transfer to water droplets
- Flow surface protection against cavitation
- Diffusion away from free surface

- Nitrogen and ammonia removal
- Design of aeration devices
- Use of radioactive gas tracers in field studies
- Foam separation of suspended materials
- Effects of audio vibrations on oxygen transfer rates
- Ice control
- Aeration with recycled foam
- Concentration of streamflow to mechanical aerators
- Stream oxygen balance
- Removal of metals from acid mine discharge by foam fractionation
- Spraying water into pressurized tank of pure oxygen or air
- Study of nucleus formation in cavitation
- Influence of surface mixing downstream from surface aerators
- Economics of water quality management programs, including reaeration
- Reaeration efficiency of Howell-Bunger valves
- Precipitation of metallic elements

### Suggestions for Future Research

The review has indicated a need for new or additional research in the following areas, in order of their importance:

- Correlation of the reaeration rate constant,  $k_2$ , with flow parameters. A fresh approach appears to be needed.
- Development of a method to determine true efficiency of reaeration devices, perhaps by assignment of a  $k_2$  for each device. Elimination or isolation of factors which modify experimental measurements and cause inaccurate evaluation of actual amount of oxygen added.
- Comparative economic analyses of aeration methods and devices. Development of guidelines to allow comparisons on the basis of cost per unit of dissolved oxygen increase.
- Development of new methods and devices for reaeration. Testing of promising methods and devices developed by others. Continuing review of research activity by others.
- Additional field testing and evaluation of injection of air or oxygen into turbines.
- Evaluation of energy dissipators, gates, and valves for reaeration capability. Field testing of prototype structures.

g. Determination of modifications for existing structures to improve reaeration characteristics. Laboratory and field tests.

h. Study of the effects of dissolved air on cavitation on high-velocity flow surfaces.

i. Development of miscellaneous engineering uses of injection of air into water.





## GLOSSARY OF TERMS

algae—a one-celled photosynthetic microscopic plant.

benthic—refers to the bottom of lakes and reservoirs.

biota—all the living organisms in a given region.

BOD—biochemical oxygen demand, amount of oxygen required for biological oxidation of organic matter.

diffusion—transport due to the difference between true convection and the time average of convection, movement of a species in a mixture from a point of higher concentration to a point of lower concentration.

diffusivity—molecular diffusion coefficient, time rate of diffusion.

dispersion—transport due to variations in longitudinal velocity in a cross section.

dissolved oxygen saturation deficit—the difference between the amount of dissolved oxygen present in a solution at a given temperature and the amount which would be present for a saturated condition at the same temperature.

dystrophic—lakes or reservoirs with very low lime content and very high humus content which often lack nutrients.

epilimnion—the upper layer of a stratified lake or reservoir, from the surface to the thermocline, usually mixed.

eutrophic—having an abundance of aquatic plant growth such as algae due to overenrichment with nutrients such as nitrogen and phosphorus.

hypolimnion—the bottom layer of a stratified lake or reservoir, from the thermocline to the bottom, isolated from surface influence.

isotropic turbulence—statistically independent of the orientation and location of the coordinate axes of velocity measurement.

molecular (tonnage) oxygen—pure oxygen, the molecular state,  $O_2$ .

nitrification—transformation of ammonia nitrogen to nitrates.

oligotrophic—lakes or reservoirs with a small supply of nutrients.

oxygen sag—a curve which depicts the concentration of dissolved oxygen along a stream.

photosynthesis—the natural process by which light and chlorophyll are used by plants to synthesize carbohydrates from  $CO_2$  and water; oxygen is produced in the process.

respiration—process by which living organisms take in oxygen from air or water.

sparge ring—a circular diffuser for the introduction of air into mechanical aerators or hydraulic turbines.

stratification—a vertical variation in temperature, dissolved oxygen, chemicals, turbidity, etc., in a stream, lake, or reservoir.



## DEFINITIONS OF MATHEMATICAL TERMS

a	= coefficient of water quality in weir equations, dimensionless
a	= ratio of bubble or water surface area to liquid volume, $L^{-1}$
A	= bubble or water surface area, $L^2$
A'	= molecular collision factor, $T^{-1}$
b	= coefficient of weir configuration, dimensionless
b	= film thickness, L
C, c	= a constant
C	= concentration, $M/L^3$
C <sub>o</sub>	= initial concentration, $M/L^3$
C <sub>s</sub>	= saturation concentration or solubility, $M/L^3$
C <sub>t</sub>	= concentration at time t, $M/L^3$
$\gamma$	= specific weight, $M/L^3$
d <sub>e</sub>	= equivalent bubble diameter, L
D	= oxygen deficit, $M/L^3$
D'	= bubble diameter, L
D <sub>L</sub>	= longitudinal mixing coefficient, $L^2/T$
D <sub>m</sub> , D <sub>AB</sub>	= molecular diffusion coefficient, $L^2/T$
D <sub>o</sub>	= initial oxygen deficit, $M/L^3$
E	= rate of energy dissipation per unit mass, $L^2/T^3$
E	= diffuser efficiency, percent
E <sub>a</sub>	= energy required by molecule to be included in reaction, $ML^2/T^3$ mole
f	= friction factor, dimensionless
g	= acceleration of gravity, $L/T^2$
G <sub>s</sub>	= airflow, $L^3/T$
h	= weir free fall height, L
H	= depth of flow, L
$\theta$	= temperature correction constant, dimensionless
k	= reaction rate, $T^{-1}$
K <sub>1</sub> or k <sub>1</sub>	= BOD rate constant, $T^{-1}$
K <sub>2</sub> or k <sub>2</sub>	= reaeration rate constant, $T^{-1}$
K <sub>d</sub>	= an exponent, dimensionless
K <sub>L</sub>	= liquid-film coefficient, $L/T$
K <sub>La</sub>	= overall transfer coefficient, $T^{-1}$
L	= liquid film thickness, L
L	= BOD, $M/L^3$
La	= initial BOD, $M/L^3$
m	= mass, M
n	= exponent, function of bubble size, dimensionless
n	= rate of mass transfer, $M/L^2-T$
N	= mechanical aeration efficiency, $M/LFT$
P	= power use, LF
Pe	= Peclet number, dimensionless
q	= transfer rate, $M/T$
r	= ratio of upstream deficit to downstream deficit for weirs, dimensionless
r	= rate of renewal of liquid film, $T^{-1}$
R	= universal gas constant, $ML^2/T^2$ per mole- $^{\circ}K$
Re	= bubble Reynolds number, dimensionless
$\rho$	= mass density, $M/L^3$
Sc	= Schmidt number, dimensionless
Se	= energy gradient, dimensionless
Sh	= Sherwood number, dimensionless
SR	= oxygen supply rate, $M/T$

## DEFINITIONS OF MATHEMATICAL TERMS—Continued

t	= time, T
t'	= time of one cycle of absorption and mixing, T
t <sub>exp</sub>	= time of bubble exposure, T
T	= temperature, degrees
TR	= oxygen transfer rate, M/T
$\bar{u}$	= average velocity, L/T
v	= bubble or liquid velocity, L/T
V	= liquid volume, L <sup>3</sup>
v <sub>t</sub>	= terminal bubble velocity, L/T
$\nu$	= kinematic viscosity, L <sup>2</sup> /T
W	= system capacity, L <sup>3</sup>
W	= mass fraction, dimensionless
x	= distance, L

## **BIBLIOGRAPHY PREFACE**

This bibliography represents a sincere attempt by the writer to prepare a comprehensive list of references on the subject of reeducation. Undoubtedly, some important references have been inadvertently omitted, while some references of questionable value have been included.

Not all of the references were available to the writer for personal review. In some cases, summaries by others were studied and, where appropriate, the information contained therein was included in this report.

The subject index which follows the bibliography was based on abstracts, annotations, or titles of the references wherever possible.



## **BIBLIOGRAPHY**





- |    |   |  |
|----|---|--|
| -1 | <p>Anon<br/> <b>COMPRESSED AIR HANDBOOK</b><br/>           Compressed Air and Gas Institute New York N Y 1947<br/>           Contains data on characteristics of air blowers</p>  | <p><b>EQUIPMENT</b><br/>           diffusers</p>   |
| -2 | <p>Anon<br/> <b>STANDARD METHODS FOR THE EXAMINATION OF WATER AND WASTEWATER</b><br/>           11th Edition American Public Health Assoc New York N Y 1960</p>   | <p><b>DO ANALYSIS</b></p>  |
| -3 | <p>Anon<br/> <b>AERATION OF LARGE VOLUMES OF WATER</b><br/>           Water and Waste Treatment J (Brit) v7 1960 p 508<br/>           Water Pollution Abstracts (Brit) v 34 1961 p 37<br/>           Describes in very general terms a system which injects compressed air into flow pumped from thermal power station cooling water discharge. Supersaturated flow is returned to main flow where surplus air comes out of solution for reaeration of the entire flow</p>  | <p><b>EQUIPMENT</b><br/>           reservoirs<br/>           pressure<br/>           injection</p> |
| -4 | <p>Anon<br/> <b>NEW LIFE FOR POLLUTED SWEDISH LAKES</b><br/>           Water Waste Treatment J v 8 1960 p 65<br/>           Water Pollution Abstracts v 40 1961 p 941<br/>           Reports on using compressed air to destratify polluted Swedish lakes; in 3 weeks oxygen content increased from 0 to 57 percent, new plant life appeared, and the original temperature differential of 12° C disappeared</p>  | <p><b>EQUIPMENT</b><br/>           reservoirs<br/>           diffusers</p>                         |
| -5 | <p>Anon<br/> <b>FLOATING PUMP FIGHTS POLLUTION</b><br/>           Chem Eng v 69 n 17 1962 p 70</p>  | <p><b>EQUIPMENT</b><br/>           reservoirs<br/>           pumps</p>                             |
| -6 | <p>Anon<br/> <b>SWEETENING A SMELLY RIVER WITH OXYGEN</b><br/>           Eng News-Record v 169 n 2 1962 p 42</p>  | <p><b>EQUIPMENT</b><br/>           streams</p>   |
| -7 | <p>Anon<br/> <b>STREAMFLOW REGULATION FOR QUALITY CONTROL</b><br/>           Robert A Taft Sanitary Eng Center Cincinnati Ohio Apr 3-5 1963</p>   | <p><b>BASIC STUDIES</b><br/>           streams<br/>           experimental</p>                     |
| -8 | <p>Anon<br/> <b>REVIEW OF LITERATURE OF 1963-1968 ON WASTEWATER AND WATER POLLUTION CONTROL</b><br/>           Water Pollution Control Federal J<br/>             v 36 n 7 Jul 1964 p 791<br/>             v 37 n 7 Jul 1965 p 887<br/>             v 38 n 7 Jul 1966 p 1049<br/>             v 39 n 7 Jul 1967 p 1049<br/>             v 40 n 6 Jun 1968 p 897<br/>             v 41 n 6 Jun 1969 p 873<br/>           Reviews and separates bibliographies of literature on water pollution; including stream self-purification in relation to oxygen sag</p> | <p><b>GENERAL</b><br/>           reviews</p>   |

- 9 Anon  
LAGOON AERATION SYSTEM BUBBLES AWAY WASTE  
TREATMENT PROBLEMS  
World Construction v 20 n 3 Mar 1967 p 19-21  
Air-Aqua grid system, originally designed for small community treatment plants, was installed in lagoons of Regina, Saskatchewan, plant to eliminate odor problems; in action and performance this system can be compared to fast-moving stream where rolling motion brings oxygen down to bottom water and also brings oxygen-deficient up to surface; installation and general details of system; 30 blowers with 30-hp motors provide air; blowers are mounted on 11-ft concrete piers to prevent movement in winter (EI 1967)
- EQUIPMENT  
waste treatment  
diffusers
- 10 Anon  
OXYGEN SPEEDS UP WASTE TREATMENT  
Ind Eng Chem v 61 n 2, 5-6  
The use of oxygen instead of air to gain maximal efficiency from the activated-sludge process is discussed. Union Carbide is to run a full-scale test for their process at the Batavia, N.Y., sewage works. The same influent stream will feed a normal aeration tank and an aeration tank supplied with oxygen, so that a direct comparison of performance can be made (Publ Wks N Y 1969 v 100 n 3 p 118) (WPA 1625 Aug 1969)
- EQUIPMENT  
waste treatment  
molecular oxygen
- 11 Anon  
SILICONE RUBBER FOR MEMBRANE LUNG  
Nature v 224 n 5217 Oct 1969 p 301-302  
Reports the development of silicone rubber membranes said to have potential applications in oxygenating blood in heart-lung machines, underwater breathing apparatus, and water desalting; membrane has high permeability to gases with a selective permeability to carbon dioxide in solution 12 times greater than for oxygen
- EQUIPMENT  
misc equipment

## A

- |     |   |  |
|-----|---|--|
| A-1 | <p>Adeney, W E Becker, H G<br/> <b>THE DETERMINATION OF THE RATE OF SOLUTION OF<br/>         ATMOSPHERIC NITROGEN AND OXYGEN BY WATER</b><br/>         Philosophical Magazine s 6 v 38 n 225 Sep 1919; v 39 n 232 Apr 1920</p>  | <p><b>BASIC STUDIES</b><br/>         experimental<br/>         reaeration</p>                      |
| A-2 | <p>Albrecht, A E<br/> <b>AERATED GRIT OPERATION DESIGN AND CHAMBER</b><br/>         Water and Sewage Works v 114 n 9 Sep 1967 p 331-335<br/>         Experimental program established to determine satisfactory method for<br/>         controlling grit chamber hydraulics; if properly designed, aerated grit<br/>         chambers will exhibit certain advantages over conventional grit chambers;<br/>         long, narrow chamber design, incorporating longitudinal baffle, was<br/>         developed; this chamber design provides 95 percent removal of 60 mesh grit<br/>         (specific gravity 2.6); organic matter content of this grit would be<br/>         approximately 5 percent (EI 1968)</p>  | <p><b>EQUIPMENT</b><br/>         waste treatment<br/>         misc uses</p>                        |
| A-3 | <p>Albrecht, D<br/> <b>BELUFTUNG DES RUHRWASSERS AM WEHR SPILLENBURG</b><br/>         (Aeration of the Ruhr Water at Spillenburg Weir)<br/>         Die Wasserwirtschaft 1968 Heft 11 In German</p>   | <p><b>EQUIPMENT</b><br/>         streams<br/>         cascades</p>                                 |
| A-4 | <p>Albrecht, Detlef<br/> <b>SCHATZUNG DER SAUERSTOFFZUFUHR WEHRE UND KASKADEN</b><br/>         (Aeration of Water by Weirs and Cascades)<br/>         Wasserwirtschaft v 59 n 11 Nov 1969 p 321-323<br/>         Discusses the use of cascades for artificial aeration and the increase in oxygen<br/>         at existing weirs and cascades In German</p>   | <p><b>EQUIPMENT</b><br/>         streams<br/>         cascades</p>                                 |
| A-5 | <p>Al-Saffar, Adnan Mustafa<br/> <b>EDDY DIFFUSION AND MASS TRANSFER IN OPEN-CHANNEL<br/>         FLOW</b><br/>         PhD Thesis U of Calif Berkeley 1964</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p> |
| A-6 | <p>Amand, M T<br/> <b>PREDICTING DISSOLVED OXYGEN CONCENTRATION IN A<br/>         LAKE COVERED WITH EVAPORATION SUPPRESSANT</b><br/>         J Water Pollution Control Federation v 40 n 11 Nov 1968 p R423-R433<br/>         Diffusion of oxygen from the atmosphere through a monomolecular film of a<br/>         hexadecanol-octadecanol mixture was investigated under quiescent<br/>         conditions. The study revealed that the oxygen-uptake rate of organisms in<br/>         water can be measured and used to predict the lowest dissolved oxygen<br/>         concentration in water during early morning hours when oxygen<br/>         concentration is most critical. Oxygen-transfer rates in distilled water at 21°<br/>         and 36° C treated with a monomolecular film were 74 and 84 percent,<br/>         respectively, of the rates for untreated distilled water. Treated pond water<br/>         containing 194 mg/l dissolved solids showed oxygen-transfer rates of 89.6 and<br/>         92.6 percent at 21° and 36° C, respectively, as compared with untreated<br/>         pond water. An equation for the temperature dependance of rate coefficients<br/>         for treated and untreated water is given. Theoretical and measured values for<br/>         minimum dissolved oxygen agree closely</p> | <p><b>BASIC STUDIES</b><br/>         reservoirs<br/>         reaeration</p>                        |

## A—Continued

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|------|---|--|
| A-7  | <p>Amberg, H R Cormack, L F Funk, W Rosenfeld, A S Blosser, R O<br/> <b>RE-AERATION OF STREAMS WITH MOLECULR OXYGEN</b><br/>         Ind Water Eng v 4 n 2 Feb 1967 p 15-20</p> <p>Artificial stream aeration is a promising method for alleviating critically low dissolved oxygen levels in streams. Stream aeration using air has been studied and used widely, but no experimental work has been reported on the use of tonnage oxygen. Aeration efficiency with air is very poor as the saturation level is approached, and this problem can be overcome by using oxygen. Experiments on the feasibility of using oxygen were conducted at a power turbine at Willamette Falls, Oregon, by venting the turbine with air and oxygen. The first run was with air, and the second with oxygen. Another oxygen trial was made using a multiple-diffuser sparge ring encircling the turbine above the runner blade. Experimental procedures and results are discussed and oxygen stream aeration systems are compared on the bases of efficiencies, costs, and effect on turbine operation</p>  | <p><b>EQUIPMENT</b><br/>         streams<br/>         turbine injection<br/>         molecular oxygen</p>                        |
| A-8  | <p>Amberg, H R and others<br/> <b>STREAM REAERATION USING TONNAGE OXYGEN</b><br/>         presented to the Regional Meeting of the National Council for Stream Improvement Crown Zellerbach Corp Portland Oreg Sep 1967</p> <p>Compared efficiency of injection of air or molecular oxygen above runner blade of Pelton turbine with single vent injection and sparge ring injection. Data on power loss and cost of oxygen are presented. Vibration of turbine resulting from injection is discussed</p>   | <p><b>EQUIPMENT</b><br/>         streams<br/>         turbine injection<br/>         molecular oxygen</p>                        |
| A-9  | <p>Amberg, H R Wise, D W Aspitarte, T R<br/> <b>AERATION OF STREAMS WITH AIR AND MOLECULAR OXYGEN</b><br/>         Tappi v 52 n 10 Oct 1969 pp 1866-71</p> <p>Results are given on full-scale river aeration by two methods (a) release of oxygen into hydroelectric turbines, and (b) diffusion of gaseous oxygen into water under pressure. Oxygen is approximately five times as effective as an equal quantity of air in imparting dissolved oxygen to streams. The authors consider that provided the oxygen is procured at \$30 per ton dissolved oxygen can be added to the water at a total cost of 3 to 4 cents per pound</p>  | <p><b>EQUIPMENT</b><br/>         streams<br/>         turbine injection<br/>         diffusers<br/>         molecular oxygen</p> |
| A-10 | <p>Ambuhl, H<br/> <b>THE PRACTICAL APPLICATION OF THE ELECTROCHEMICAL DETERMINATION OF OXYGEN IN WATER</b><br/>         Schweizerische Zeitschrift fur Hydrol v 22 Fasc 1 1960 p 23-29<br/>         Transl from German USBR No 614</p> <p>A commercial limnological probe was developed for the remote simultaneous determination of temperature, oxygen, and conductivity by electrochemical methods. The fundamentals of electrochemical methods and technical details involved in the selection of instrumentation systems are discussed. Some basic features of the probe include: (1) cable coupling arrangement to make possible the use of cables of different lengths; (2) temperature measurements made with a thermistor sensor and an alternating-current-powered Wheatstone bridge; (3) simultaneous determination of resistivity and conductivity. Conductivity is measured directly by rearranging bridge members and measuring the reciprocal resistance. Conductivity may be measured continuously, but temperature effects must be compensated. Automatic temperature compensation is technically feasible, but is presently uneconomical; and (4) measurement of high and low oxygen contents. Low oxygen contents are determined by measuring only the diffusion currents at</p> | <p><b>DO ANALYSIS</b><br/>         instrumentation</p>   |

**A—Continued**

the electrodes. High oxygen contents are determined potentiometrically by supplying an auxiliary voltage to the electrodes. The step-by-step operation of the instrument is covered in detail

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| A-11 | <p>Anderson, C A<br/> AERATION RECOVERY OF LANOLIN FROM WOOL SCOUR<br/> LIQUOR<br/> Textile Res J v 30 1960 p 51-57<br/> Investigation of the aeration process has resulted in an improved design for a continuous recovery plant. On a pilot scale the design has permitted throughput rates about 2-1/2 times greater than previous designs, with equal recovery efficiencies. (Livengood-N C) W69-10286</p>   | <p>EQUIPMENT<br/> waste treatment</p>                  |
| A-12 | <p>Angelino, H<br/> HYDRODYNAMIQUE DES GROSSES BULLES DANS LES<br/> LIQUIDES VISQUEUX<br/> Chem Eng Sci v 21 n 6-7 Jun-Jul 1966 p 541-550<br/> Hydrodynamics of large bubbles in viscous liquids; with four columns of diameter between 10 and 40 cm, it has been possible to make systematic study of rising motion of air bubbles of various volume through liquids of different viscosity; evolution of bubble's shape with increasing volume is studied, and relation between frontal diameter and volume is proposed; study is made of influence upon velocity of ascension of proximity of walls. 28 refs. In French (EI 1967)</p> | <p>EQUIPMENT<br/> diffusers</p>                        |
| A-13 | <p>Aris, R<br/> ON THE DISPERSION OF A SOLUTE IN A FLUID<br/> FLOWING THROUGH A TUBE<br/> Proc Royal Society of London v 235A 1956 p 67</p>  | <p>BASIC STUDIES<br/> experimental<br/> reaeration</p> |

## B

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| B-1 | <p>Baars, J K Muskat, J<br/> <b>OXYGENATION OF WATER BY BLADED ROTORS</b><br/>         J and Proc Inst Sewage Purif (Brit) pt 5 1963 p 454</p>   | <p><b>EQUIPMENT</b><br/>         waste treatment<br/>         mechanical<br/>         aerators</p>                              |
| B-2 | <p>Bain, Richard C Jr<br/> <b>PREDICTING DO VARIATIONS CAUSED BY ALGAE</b><br/>         Proc ASCE V 94 n SA 5 1968 p 867-881<br/>         Eutrophic environments are often dominated by planktonic algal populations (phytoplankton) which can cause diurnal variations in DO concentrations through respiratory activity and photosynthesis. Photosynthetic oxygenation and respiratory deoxygenation rates of estuarine phytoplankton were measured at various standing crop (chlorophyll) levels. Oxygen production and consumption rates for actively growing phytoplankton populations were related to standing crop at 20° C and nonlimiting light. Variations in algal photosynthetic production rate, as related to light adaption, age of cells, nutrition, temperature, and algal type, are considered. The Streeter-Phelps equation was modified to include phytoplankton production and respiration rates in formulations designed to predict DO concentrations over a 24-hr period. An example is given and the resulting predictions are compared with field measurements from a tidal reach of the San Joaquin River, Calif</p> | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         photosynthesis<br/>         respiration</p> |
| B-3 | <p>Barkov, N K<br/> <b>VPUSK SZHATOGO VOZDUKHA V ZONU RABOCHEGO KOLESA<br/>         PRI NESPOKOINOM REZHIME RABOTY RADIAL'NO-OSEVOI<br/>         GIDROTURBINY</b><br/>         Energomashinostroenie n 4 Apr 1968 p 39-40<br/>         Injection of compressed air into runner section during perturbed operation of radial-axial hydraulic turbine; results are reported of experiments performed on turbine provided with system of 12 pipes, 50-mm diameter radially disposed on turbine hood and connected to 49-cu-m air receiver; compressed air at 5 to 8 atm pressure was injected under hood; ratio between air and water flow rate was 0.0462; besides effecting quiet operation of turbine, air injection reduced considerably blade area subject to cavitating erosion and increased service life of blades. In Russian (EI 1968)</p>  | <p><b>EQUIPMENT</b><br/>         streams<br/>         turbine injection</p>   |
| B-4 | <p>Barnhart, Edwin L<br/> <b>TRANSFER OF OXYGEN IN AQUEOUS SOLUTIONS</b><br/>         Proc ASCE v 95 n SA 3 Jun 1969 p 645-661<br/>         The paper reports the results of studies which describe the influence of geometry and temperature on the liquid film coefficient, <math>K_L</math>, and the mass transfer coefficient, <math>K_L a</math>, for the transfer of oxygen from air bubbles rising in a liquid. It is shown that the liquid film coefficient is related to the total drag force operating at the liquid gas interface. The influence of several surface active agents on <math>K_L a</math> and <math>K_L</math> are reported. The study indicates that at low concentrations, the principle influence of surface active agents is their effect on the bubble size and rate of rise</p>   | <p><b>BASIC STUDIES</b><br/>         experimental<br/>         reaeration</p>   |
| B-5 | <p>Barrett, M J Gameson, A L H Ogden, C G<br/> <b>AERATION STUDIES AT FOUR WEIR SYSTEMS</b><br/>         Water and Water Eng (Brit) v 64 1960 p 407<br/>         Data from four weir systems with discharges from 1 to 500 mgd were used to verify an empirically derived predictive equation. Discusses effect of weir configuration (steps vs free weirs)</p>  | <p><b>EQUIPMENT</b><br/>         streams<br/>         cascades</p>  |

## B—Continued

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| B-6  | <p>Bartsch, A F<br/> <b>ALGAE AS A SOURCE OF OXYGEN IN WASTE TREATMENT</b><br/> Sewage and Ind Wastes v 33 1961 p 239-249</p>  | <p><b>BASIC STUDIES</b><br/> experimental<br/> photosynthesis</p>                  |
| B-7  | <p>Batchelor, G K<br/> <b>TURBULENT DIFFUSION</b><br/> Lecture Series No. 4 U of Maryland College Park 1960</p>  | <p><b>BASIC STUDIES</b></p>  |
| B-8  | <p>Bayley, R W Wyatt, K<br/> <b>AERATION OF EFFLUENTS BY VENTURI TUBE</b><br/> Water and Waste Treatment J Nov-Dec 1961<br/> Laboratory tests show effective aeration can be achieved by a Venturi tube by air bubbles introduced through holes in the throat of the Venturi; however predictions on performance of a full-size unit are not made because of other important factors</p>   | <p><b>EQUIPMENT</b><br/> Venturis</p>  |
| B-9  | <p>Beck, A J<br/> <b>DIFFUSER PLATE STUDIES</b><br/> Sewage Works J 8 1936 p 22</p>  | <p><b>EQUIPMENT</b><br/> waste treatment<br/> diffusers</p>                        |
| B-10 | <p>Becker, H G<br/> <b>MECHANISM OF ABSORPTION OF MODERATELY SOLUBLE GASES IN WATER</b><br/> Ind Eng Chem v 16 1924 p 1220</p>   | <p><b>BASIC STUDIES</b><br/> reaeration</p>  |
| B-11 | <p>Bella, D A Dobbins, W E<br/> <b>DIFFERENCE MODELING OF STREAM POLLUTION</b><br/> Proc ASCE v 94 n SA 5 1968 p 995</p>   | <p><b>BASIC STUDIES</b><br/> streams<br/> theoretical</p>                          |
| B-12 | <p>Benjes, Henry H Jr McKinney, Ross E<br/> <b>SPECIFYING AND EVALUATING AERATION EQUIPMENT</b><br/> Proc ASCE v 93 n SA 6 Dec 1967 p 55-64<br/> One of the most complex aspects of designing a modern activated sludge waste water treatment system is concerned with the selection of optimum aeration equipment. A performance evaluation for initial operating conditions has been developed which can be extrapolated to the design operating conditions. The performance evaluation requires determination of operating air-flow rates, temperature, mixed liquor suspended solids, oxygen demand rates, and dissolved oxygen. The application of the performance evaluation technique to the aeration equipment furnished for the Grand Island, Nebr., activated sludge plant is described. The experience obtained from the performance evaluation at Grand Island has pointed to certain necessary refinements in the evaluation technique. A sample aeration equipment performance specification is appended incorporating these refinements</p> | <p><b>EQUIPMENT</b><br/> waste treatment</p>                                       |
| B-13 | <p>Bennett, G F Kempe, L L<br/> <b>OXYGEN TRANSFER IN BIOLOGICAL SYSTEMS</b><br/> PURDUE U—Eng Extension Ser v 118 1965 p 435-449<br/> Oxygen transfer rate in unsparged, but agitated system is shown less than rate in system that is both sparged and agitated simultaneously; differences between these measurements increase as gas-liquid interface or partial pressure of oxygen in gas is increased; data suggest two parallel paths for oxygen transfer from air to cell; in unsparged liquid, microorganism has available only oxygen dissolved in liquid; in sparged system, some cells adsorb</p>  | <p><b>BASIC STUDIES</b><br/> waste treatment<br/> experimental<br/> reaeration</p> |

## B—Continued

on air bubbles, or air bubbles adsorb on cells; by this process, some resistance to oxygen transfer is promoted. 43 refs (EI 1967)

- B-14 Bernhart, A P  
POWER OF SELF-PURIFICATION IN RIVERS EXEMPLIFIED  
BY TORONTO'S DON RIVER  
Eng J v 48 n 2 Feb 1965 p 31-34  
Water recovery in upper Don after pollution shock is indicated by fast reduction BOD, phosphates and coli bacteria as well as by increase in dissolved oxygen; lighter water color, improved conditions of streambed and reappearance of higher organisms also indicate strong self-purification (EI 1965)
- B-15 Bernhardt, H  
AERATION OF WAHNBACH RESERVOIR WITHOUT CHANGING  
TEMPERATURE PROFILE  
American Water Works Assoc J v 59 n 8 Aug 1967 p 943-964  
Results of aeration tests on reservoir in Siegburg, West Germany, which contains 33,740 acre-ft, has maximum depth of 141 ft, with its surface 410 ft above sea level, are reported; tests showed among other things that aeration and mixing of impoundment are feasible and that complete destratification by diffused air bubble method and aeration of hypolimnion only both had favorable effect on water quality, but aeration of hypolimnion had additional advantage of preserving quantity of cold water for use as drinking water. 26 refs (EI 1967)
- B-16 Beuthe, C G  
IMPROVEMENTS IN FINE-BUBBLE AERATION FROM THE  
STANDPOINTS OF TECHNIQUE AND OPERATION  
Water Pollution Control London v 68 1969 p 51-58  
The mathematical relations for activated-sludge tanks operating as homogeneous and heterogeneous reactors and with constant hydraulic loading (see Water Pollution Abstracts v 41 n 1649 1968) were tested by observing the performance of two plants equipped with tubular diffusers. The results indicate that for maximal efficiency an aeration tank should have longitudinal flow, constant sludge loading, and tapered aeration. The advantages of fine-bubble aeration by tubular diffusers over surface aeration are indicated (WPA 1382 Jul 1969)
- B-17 Bewtra, J K Nicholas, W R  
BASIC VARIABLES OF OXYGENATION FROM DIFFUSED  
AIR AERATION TANKS  
presented at the 17th Annual Purdue Ind Wastes Conf 1962
- B-18 Bewtra, J K Nicholas, W R  
OXYGENATION FROM DIFFUSED AIR IN AERATION  
TANKS  
Water Pollution Control Federation J v 36 n 10 Oct 1964 p 1195-1224  
Oxygen transfer studies conducted in 4-ft-long section of full-scale aeration tank at Philip F. Morgan Sanitary Engineering Laboratory, State University of Iowa; variables of oxygen transfer from air to water were studied; variables are presented mathematically and their relative importance is discussed; development of oxygen transfer equation; effect of diffuser submergence on oxygenation; effect of aeration tank width on oxygenation. 24 refs (EI 1965)
- BASIC STUDIES  
streams  
experimental  
reaeration
- EQUIPMENT  
reservoirs  
diffusers
- EQUIPMENT  
waste treatment  
diffusers
- EQUIPMENT  
waste treatment  
diffusers



## B—Continued

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|------|---|--|
| B-19 | Bird, R B Stewart, W E Lightfoot, E N<br>TRANSPORT PHENOMENA<br>John Wiley and Sons, Inc N Y 1960   | GENERAL  |
| B-20 | Bischofsberger Tofaute<br>POROUS PLASTICS FOR FINE BUBBLE AERATION OF<br>WASTE WATERS<br>Tech Scientific Reports of the Ems Federation and the Lippe Assoc v 6 1964<br>p 26-43  | EQUIPMENT<br>waste treatment<br>diffusers              |
| B-21 | Black, S A<br>SUPPLEMENTARY AERATION OF WASTE STABILIZATION<br>PONDS FOR INDUSTRIAL WASTES<br>Water and Pollution Control v 105 n 1 Jan 1968 p 30-31<br>Raw industrial and domestic wastes were contained in stabilization pond for<br>treatment and used for operational and performance data collection and<br>evaluation when aerated by surface mechanical-aeration device; method of<br>study and results obtained; steps are suggested for effective treatment of<br>waste (EI 1967)  | EQUIPMENT<br>waste treatment<br>mechanical<br>aerators |
| B-22 | Black, S A<br>CAN AERATION PONDS POLISH SEWAGE PLANT EFFLUENT<br>Water and Pollution Control v 105 n 6 Jun 1967 p 38, 40, 42<br>Effluent polishing pilot plant study was performed to evaluate polishing<br>processes suitable to provide additional treatment to secondary treatment<br>plant effluents in Ontario; pilot plant consisted of aeration pond and settling<br>lagoon coupled in series; from study it was concluded that if certain design<br>and operational requirements are met, effluent with BOD and suspended<br>solids content not exceeding 8 ppm may be maintained by aeration pond;<br>aeration pond should be followed by settling lagoon of 1 to 2 days' retention<br>to raise dissolved oxygen of effluent to 4 ppm before its introduction to<br>receiving stream (EI 1967) | EQUIPMENT<br>waste treatment                           |
| B-23 | Blain, W A McDonnel, A J<br>REAERATION MEASUREMENTS IN A EUTROPHIC STREAM<br>Proc 22nd Int Waste Conf Purdue U Ext Ser 129 1968 p 1044  | BASIC STUDIES<br>streams<br>experimental<br>reaeration |
| B-24 | Blodgett, J H<br>AIR DIFFUSION WITH SARAN-WRAPPED TUBES<br>Sewage and Ind Wastes v 22 1950 p 1290   | EQUIPMENT<br>waste treatment<br>diffusers              |
| B-25 | Bohnke, B<br>EFFECTS OF ORGANIC WASTEWATER AND COOLING WATER<br>ON SELF-PURIFICATION OF WATERS<br>Proc 22nd Ind Waste Conf Purdue U Ext Ser 129 1968 p 752  | BASIC STUDIES<br>streams<br>experimental<br>reaeration |
| B-26 | Browning, Jon E<br>O <sub>2</sub> & O <sub>3</sub> —RX FOR POLLUTION?<br>Chem Eng v 77 n 4 Feb 23 1970 p 46-48<br>New oxygenation and ozonation processes look promising for waste<br>treatment and water purification; gives brief descriptions and some costs for<br>Linde's oxygenation municipal sewage treatment plant at Ratavia, N. Y.; Air<br>Reduction Co.'s ozone system for tertiary waste treatment; Crown  | EQUIPMENT<br>waste treatment                           |

## B—Continued

Zellerbach's oxygenation system for a paper mill at Bogalusa, La.; and  
Container Corp.'s oxygenation of paper mill waste water at Brewton, Ala

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| B-27 | <p>Bryan, J G<br/>IMPROVEMENT IN THE QUALITY OF RESERVOIR DISCHARGES<br/>THROUGH RESERVOIR MIXING AND AERATION<br/>U S Dept Health Education Welfare Symposium on Streamflow Regulation for<br/>Quality Control Public Health Service Pub No 999-WP-30 Jun 1965 p 317-344<br/>Describes the aerohydraulic gun and the aeration capacity and mixing<br/>produced by these guns. Examples of practical applications are given at<br/>Blelham Tarn, Inniscarra Reservoir, and Lock Turret Reservoir</p>   | <p>EQUIPMENT<br/>reservoirs<br/>hydraulic guns</p>          |
| B-28 | <p>Bruijn, Jacob Tuinzaad, Hendrick<br/>THE RELATIONSHIP BETWEEN DEPTH OF U-TUBES AND<br/>THE AERATION PROCESS<br/>J American Water Works Assoc Jul 1958 p 879<br/>Reports original development of U-tube oxygenation method and describes<br/>prototype installation</p>  | <p>EQUIPMENT<br/>streams<br/>U-tubes</p>                    |
| B-29 | <p>Bryson, R A Sumoi, V E<br/>MIDSUMMER RENEWAL OF OXYGEN WITHIN THE<br/>HYPOLIMNION<br/>J Marine Research v 10 1951 p 263-269</p>   | <p>EQUIPMENT<br/>reservoirs</p>                             |
| B-30 | <p>Bulicek, J<br/>ARTIFICIAL AERATION OF WATER IN THE MOLDAU<br/>IMPOUNDING RESERVOIRS AND IN CZECHOSLOVAKIA<br/>Vodn Hospod v 9 1957 Czech<br/>Wasserwirtschaft (Stuttgart) v 49 1959 p 25<br/>Water Pollution Abstracts v 40 1960 p 1910<br/>Describes an unsuccessful attempt to save fish by aerating water with<br/>paddle-wheel steamers</p>   | <p>EQUIPMENT<br/>streams<br/>mechanical<br/>aerators</p>    |
| B-31 | <p>Burdick, M E<br/>OPEN WATER IN WINTER<br/>Wisconsin Conservation Bull v 24 1959 p 21<br/>Reports on compressed air mixing of lakes to prevent winterkill of fish when<br/>the lake freezes over and cuts off the oxygen supply</p>  | <p>EQUIPMENT<br/>reservoirs<br/>diffusers<br/>misc uses</p> |
| B-32 | <p>Burns, O B Jr Eckenfelder, W W Jr<br/>AERATION IMPROVEMENTS AND ADAPTION OF COOLING<br/>TOWER TO ACTIVATED SLUDGE PLANT<br/>Tappi v 48 n 11 Nov 1965 p 96A-99A<br/>Problems associated with high temperature of waste effluent during summer<br/>and inadequate aeration capacity were solved by installation of counter-flow<br/>cooling tower and by modification of aeration tanks; by these changes, plant<br/>overall efficiency is maintained in range from 85 to 90 percent and average<br/>final effluent BOD is improved from 43.9 to 25.4 ppm (EI 1966)</p> | <p>EQUIPMENT<br/>waste treatment</p>                        |

## B—Continued

- B-33 Burns, O B Jr St. John, J P O'Connor, D J  
PILOT MECHANICAL AERATION STUDIES OF THE  
JACKSON RIVER IN COVINGTON, VIRGINIA  
Proc 21st Ind Waste Conf Purdue U Ext Ser 121 1966 p 799  
Describes use of plate-type surface aerator placed at location of minimum DO in stream. Efficiency of 2.15 lb oxygen/hp-hr for 100-percent DO deficit. Discussion of paper describes German use of floating surface aerators (1.75 lb oxygen/kwhr at 50-percent deficit), diffuser (5-percent efficiency at 50-percent deficit), and injection above runner of hydroturbine (efficiency not given)
- B-34 Burrows, M G  
INHIBITION OF AERATION PROCESS: QUANTITATIVE  
ASSESSMENT OF SOME TOXIC MATERIALS  
Water Pollution Control v 68 n 4 1969 p 457  
The cost of treating industrial effluents containing inhibitors can be evaluated by using a laboratory activated sludge apparatus consisting of a set of aeration tanks into which a 30:20 effluent is added as control and, in other tanks, settled sewage containing 2 mg/l of various inhibitors fed. After daily aeration cycles had been carried out for a week, the supernatant liquor was sampled and analyzed and performance evaluated in each case. The inhibitory effects of various metals and cyanide were tabulated
- B-35 Butts, T A Schnepfer, D H  
OXYGEN ABSORPTION IN STREAMS  
Water and Sewage Works v 114 1967 p 385
- EQUIPMENT  
streams  
mechanical  
aerators  
diffusers  
turbine injection
- BASIC STUDIES  
waste treatment  
experimental
- BASIC STUDIES  
streams  
experimental  
reaeration

## C

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| C-1 | <p>Cable, M<br/> <b>DISSOLVING OF STATIONARY GAS BUBBLES IN LIQUID</b><br/>         Chem Eng Sci v 22 n 11 Nov 1967 p 1393-1398<br/>         Theoretical interpretation of dissolving of gas bubbles in liquids has usually been based on model which ignores effect of motion of liquid on concentration field and predicts linear relation between square of size and time; experimental data plotted in this way often show decrease in slope; theoretical results are now available which take radial motion of liquid into account; these show that decrease in slope is in accordance with theory; some experimental results are in good agreement with theory, but others show marked deviations; possible reasons for these deviations are discussed. 22 refs (EI 1968)</p>  | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         theoretical<br/>         experimental<br/>         reaeration</p>    |
| C-2 | <p>Cadwallader, E Thomas McDonnell, J Archie<br/> <b>A MULTIVARIATE ANALYSIS OF REAERATION DATA</b><br/>         Water Research Pergamon Press v 3 1969 p 731-742<br/>         Describes the application of the statistical technique of multivariate analysis to two sets of prototype reaeration data and one set of laboratory data, and to a combined set. The exchange coefficient was found to be consistently defined by the rate of energy dissipation (E) for values of <math>E &gt; 0.001 \text{ ft}^2/\text{sec}^3</math>. For <math>E &lt; 0.001</math> factors related to molecular diffusion are controlling</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p>                             |
| C-3 | <p>Camp, Thomas R<br/> <b>FIELD ESTIMATES OF OXYGEN BALANCE PARAMETERS</b><br/>         Proc ASCE v 91 n SA 5 Oct 1965 p 1-17<br/>         Field studies of oxygen balance in Merrimack River, Mass; Streeter-Phelps equations, extended to include addition of BOD from bottom deposits, removal of BOD by settling, production of dissolved oxygen by photosynthesis, and longitudinal mixing by tides, indicated 50 to 80 percent of BOD by settling and approximately two-thirds of oxygen furnished by algae in photosynthesis; atmospheric reaeration rate constant was found to be considerably less than expected; algae was found to be essential to pollution control</p>  | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration<br/>         photosynthesis</p> |
| C-4 | <p>Carver, C E Jr<br/> <b>ABSORPTION OF OXYGEN IN BUBBLE AERATION</b><br/>         Biological Treatment of Sewage and Ind Wastes v 1 1955</p>  | <p><b>EQUIPMENT</b><br/>         waste treatment<br/>         diffusers</p>  |
| C-5 | <p>Carver, C E Jr<br/> <b>OXYGEN TRANSFER FROM FALLING WATER DROPLETS</b><br/>         Proc ASCE v 95 n SA 2 Apr 1969 p 239-251<br/>         Overall oxygen transfer coefficients are obtained for deaerated water droplets falling freely through the atmosphere with and without 50 ppm of a synthetic detergent. Drop distances ranged from 0 to 13 ft, and droplet surface areas varied from 0.47 to 0.55 <math>\text{cm}^2</math>. Transfer coefficients are found to decrease somewhat with increasing droplet size, becoming independent of droplet size above 6.0 ppm of DO. With detergent present, the coefficients are reduced approximately 50 percent. Experiments were also performed with fully aerated water droplets falling freely through a nitrogen atmosphere. For this case, droplet surface area ranged from 0.15 to 0.50 <math>\text{cm}^2</math>. Transfer coefficients are found to increase with increasing droplet size. Although no direct comparison of droplet sizes could be made, it is concluded that the rate of oxygen transfer for both inward and outward transfer from a droplet is not substantially different</p> | <p><b>BASIC STUDIES</b><br/>         experimental<br/>         reaeration</p>  |

## C—Continued

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| C-6  | <p>Chasick, A H Bootes, R L<br/> <b>DETERMINING THE EFFICIENCY OF AIR FILTERS</b><br/>         Water Works and Wastes Eng v 1 n 1 1965 p 50</p>  | <p><b>EQUIPMENT</b><br/>         waste treatment<br/>         diffusers</p>  |
| C-7  | <p>Chernykh, E M<br/> <b>O NEUSTOICHIVOSTI SFERICHESKOGO GAZOVOGO<br/>         PUZYRAYA V POLE PEREMENNOGO DAVLENIYA</b><br/>         Akademiya Nauk Izvestiya Mekhanika Zhidkosti i Gaza n 1 Jan-Feb 1967<br/>         p 38-42<br/>         Instability of spherical gas bubble in variable pressure field; stability of radial motion of bubble boundary in incompressible nonviscous liquid is investigated for case of variable external pressure; possibility of steady motion existence is investigated for case of monotonic and periodic time functions of external pressure; it is proved that stability is only possible for infinitely large radii of bubble, or under very particular assumptions regarding initial conditions and pressure variations. In Russian (EI 1967)</p> | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         theoretical</p>  |
| C-8  | <p>Churchill, M A<br/> <b>EFFECT OF DENSITY CURRENTS UPON RAW WATER<br/>         QUALITY</b><br/>         J American Water Works Assoc v 39 n 4 1947 p 357-360</p>   | <p><b>BASIC STUDIES</b><br/>         reservoirs<br/>         experimental<br/>         reaeration<br/>         oxidation</p> |
| C-9  | <p>Churchill, M A Buckingham, R A<br/> <b>STATISTICAL METHOD FOR ANALYSIS OF STREAM<br/>         PURIFICATION CAPACITY</b><br/>         Sewage and Ind Wastes v 28 Apr 1956</p>  | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p>                           |
| C-10 | <p>Churchill, M A<br/> <b>EFFECTS OF STORAGE IMPOUNDMENTS ON WATER QUALITY</b><br/>         Proc ASCE v 83 n SA 1 Feb 1957<br/>         Discusses thermal stratification and effects on dissolved oxygen</p>   | <p><b>BASIC STUDIES</b><br/>         reservoirs<br/>         experimental<br/>         reaeration<br/>         oxidation</p> |
| C-11 | <p>Churchill, M A<br/> <b>EFFECT OF WATER TEMPERATURE ON STREAM<br/>         REAERATION</b><br/>         Proc ASCE v 87 n SA 6 1961 p 59</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p>                           |
| C-12 | <p>Churchill, M A Buckingham, R A Elmore, H L<br/> <b>PREDICTION OF STREAM REAERATION RATES</b><br/>         Proc ASCE v 88 n SA 4 Jul 1962 p 1-46<br/>         Results are given of many field measurements of actual rates at which river water that is low in dissolved oxygen, but free of organic pollution, absorbs oxygen from atmosphere; by using dimensional analysis and multiple-regression techniques, observed reaeration rates have been related to hydraulic properties of river channels; several reaeration formulas thus developed can be used to predict accurately rate at which oxygen will be absorbed by water flowing in natural stream channels</p>  | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p>                           |

## C—Continued

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| C-13 | <p>Churchill, M A Nicholas, W R<br/> <b>EFFECTS OF IMPOUNDMENTS ON WATER QUALITY</b><br/>         National Symposium on Quality Standards for Natural Waters Ann Arbor Mich<br/>         Paper 2P1-1 Jul 1966</p> <p>Results of selected studies of the quality of water flowing through large main river reservoirs in the Tennessee Valley are discussed. Selected data on the quality of water found in certain upstream storage reservoirs—primarily Gunterville, Wheeler, and Pickwick—are also presented. A beginning is made on the difficult job of predicting concentrations of DO in water released through low-level outlets from large storage impoundments. These first attempts are discussed and given an indication of the direction in which current studies are progressing. A preliminary DO prediction equation is given. As more data become available, the equation will be expanded to consider several pertinent water quality factors (biochemical oxygen demand, chemical oxygen demand, and nutrients) in the reservoir inflow, thus permitting more accurate predictions to be made for reservoir project design, operation, and water quality conditions</p>   | <p><b>BASIC STUDIES</b><br/>         reservoirs<br/>         experimental<br/>         reaeration<br/>         oxidation</p> |
| C-14 | <p>Churchill, M A Nicholas, W R<br/> <b>EFFECTS OF IMPOUNDMENTS ON WATER QUALITY</b><br/>         Proc ASCE v 93 n SA 6 Dec 1967 p 73-90</p> <p>Changes occurring in the quality of water during its passage through Tennessee River reservoirs and during lengthy storage in tributary impoundments are observed. Seasonal variations of temperatures of water discharged from main-river impoundments are discussed. DO concentrations in the water discharged from main-river reservoirs recede during the summer months but do not reach the low concentrations observed below storage impoundments. Both total coliform and fecal coliform concentrations in main stream reservoirs increase greatly below local municipalities. In tributary storage impoundments strong thermoclines develop in early spring, and relatively cool water, low in DO, is discharged through low-level power intakes well into or throughout the summer. Low DO concentrations are also caused by biological activity in eutrophic impoundments, inflow to which are otherwise relatively free of pollution. A multiple regression technique is used to develop an equation for predicting DO concentrations to be expected in releases from a proposed impoundment</p> | <p><b>BASIC STUDIES</b><br/>         reservoirs<br/>         experimental<br/>         reaeration<br/>         oxidation</p> |
| C-15 | <p>Clair, William F Beck, John D<br/> <b>PITTSBURG GIVES ITS WATER THE AIR</b><br/>         Water and Waste Eng Jun 1969</p> <p>Describes the Air-Aqua Turnover System installed on Pittsburg water supply reservoirs and results of aeration</p>   | <p><b>EQUIPMENT</b><br/>         reservoirs<br/>         diffusers</p>   |
| C-16 | <p>Cleary, E J<br/> <b>THE REAERATION OF RIVERS</b><br/>         Ind Water Eng Jun 1966 p 16-21</p>   | <p><b>EQUIPMENT</b><br/>         streams</p>   |
| C-17 | <p>Cleasby, J L Baumann, E R<br/> <b>OXYGENATION EFFICIENCY OF BLADED ROTOR</b><br/>         Water Pollution Control Federation J v 40 n 3 pt 1 Mar 1968 p 412-424</p> <p>Oxygen transfer data for bladed-rotor mechanical aerator are presented and factors affecting oxygen transfer are discussed; test apparatus is examined; method used for efficiency determination is demonstrated by examples; included are results of 45 experimental runs plus comparison of diffused air</p>  | <p><b>EQUIPMENT</b><br/>         mechanical<br/>         aerators</p>  |

## C—Continued

and mechanical aeration, showing rotor studied to be more efficient than hypothetical diffuser. 18 refs (EI 1968)

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| C-18 | <p>Cole, R<br/> <b>MOTION OF VAPOR BUBBLES IN SATURATED LIQUIDS</b><br/> <i>AIChE J</i> v 13 n 2 Mar 1967 p 403-404<br/>           Data for vapor bubbles rising through saturated liquids have been obtained experimentally for variety of liquids under pressures ranging from 48 to 540 mm Hg; equivalent diameters of these bubbles ranged from 0.1 to 1.3 cm and thus cover precisely region in which H. D. Mendelson's analysis should be applicable; although considerable scatter of data is evident, it is apparent that mean of data is in agreement with Mendelson's analysis. 4 refs (EI 1967)</p>   | <p><b>BASIC STUDIES</b><br/>           bubbles<br/>           experimental</p>    |
| C-19 | <p>Collins, R<br/> <b>SIMPLE MODEL OF PLANE GAS BUBBLE IN FINITE LIQUID</b><br/> <i>J Fluid Mechanics</i> v 22 pt 4 Aug 1965 p 761-763<br/>           Study of large gas bubbles rising in liquids has been stimulated by analogy that bubble rising in bed of solid particles fluidized by vertical flow of gas through it, appears to behave like gas bubble rising in liquid; using method due to Davies and Taylor, simple model is employed to derive velocity of two-dimensional gas bubble rising in liquid along axis of channel of finite width (EI 1966)</p>   | <p><b>BASIC STUDIES</b><br/>           bubbles<br/>           theoretical</p>     |
| C-20 | <p>Committee on Sanitary Engineering Research<br/> <b>SOLUBILITY OF ATMOSPHERIC OXYGEN IN WATER</b><br/> <i>Proc ASCE</i> v 86 n SA 4 Jul 1960<br/>           For many years the saturation concentrations of gaseous oxygen dissolved in distilled water (as determined by Fox and reported by Whipple and Whipple) have been accepted as correct. Recently a group of researchers in England conducted experiments that showed significant differences from the previously accepted saturation concentrations. The research reported herein was conducted not to determine whether the new or the old values were correct but, independently, to determine true saturation values throughout the normal range of natural stream water temperatures</p>   | <p><b>BASIC STUDIES</b><br/>           experimental<br/>           reaeration</p> |
| C-21 | <p>Committee on Sanitary Engineering Research<br/> <b>EFFECT OF WATER TEMPERATURE ON STREAM REAERATION</b><br/> <i>Proc ASCE</i> v 87 n SA 6 Nov 1961 p 59<br/>           A search of the literature indicated that the effect of water temperature on stream reaeration rates had not been definitely established. Extensive studies of actual stream reaeration rates required knowledge of this effect. Consequently, it was necessary to undertake experimental evaluation of the temperature coefficient, (<math>\theta</math>), of the reaeration coefficient, (<math>k_2</math>). This was done in a series of carefully controlled, high-precision, laboratory experiments that indicate the reaeration rate increases geometrically at the rate of 2.41 percent per <math>^{\circ}\text{C}</math></p> | <p><b>BASIC STUDIES</b><br/>           streams<br/>           experimental</p>    |
| C-22 | <p>Committee on<br/> <b>WATER QUALITY CRITERIA</b><br/> <i>Federal Water Pollution Control Admin</i> Apr 1968 p 44<br/>           Includes recommendations for dissolved oxygen levels considered essential for maintaining native populations of fish and other aquatic life</p>  | <p><b>GENERAL</b><br/>           criteria</p>                                     |

## C—Continued

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| C-23 | <p>Conway, R A   Kumke, G W<br/> <b>FIELD TECHNIQUES FOR EVALUATING AERATORS</b><br/> Proc ASCE v 92 n SA 2 Apr 1966 p 21-42</p> <p>Rational design and operation of an aerated biological unit requires a knowledge of the oxygen-transfer capacity of the aeration systems either under consideration or installed. Detailed methods are described for use by operating engineers in injecting the required performance data through tests of commercial aerators installed in full-scale basins. The essential features of oxygen-transfer theory are reviewed together with the relationships needed to adjust the test data to specified conditions. Two important test conditions, the required auxiliary measurements, and the basic oxygen-transfer measurements are enumerated. The results of full-scale tests based on oxygenation rates, gas-stream oxygen balances, sulfite-ion depletion rates, and biological oxygen-uptake rates are presented for large sparged turbine and entrainment aerators. The ASCE Committee on Sanitary Engineering Research is considering means of collecting, correlating, and publishing the results obtained by plant engineers and their consultants in using these techniques to conduct aerator tests</p> | <p><b>EQUIPMENT</b><br/> waste treatment<br/> mechanical<br/> aerators</p> |
| C-24 | <p>Coon, C P C   Campbell, H<br/> <b>DIFFUSED AERATION IN POLLUTED WATER</b><br/> Water and Sewage Works v 114 1967 p 461</p>   | <p><b>EQUIPMENT</b><br/> waste treatment<br/> diffusers</p>                |
| C-25 | <p>Coulter, J B<br/> <b>OBJECTIVES AND CRITERIA FOR WATER POLLUTION CONTROL</b><br/> U S Dept Health Education Welfare Symposium on Streamflow Regulation for Quality Control Public Health Service Pub No 999-WP-30 Jun 1965 p 261-278</p> <p>Discusses the judgment involved in establishing water quality criteria and the economic analysis of benefits in potential water uses</p>   | <p><b>GENERAL</b><br/> criteria<br/> economics</p>                         |
| C-26 | <p>Courchaine, R J<br/> <b>SIGNIFICANCE OF NITRIFICATION IN STREAM BALANCE—EFFECTS ON THE OXYGEN BALANCE</b><br/> J Water Pollution Control Federation v 40 n 5 May 1968 p 835</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> oxidation</p>  |
| C-27 | <p>Curtet, R   Djonin, K<br/> <b>ETUDE D'UN ECOULEMENT MIXTE AIR-EAU VERTICAL DESCENDANT—REGIMES, EVOLUTION DE LA CONCENTRATION</b><br/> Houille Blanche v 22 n 5 1967 p 531-550</p> <p>Study of flow and concentration conditions of vertical downward mixed water and air flow; emulsion formed by jet of water on impact against free water surface in vertical cylindrical duct is discussed and flow conditions are classified in terms of initial data for flow without air, stable air entrainment, and air entrainment with unstable pockets; air concentration pattern in water is measured by gamma-ray technique; mean slip velocity theory is discussed. In French (EI 1968)</p>  | <p><b>BASIC STUDIES</b><br/> experimental<br/> reaeration</p>              |



## D

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| D-1 | <p><b>Dal'Man, V V Zhilyaeva</b><br/> <b>INVESTIGATION OF LONGITUDINAL MIXING DURING</b><br/> <b>BUBBLING IN STRAIGHT-THROUGH FLOW-TYPE</b><br/> <b>REACTOR COLUMNS</b><br/>         Chem and Tech of Fuels and Oils (English translation of Khimiya i Teknologiya<br/>         Topliv i Masel) p 12 Dec 1965 p 941-945<br/>         Study was made in steel and glass columns up to 9 m high and 4.1 to 29.6 cm<br/>         ID; bubblers at bottom consist of porous cermet and stainless steel plates;<br/>         values of turbulent diffusion coefficient D under steady state and transient<br/>         conditions were obtained using pulse and concentration shift methods;<br/>         experimental plots are drawn correlating Peclet diffusion number, true mean<br/>         liquid velocity, coefficient f and D with gas velocity; results agree with<br/>         calculated values. 20 refs (EI 1967)</p> | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         experimental</p>   |
| D-2 | <p><b>Danckwerts, P V</b><br/> <b>SIGNIFICANCE OF LIQUID FILM COEFFICIENT IN</b><br/> <b>GAS ABSORPTION</b><br/>         Ind and Eng Chem v 43 n 6 Jun 1951 p 1460<br/>         Describes extension of penetration theory with emphasis on concept of<br/>         surface renewal</p>  | <p><b>BASIC STUDIES</b><br/>         theoretical<br/>         reaeration</p> |
| D-3 | <p><b>Davenport, W G Richardson, F D</b><br/> <b>SPHERICAL CAP BUBBLES IN LOW DENSITY LIQUIDS</b><br/>         Chem Eng Sci v 22 n 9 Sep 1967 p 1221-1235<br/>         Measurements have been made of rising velocities and shapes of spherical cap<br/>         bubbles in column 15 cm in diameter; liquids used were water, aqueous<br/>         solutions of polyvinyl alcohol (PVA) with viscosities up to 216 centipoise and<br/>         ethyl alcohol; gases were air, nitrogen, and carbon dioxide; with carbon<br/>         dioxide, mass transfer coefficients were also obtained; relationships between<br/>         measured quantities and properties of various liquids are considered; liquid<br/>         viscosities up to 50 centipoise have no effect on either rising velocity or shape<br/>         of spherical cap bubbles. 20 refs (EI 1968)</p>   | <p><b>BASIC STUDIES</b><br/>         bubbles.<br/>         experimental</p>  |
| D-4 | <p><b>Davis, R E Acrivos, A</b><br/> <b>INFLUENCE OF SURFACTANTS ON CREEPING MOTION</b><br/> <b>OF BUBBLES</b><br/>         Chem Eng Sci v 21 n 8 Aug 1966 p 681-685<br/>         Simple model is proposed for creeping motion of bubble contaminated with<br/>         "insoluble" surface-active agent; existence of stagnant cap over rear of bubble<br/>         is taken for granted and cap size and associated bubble drag are then<br/>         computed theoretically, as functions of surface pressure at which<br/>         contaminant film collapses; model, which employs no adjustable parameters,<br/>         is consistent with experimental observations and, in particular, explains<br/>         success of empirical correlation relating bubble drag to Bond number (EI<br/>         1967)</p>   | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         experimental</p>   |
| D-5 | <p><b>De Nevers, N</b><br/> <b>BUBBLE DRIVEN FLUID CIRCULATIONS</b><br/>         A I Ch E J v 14 n 2 Mar 1968 p 222-226<br/>         Bubble-driven fluid circulations are present in bubble columns, gas lifts, pool<br/>         boiling, etc; their mechanism is shown to be quite similar to mechanism of<br/>         natural convection but with much larger driving forces; these circulations are<br/>         stable in many baffled systems but unstable and rapidly changing in size,</p>   | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         experimental</p>   |

## D—Continued

shape, and orientation in unbaffled systems; effect of these circulations in bubble columns is to lower holdup and vapor residence time, thus decreasing mass-transfer efficiency of column. 14 refs (EI 1968)

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| D-6  | <p>Derby, Ray L<br/> <b>CHLORINATION OF DEEP RESERVOIRS FOR TASTE AND ODOR CONTROL</b><br/> J American Water Works Assoc v 48 Jul 1956 p 777<br/> Reports attempts to mix two Los Angeles reservoirs by compressed air introduced through a perforated hose; water was lifted in large quantities but fell back to the bottom because of inadequate horizontal circulation</p>   | <b>EQUIPMENT</b><br>diffusers<br>reservoirs                                |
| D-7  | <p>Diachishin, A N<br/> discussion of <b>MECHANISM OF REAERATION IN NATURAL STREAMS</b> by O'Connor and Dobbins<br/> Trans ASCE v 123 1958 p 672</p>   | <b>BASIC STUDIES</b><br>streams<br>experimental<br>reaeration              |
| D-8  | <p>Dietrich, K R<br/> <b>DAS DIFFUMAT-BELUEFTUNGSSYSTEM</b><br/> Gesundheits-Ingenieur v 87 n 9 Sep 1966 p 257-261<br/> "Diffumat" aeration system; illustrated description of new patented system in which aeration of activated sludge is carried out by injecting compressed air in form of large bubbles at bottom of high (8 m and more) slim tanks; advantages of this system over surface absorption systems with water stirring and other air injection systems are shown in table listing oxygen transfer and electric energy consumption. In German (EI 1967)</p>  | <b>EQUIPMENT</b><br>waste treatment<br>diffusers                           |
| D-9  | <p>Dijkman, H K M Vrengdenhil, C B<br/> <b>THE EFFECT OF DISSOLVED GAS ON CAVITATION IN HORIZONTAL PIPELINES</b><br/> J of Hydraulic Res v 7 n 3 1969<br/> In a horizontal pipeline a pump failure may cause water-column separation at intermediate points of the pipeline. In this paper a mathematical description is given for the case of water containing dissolved gas. The main assumption is that the gas collects into a single cavity at the top of the pipeline. Using this model, the effect of the gas is considered by comparison with previous results for pure water. As a provisional conclusion it is found that the pressure-rise after compression of the cavity is less serious than in the case with vapor only</p> | <b>CAVITATION</b>  |
| D-10 | <p>DiToro, D M O'Connor, D J<br/> <b>THE DISTRIBUTION OF DISSOLVED OXYGEN IN A STREAM WITH TIME VARYING VELOCITY</b><br/> Water Resources Res v 4 n 3 1968 p 639</p>   | <b>BASIC STUDIES</b><br>streams<br>experimental<br>reaeration              |
| D-11 | <p>Dobbins, William E<br/> <b>BOD AND OXYGEN RELATIONSHIPS IN STREAMS</b><br/> Proc ASCE v 90 n SA 3 Jun 1964 p 53-79; closure in v 91 n SA 5 Oct 1965 p 549-555</p>   | <b>BASIC STUDIES</b><br>streams<br>experimental<br>reaeration<br>oxidation |

## D—Continued

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| D-12 | <p>Dobbins, W E<br/> <b>DIFFUSION AND MIXING</b><br/>           Boston Soc Engrs J v 52 n 2 Apr 1965 p 108-128<br/>           Based on Fick's laws of diffusion, and convection, and movement of nonconservative substances analysis is made on transport of sediment in river, and river and estuary pollution; diagrams are plotted for variation of eddy diffusivity with scale, rate of absorption of oxygen at fixed point on surface, and oxygen absorption coefficients. 20 refs (EI 1966)</p>      | <p><b>BASIC STUDIES</b><br/>           streams<br/>           estuaries<br/>           experimental<br/>           reaeration</p>   |
| D-13 | <p>Dobbins, W E<br/> <b>MECHANISM OF GAS ABSORPTION BY TURBULENT LIQUIDS</b><br/>           Advances in Water Res Proc 1st International Conf Water Pollution Res Pergamon Press Ltd London England v 2 1964 p 61<br/>           Develops a theoretical model for reaeration in turbulent systems. Best fit to experimental results occurs with model consisting of continuously replaced laminar liquid film. Includes good review and evaluation of previous theories. Discussions of paper are good</p> | <p><b>BASIC STUDIES</b><br/>           streams<br/>           theoretical<br/>           experimental<br/>           reaeration</p> |
| D-14 | <p>Dobbins, William E<br/> <b>THE NATURE OF THE OXYGEN TRANSFER COEFFICIENT IN AERATION SYSTEMS</b><br/>           Part 2-1 of Biological Treatment of Sewage and Ind Wastes by McCabe and Eckenfelder Reinhold New York N Y 1956</p>  | <p><b>EQUIPMENT</b><br/>           waste treatment</p>  |
| D-15 | <p>Downing, A L Bayley, R W Boon, A G<br/> <b>THE PERFORMANCE OF MECHANICAL AERATORS</b><br/>           Inst Sewage Purification J Proc pt 3 1960 p 231-247<br/>           The paper compares oxygenation efficiencies for several types of surface aerators of British manufacture. Effects of temperature, immersion depth, surfactants, and foam suppressors are discussed. The performance of one type is compared with aeration at weirs. A short discussion of diffusers is included</p>             | <p><b>EQUIPMENT</b><br/>           mechanical<br/>           aerators<br/>           cascades<br/>           diffusers</p>          |
| D-16 | <p>Downing, A L Melbourne, K V Bruce, A M<br/> <b>THE EFFECT OF CONTAMINANTS ON THE RATE OF AERATION OF WATER</b><br/>           J of Applied Chem v 7 1957 p 590</p>  | <p><b>BASIC STUDIES</b><br/>           experimental<br/>           reaeration</p>   |
| D-17 | <p>Downing, A L Truesdale, G A<br/> <b>SOME FACTORS AFFECTING THE RATE OF SOLUTION OF OXYGEN IN WATER</b><br/>           J of Applied Chem v 5 Oct 1955 p 570<br/>           The effects of a number of factors on the rate of solution of oxygen in fresh and saline water were investigated experimentally to provide information about reaeration in a polluted estuary</p>   | <p><b>BASIC STUDIES</b><br/>           experimental<br/>           reaeration</p>   |
| D-18 | <p>Drachev, S M<br/> <b>PROTSESSY SAMOOCHISHCHENIYA V SILNO SAGRYAZNENNYKH REKAKH S MALYM TASKHODOM</b><br/>           (Processes of Self-Purification in Very Polluted Rivers with a Small Flow)<br/>           Vodostnabzh i santekhnika v 15 n 7 1940 In Russian</p>  | <p><b>BASIC STUDIES</b><br/>           streams<br/>           reaeration</p>  |

## D—Continued

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| D-19 | <p>Dresnack, R Dobbins, W E<br/> <b>NUMERICAL ANALYSIS OF BOD AND DO PROFILES</b><br/> Proc ASCE v 94 n SA 5 Oct 1968 p 789-807</p> <p>The variation of Biochemical Oxygen Demand (BOD) and Dissolved Oxygen (DO) along a stretch of a polluted natural stream can be represented by two second-order partial differential equations. These equations are similar to the equation representing the conduction of heat in solids, with the exception that the stream equations contain additional lower-order terms. Analytical solutions have been obtained for many cases of the heat-conduction problem. However, the presence of the lower-order terms and the complexities of many of the boundary conditions make it impossible to obtain analytical solutions to the BOD and DO profile equations for most cases of practical interest. Furthermore, the numerical procedures which have been found to work for the solution of the heat conduction equation are not satisfactory for the BOD and DO equations because of the effects introduced by the lower-order terms. Procedures are presented for the numerical solution of the BOD and DO equations under temporally and spatially varying BOD and DO inputs. The procedures described are confined to the condition of steady, uniform stream flow</p> | <p><b>BASIC STUDIES</b><br/> streams<br/> theoretical<br/> reaeration<br/> oxidation</p>   |
| D-20 | <p>Driver, E E Krenkel, P A<br/> <b>THE EFFECTS OF MODIFICATIONS OF THE FLOW<br/> REGIME ON WASTE ASSIMILATIVE CAPACITY OF<br/> THE COOSA RIVER</b><br/> Vanderbilt U Dept of Civil Eng Sanitary and Water Res Eng Tech Report No. 5<br/> 1965 Nashville Tenn</p> <p>Discusses the assimilative capacity and hydraulic characteristics of the Coosa River, Georgia, and the effects of waste discharges from the Georgia Kraft Company, Weiss Dam, and operations of Allatoona Dam on water quality. A reduction of 80 percent of the waste assimilative capacity may be directly attributed to the impoundment of Coosa River by Weiss Dam and the stratification induced by the heated discharge contributed by a steam electric generating plant</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> reservoirs<br/> reaeration</p> |
| D-21 | <p>Dziallas, R Voith, J M<br/> <b>FRANCIS TURBINES UNDER PARTIAL LOAD AND OVERLOAD</b><br/> Transl from German by W O Wunderlich and S Vigander Tennessee Valley<br/> Authority Nov 1966</p> <p>Includes discussion of aeration for control of draft tube disturbances. Suggests that, at atmospheric pressure, an airflow corresponding to approximately 0.25 to 1 percent of the full load turbine discharge is necessary for control of the disturbances. States that larger quantities of air, under certain circumstances, may cause more serious disturbances, and in any case lead to a drop in efficiency</p>  | <p><b>EQUIPMENT</b><br/> streams<br/> turbine<br/> injection</p>                           |

## E

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| E-1 | <p>Eckenfelder, W W Jr<br/> <b>ABSORPTION OF OXYGEN FROM AIR BUBBLES IN WATER</b><br/> Proc ASCE v 85 n SA 4 Jul 1959</p> <p>Several correlations have been developed to define the absorption of oxygen from gas bubbles in water. In most cases, these correlations have been derived from bubble cap plates and other low head devices. This paper develops relationships between the liquid film coefficient, <math>K_L</math> and the Reynolds and Schmidt Numbers at liquid submergence depth up to 15 feet. Correlations are also developed relating the overall coefficient, <math>K_L a</math>, to pertinent process variables. The correlations developed from laboratory data are extended to commercial diffusion devices</p>   | <p><b>BASIC STUDIES</b><br/> bubbles<br/> experimental</p>                     |
| E-2 | <p>Eckenfelder, W W Jr<br/> <b>OXYGEN TRANSFER AND AERATION</b><br/> Manual of Treatment Processes v 1 Environmental Sci Services Corp 1968</p> <p>Discusses effect of waste characteristics on oxygen transfer, aerator types, and aeration design for application to sewage treatment problems</p>  | <p><b>EQUIPMENT</b><br/> waste treatment</p>                                   |
| E-3 | <p>Eckholdt, M<br/> <b>THE ARTIFICIAL AERATION OF RIVER WATER<br/> ACCORDING TO R. VON WOLFF</b><br/> Soutsche Gewasserkundliche Mitteilungen v 10 n 1 1966 p 1-11</p> <p>Results of experiments at the Saar Hydroelectric Station at Mettlack (1964)<br/> In German</p>  | <p><b>EQUIPMENT</b><br/> streams<br/> turbine injection</p>                    |
| E-4 | <p>Edwards, R W Owens, M<br/> <b>THE OXYGEN BALANCE OF STREAMS</b><br/> Ecology and the Industrial Society Oxford 1965</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> reaeration</p>     |
| E-5 | <p>Edwards, R<br/> <b>PLANTS AS OXYGENATORS IN RIVERS</b><br/> Water Res v 2 1968 p 243</p>   | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> photosynthesis</p> |
| E-6 | <p>Einstein, A<br/> <b>INVESTIGATIONS ON THE THEORY OF THE BROWNIAN<br/> MOVEMENT</b><br/> Ann Physik v 17 1905 p 549</p>   | <p><b>BASIC STUDIES</b><br/> experimental</p>                                  |
| E-7 | <p>Elder, R A Smith, M N Wunderlich, W O<br/> <b>AERATION EFFICIENCY OF HOWELL-BUNGER VALVES</b><br/> J Water Pollution Control Federation v 41 n 4 Apr 1969 p 629-639</p> <p>The effectiveness of the Howell-Bunger valve as a device for aerating discharges from reservoirs was investigated under conditions of free discharge to a catchment area and discharge to a tailwater pool. The results showed that the aeration efficiency is related to the discharge velocity, and that thickness of jet and initial dissolved-oxygen concentration have little effect. At discharge velocities of 30 ft per sec or more the valve proved a highly efficient aeration device for both types of discharge, while at lower velocities it was slightly more effective for free discharges than for confined discharges. A further series of tests is planned to investigate the aeration achieved when the valve discharges into a tunnel (WPA 1502 Aug 1969)</p> | <p><b>EQUIPMENT</b><br/> streams<br/> Howell-Bunger<br/> valves</p>            |

## E—Continued

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| E-8  | <p>Elmore, H L<br/> <b>EFFECT OF WATER TEMPERATURE ON STREAM REAERATION</b><br/> Proc ASCE n SA 6 1961 p 59</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> reaeration</p> |
| E-9  | <p>Erickson, L E Ho, Y S Fan, L T<br/> <b>MODELING AND OPTIMIZATION OF STEP AERATION<br/> WASTE TREATMENT SYSTEMS</b><br/> Water Pollution Control Federation J v 40 1968 p 717</p> <p>Several flow systems for use with step aeration process were examined under optimal operating conditions—completely mixed tanks-in-series systems, plug-flow systems, and composite of two; allocation of feed along system is desirable and method of determining optimum allocation and tank volumes for given type of step aeration is shown; mathematical model developed is based on certain simplifying assumptions and is considered only approximation of complex treatment process</p>   | <p><b>EQUIPMENT</b><br/> waste treatment</p>                               |
| E-10 | <p>Ettelt, G A<br/> <b>ACTIVATED SLUDGE THICKENING BY DISSOLVED AIR<br/> FLOTATION</b><br/> Purdue U—Eng Extension Ser 117 pt 1 1965 p 210-244</p> <p>Use of dissolved air flotation process for sludge thickening at Chicago Southwest plant is described; theoretical aspects of flotation are expressed in mathematical relationships; laboratory tests on activated sludge were conducted in pressure cell; subsequent tests were performed to experimentally correlate terminal velocity of activated solids for various conditions; two proprietary dissolved air flotation pilot units of approximately 150 gpm feed rate were tested; performance of flotation unit was dependent on proper inlet design to maximize adhesion efficiency. Before 19th Industrial Waste Conference May 1964 (EI 1965)</p> | <p><b>EQUIPMENT</b><br/> waste treatment<br/> misc uses</p>                |

## F

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|-----|---|---|
| F-1 | <p>Fair, G M Geyer, J C<br/> <b>WATER SUPPLY AND WASTE WATER DISPOSAL</b><br/>         John Wiley and Sons Inc New York N Y 1954</p>  | <p><b>GENERAL</b></p>   |
| F-2 | <p>Falk, A<br/> <b>EINSATZ VON KOLBENKOMPRESSOREN AUF KLAERANLAGEN</b><br/>         Gas- u Wasserfach v 106 n 32 Aug 1965 p 903-905<br/>         Use of piston compressors in sewage treatment plants; certain aeration processes can be aided by compressed air, such as large delivery blowers with low pressure for aerobic decomposition, for delivery of sludge and its by-products where fast rotary pumps were found insufficient; compressed air has been found economical in transportation of sludge between treatment and drying plants separated by great distances and at different levels; procedure and equipment, and integration for automatic control (EI 1966)</p> | <p><b>EQUIPMENT</b><br/>         waste treatment</p>  |
| F-3 | <p>Fish, F F Hull, C H J Peters, B J Knight, W E<br/> <b>A STUDY OF THE EFFECTS OF A SUBMERGED WEIR<br/>         IN THE ROANOKE RAPIDS RESERVOIR UPON<br/>         DOWNSTREAM WATER QUALITY</b><br/>         Special Report No. 1 Roanoke River Studies<br/>         Compiled by Special Report Committee for Committee for Roanoke River Studies Feb 6 1958</p>  | <p><b>BASIC STUDIES</b><br/>         reservoirs<br/>         experimental</p>                       |
| F-4 | <p>Fischer, H B<br/> <b>DISPERSION PREDICTIONS IN NATURAL STREAMS</b><br/>         Proc ASCE v 94 n SA 5 1968 p 927</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         theoretical<br/>         experimental</p> |
| F-5 | <p>Fischerstrom, N C H<br/> <b>LOW PRESSURE AERATION OF WATER AND SEWAGE</b><br/>         Proc ASCE v 86 n SA 5 Sep 1960<br/>         Based on simplified theoretical considerations, a calculable system utilizing dispersed air at shallow depths has been developed. Elaborate tests and full-scale operation have proved that it is possible to obtain a good economy and an extremely high oxygenation capacity with this principle and perforated pipes as air distributors. Clogging of the pipes has been studied and satisfactorily eliminated</p>   | <p><b>EQUIPMENT</b><br/>         waste treatment<br/>         diffusers</p>                         |
| F-6 | <p>Ford, Maurice E Jr<br/> <b>AIR INJECTION FOR CONTROL OF RESERVOIR LIMNOLOGY</b><br/>         J American Water Works Assoc v 55 Mar 1963 p 267<br/>         Describes trials at Lake Wohlford, Calif. using compressed air to mix stratified water; lake was completely destratified after 58 hours of operation</p>  | <p><b>EQUIPMENT</b><br/>         reservoirs<br/>         diffusers</p>                              |
| F-7 | <p>Ford, M E Jr<br/> <b>ARTIFICIAL CONTROL OF RESERVOIR LIMNOLOGY AND<br/>         ITS EFFECTS ON WATER QUALITY</b><br/>         Paper presented at the Calif Section Fall Conf Santa Monica Calif Oct 25 1962</p>  | <p><b>EQUIPMENT</b><br/>         reservoirs<br/>         diffusers</p>                              |
| F-8 | <p>Fortescue, G E Pearson, J R A<br/> <b>ON GAS ABSORPTION INTO A TURBULENT LIQUID</b><br/>         Chem and Eng Sci v 22 1967 p 1163</p>   | <p><b>BASIC STUDIES</b><br/>         reaeration</p>   |

## F—Continued

- F-9 Foster, J M Botts, J A Barbin, A R Vachon, R I  
BUBBLE TRAJECTORIES AND EQUILIBRIUM LEVELS IN  
VIBRATED LIQUID COLUMNS

ASME—Paper 68-FE-1 for meeting May 6-9 1968

Analysis of bubble behavior in vertically vibrated liquid column and experimental results of equilibrium level determinations are presented; analysis avoids usual approximation of small bubble pulsation and predicts nonharmonic volume pulsation; it can be used to predict bubble trajectories and equilibrium levels; vibrational amplitude affects bubble motion indirectly through its effect on thermodynamic behavior of bubble; experimental results compare favorably with analysis (EI 1968)

## BASIC STUDIES

bubbles  
theoretical  
experimental



## G

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| G-1 | <p>Gal-Or, B Resnick, W<br/> <b>MASS TRANSFER FROM GAS BUBBLES IN AGITATED VESSEL WITH AND WITHOUT SIMULTANEOUS CHEMICAL REACTION</b><br/>         Chem Eng Sci v 19 n 9 Sep 1964 p 653-663<br/>         Model permits prediction of total mass transfer rates for sparingly soluble gas in gas-liquid contactor; model is based on average residence time of gas bubbles in continuous phase, and permits estimation of rate of diffusion per unit area as well as total area for diffusion; equations have been solved for range of variables and results are presented graphically (EI 1965)</p> | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         theoretical</p>   |
| G-2 | <p>Gameson, A L H Truesdale, G A Downing, A L<br/> <b>RE-AERATION STUDIES IN A LAKE LAND BECK</b><br/>         J Inst Water Engr (Brit) v 9 1955 p 571<br/>         Develops a theoretical model for estimating reaeration in turbulent streams</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         theoretical<br/>         experimental<br/>         reaeration</p> |
| G-3 | <p>Gameson, A and others<br/> <b>SOLUBILITY DATA FOR SALT WATER</b><br/>         J of Applied Chem v 5 1955 p 502</p>   | <p><b>BASIC STUDIES</b><br/>         experimental<br/>         reaeration</p>   |
| G-4 | <p>Gameson, A L H Truesdale, G A<br/> <b>SOME OXYGEN STUDIES IN STREAMS</b><br/>         J Inst of Water Eng Nov 1955</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p>                          |
| G-5 | <p>Gameson, A Truesdale, G A Varley<br/> <b>SOME FACTORS AFFECTING THE AERATION OF FLOWING WATER</b><br/>         Water and Sanitary Eng v 6 n 2 Jul 1956 p 52</p>  | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p>                          |
| G-6 | <p>Gameson, A<br/> <b>WEIRS AND THE AERATION OF RIVERS</b><br/>         J Inst of Water Engrs v 11 n 6 Oct 1957 p 477<br/>         Measurements at a number of weirs resulted in the relationship:</p> $r = 1 + abh/2$ <p>Where r is the ratio of upstream deficit to downstream deficit,<br/>         a = 1.25 in slightly polluted water, 1.0 in moderately polluted water, and 0.85 in sewage effluents;<br/>         b = 1 for a free weir, 1.3 for a step weir, h is the height of fall in meters</p>  | <p><b>EQUIPMENT</b><br/>         streams<br/>         cascades</p>  |
| G-7 | <p>Gameson, A L H Vandyke, K G Ogden, C G<br/> <b>THE EFFECT OF TEMPERATURE ON AERATION AT WEIRS</b><br/>         Water and Water Eng (Brit) v 62 1958 p 489</p>  | <p><b>EQUIPMENT</b><br/>         streams<br/>         cascades</p>  |
| G-8 | <p>Gannon, J J<br/> <b>RIVER AND LABORATORY BOD RATE CONSIDERATIONS</b><br/>         Proc ASCE v 92 n SA 1 Feb 1966 p 135-161<br/>         Differences observed between laboratory bottle BOD rate, and river BOD rate, motivated investigation of river BOD conditions to develop better understanding of deoxygenation component of river oxygen balance</p>  | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         oxidation</p>                           |

## G—Continued

relationship, limiting consideration, however, to effect of BOD rate; two river situations in Mich., one domestic waste problem on Clinton River below Pontiac, Mich. waste treatment plant, other industrial problem on Tittabawassee River below Dow Chemical Co. at Midland were studied. 39 refs (EI 1966)

- G-9 Gannon, J J  
AERATION AT WASTE TREATMENT PLANT OUTFALL  
STRUCTURES  
Water and Wastes Eng v 4 n 4 Apr 1967 p 62-65  
Significance of aeration at waste treatment plant outfall structures is discussed and illustrated in terms of two situations—Pontiac, Mich., waste treatment plant, discharging its effluent into Clinton River, and Dow Chemical Co. waste treatment plant at Midland, Mich., discharging its effluent into Tittabawassee River; comparisons made between observed and predicted results, using equations developed by British workers studying aeration at weir systems, indicate good agreement for Pontiac, but indicate that predictions are about 13 to 14 percent higher than observed results for Dow. 12 refs (EI 1967)
- G-10 Garancher, J  
LA PROTECTION D'UN PORT PETROLIER PAR UN  
RIDEAU DE BULLES  
Houille Blanche v 22 n 4 1967 p 387-390  
Bubble screen protection for oil harbors is provided by submerged network of pipes discharging compressed air through row of nozzles along their top, and generating vertical bubble screens which form impenetrable barrier for any oil accidentally discharged into harbor; results obtained at several French ports are described; method can be used to protect beaches and river water intakes from pollution by oil and sewage. In French (EI 1968)
- G-11 Geckler, J R Mackenthun, K M Ingram, W M  
GLOSSARY OF COMMONLY USED BIOLOGICAL AND  
RELATED TERMS IN WATER AND WASTE WATER  
CONTROL  
Public Health Service Cincinatti Jul 1963
- G-12 Giebler, G Koppe, P  
METHODE SUR BESTIMMUNG DER WIRKUNG DES OZONS  
BEI DER AUFBEREITUNG VON WASSER  
Gas- u Wasserfach v 106 n 8 Feb 1965 p 215-219  
Method of determining effect of ozone during water treatment; method consists of treating water with gas mixture containing ozone; effect of ozone is measured by determining content of substances remaining in water after treatment; design and performance of experimental equipment and data on chemical action of ozone In German (EI 1965)
- G-13 Glover, Robert E  
DISPERSION OF DISSOLVED OR SUSPENDED MATERIALS  
IN FLOWING STREAMS  
U S Geological Survey Prof Paper No 433-B Washington D C 1964
- EQUIPMENT  
streams  
cascades
- EQUIPMENT  
diffusers  
misc uses
- GENERAL  
terms
- BASIC STUDIES  
waste treatment  
experimental
- BASIC STUDIES  
streams  
experimental

## G—Continued

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| G-14 | <p>Godfrey, Richard G Frederick, Bernard J<br/> <b>DISPERSION IN NATURAL STREAMS</b><br/>         Open-File Reports U S Geological Survey Washington D C 1963</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental</p>   |
| G-15 | <p>Gomella, C<br/> <b>DIFFUSION DE L'OZONE DANS L'EAU</b><br/>         Houille Blanche v 22 n 4 1967 p 439-449<br/>         Ozone diffusion in water; physical and chemical features of ozone are reviewed, also how 10 to 20 g/cu m of ozonized air is obtained industrially; oxidizing effect of ozone on chemical compounds in water is discussed; ozone distribution and decrease in its residual proportion in water by self-destruction are considered theoretically; application technique was tested on industrial scale. In French with English summary (EI 1968)</p>  | <p><b>BASIC STUDIES</b><br/>         waste treatment<br/>         experimental</p>   |
| G-16 | <p>Grace, J R Harrison, D<br/> <b>INFLUENCE OF BUBBLE SHAPE ON RISING VELOCITIES OF LARGE BUBBLES</b><br/>         Chem Eng Sci v 22 n 10 Oct 1967 p 1337-1347<br/>         Equations are derived in two and three dimensions which relate rising velocity of large bubble in inviscid liquid to its size and to radius of curvature of its leading edge; elliptical-cap and ovary ellipsoidal bubbles rise faster than corresponding circular- and spherical-cap bubbles, and this has been confirmed experimentally using "two-dimensional" air bubbles in water; bubbles take up elliptical shapes if they enclose surface (e.g., rod) as they rise, and stability of bubbles under these conditions is considered; relevant to behavior of bubbles in fluidized beds. 11 refs (EI 1968)</p>                                 | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         theoretical<br/>         experimental</p>  |
| G-17 | <p>Grindrod, J<br/> <b>BRITISH RESEARCH ON AERATION AT WEIRS</b><br/>         Water and Sewage Works v 109 1962 p 395<br/>         Contains brief descriptions of aeration at weirs and mentions aeration occurring at sewage works outfalls</p>  | <p><b>EQUIPMENT</b><br/>         streams<br/>         cascades</p>   |
| G-18 | <p>Guillaume, F<br/> <b>EVALUATING AERATION DEVICES</b><br/>         Water Pollution Control Ontario v 107 n 1 1969 p 26<br/>         The author discusses the article on evaluation of aeration devices, by Black, S. A., (see Water Pollution Abstract v 42 n 978 1969), and queries the practicality of the extension of the test procedure which rates the aerator using tap water, for evaluating its adequacy for intended use and its suitability for a particular plant design. Modifications in the procedure are suggested (WPA 1621 Aug 1969)</p>  | <p><b>EQUIPMENT</b><br/>         waste treatment</p>   |
| G-19 | <p>Gunnerson, C G Bailey, T E<br/> <b>OXYGEN RELATIONSHIP IN THE SACRAMENTO RIVER</b><br/>         Proc ASCE v 89 n SA Aug 1963 p 95<br/>         A 15-month pollution survey of the Sacramento River showed the effects of agricultural, municipal, and industrial discharges into the river. Unexpected results of the investigation included the observation of nighttime increases and other anomalies in dissolved oxygen concentrations which limit both classical and modern approaches to characterizing oxygen relationships. Variations in respiration, which cannot be predicted with present knowledge, provide the best explanation of the observed anomalies. Additional study of changes in respiration rates of aquatic communities is required for predicting the response of a stream to waste discharges</p> | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration<br/>         oxidation<br/>         respiration</p> |

## G—Continued

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| G-20 | Gustafson, Bengt Wistberg, Nils<br>ACTIVATED SLUDGE PROCESS UNDER DEFINED CONDITIONS<br>Kungl Teknisha Hogsholan (Sweden) 1964 .   | EQUIPMENT<br>waste treatment             |
| G-21 | Gutti, S R<br>BEHAVIOR OF SMALL GAS BUBBLES IN ACCELERATED<br>LIQUID<br>Proc ASCE v 94 n HY 4 Jul 1968 p 1073-1082<br>Time dependent motion of small gas bubbles in liquids subjected to linear pressure gradient was studied; expression for bubble slip, was derived as function of liquid and gas densities, initial velocities, and liquid velocity gradient was studied; expression for bubble slip was derived as function of liquid and gas densities, initial velocities, and liquid velocities, and approaches value of 0.9967 for highly accelerating flows. 14 refs (EI 1968) | BASIC STUDIES<br>bubbles<br>experimental |

## H

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| H-1 | <p><b>Hamalainen, M</b><br/> <b>PREVENTING THE DEPLETION OF OXYGEN BY</b><br/> <b>CHANGING THE HYPOLIMNION</b><br/>         Vesitalous v 10 n 3 1969 p 25-27</p> <p>In winter the ice cover on many Finnish lakes causes oxygen depletion with adverse effects on water quality and fish. In the artificial lake Dammen, in Espoo, the problem has been solved by installing a siphon spillway composed of plastic pipes and extending into the hypolimnion so that a continuous circulation of water is maintained, giving a satisfactory concentration of oxygen throughout the year. The method is cheap and can be adapted for use in many lakes, including impounded lakes where the head of water can be utilized to produce the necessary circulation and prevent oxygen depletion in the hypolimnion. Water Pollution Abstracts</p> | <p><b>EQUIPMENT</b><br/>         reservoirs<br/>         misc equipment</p>   |
| H-2 | <p><b>Hanes, N B Irvine, R L</b><br/> <b>NEW TECHNIQUES FOR MEASURING OXYGEN UPTAKE</b><br/> <b>RATES</b><br/>         J Water Pollution Control Federation v 40 n 2 Feb 1968 p 223</p>   | <p><b>BASIC STUDIES</b><br/>         experimental<br/>         oxidation</p>  |
| H-3 | <p><b>Hann, R W Jr</b><br/> <b>WATER QUALITY ASPECTS OF WATER RESOURCES</b><br/> <b>PLANNING</b><br/>         Texas A&amp;M U Oct 1968<br/>         Textbook for course in water quality management for USBR personnel</p>  | <p><b>GENERAL</b></p>   |
| H-4 | <p><b>Harleman, D R F Holley, E R</b><br/>         discussion of <b>TURBULENT DIFFUSION AND THE</b><br/> <b>REAERATION COEFFICIENT</b> by Krenkel and Orlob<br/>         Trans ASCE v 128 III p 327-333 1963</p>  | <p><b>BASIC STUDIES</b><br/>         streams<br/>         theoretical<br/>         experimental<br/>         reaeration</p> |
| H-5 | <p><b>Harper, J F Moore, D W Pearson, J R A</b><br/> <b>EFFECT OF VARIATION OF SURFACE TENSION WITH</b><br/> <b>TEMPERATURE ON MOTION OF BUBBLES AND DROPS</b><br/>         J Fluid Mechanics v 27 pt 2 Feb 1967 p 361-366</p> <p>Boundary conditions at surface of small bubble rising in liquid are examined theoretically, and it is shown by order-of-magnitude arguments, which are confirmed by detailed calculation in special case, that although surface-tension gradients must always exist around bubble, they are too small to affect motion appreciably unless surface-active substances are present. 13 refs (EI 1967)</p>  | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         theoretical</p>   |
| H-6 | <p><b>Hart, I C</b><br/> <b>NOMOGRAPHS TO CALCULATE DISSOLVED OXYGEN CONTENTS</b><br/> <b>AND EXCHANGE (MASS TRANSFER) COEFFICIENTS</b><br/>         Water Res v 1 1967 p 391</p>   | <p><b>BASIC STUDIES</b><br/>         experimental<br/>         reaeration</p>   |
| H-7 | <p><b>Hays, James R</b><br/> <b>MASS TRANSPORT MECHANISMS IN OPEN-CHANNEL FLOW</b><br/>         PhD Thesis Vanderbilt U Nashville Tenn 1966</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         reaeration</p>  |

## H—Continued

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| H-8  | <p>Hazen, R<br/> <b>GETTING MORE FOR WATER POLLUTION CONTROL DOLLAR</b><br/>         Civil Eng (NY) v 37 n 12 Dec 1967 p 38-39<br/>         Present laws and policies that require waste water effluent treatment to be same regardless of effect on receiving water are unrealistic; reaeration of rivers can be done much more economically by reoxygenation than by dilution; cost might be \$33/1,000 lb of oxygen added, compared to \$250 for reservoir to supply extra water for dilution; zoning should allow waste producing industries only where adequate water is available; research money should be spent for usable information only, not to support laboratories and researchers; halt should be called to producing volumes of statistics on needs and subsequent savings should be spent on construction (EI 1968)</p> | GENERAL<br>economics                                       |
| H-9  | <p>Hemphill, J<br/> <b>METHOD OF WINTERKILL PREVENTION</b><br/>         Arizona Game and Fish Dept 1954<br/>         Uses compressed air mixing of lakes to prevent ice forming and cutting off the oxygen supply</p>  | EQUIPMENT<br>reservoirs<br>diffusers<br>misc uses          |
| H-10 | <p>Higbie, R<br/> <b>THE RATE OF ABSORPTION OF A PURE GAS INTO<br/>         A STILL LIQUID DURING SHORT PERIODS OF<br/>         EXPOSURE</b><br/>         Trans American Inst of Chem Eng v 21 1935 p 365<br/>         Compares experimental rates of gas absorption with rates predicted by Lewis-Whitman film theory and penetration theory. Primarily concerned with short exposure periods in industrial absorption applications</p>   | BASIC STUDIES<br>theoretical<br>experimental<br>reaeration |
| H-11 | <p>Hinde, J Nelson<br/> <b>REVITALIZING WATER THE NATURAL WAY</b><br/>         paper American Water Works Assoc 89th Annual Conf San Diego Calif<br/>         May 18-22 1969<br/>         Describes the Air-Aqua system for controlled aeration of lakes and reservoirs. System releases air from a weighted valved tubing laid on the bottom of the lake; controlled bubble size produces a laminar uplift of a low-velocity nonturbulent flow which requires very little energy</p>  | EQUIPMENT<br>reservoirs<br>diffusers                       |
| H-12 | <p>Hinde Engineering Company<br/> <b>WATER IMPOUNDMENT RESERVOIR, HIGHLAND SEWER<br/>         AND WATER AUTHORITY, HIGHLAND, PENNSYLVANIA</b><br/>         Sales brochure Air-Aqua Case History 2602 Hinde Eng Co Highland Park III<br/>         Describes the Air-Aqua aeration system installed at Lloydell Reservoir to improve water quality; cost amounts to \$1.45 per day for electricity, maintenance and amortization for the 208-million-gallon reservoir</p>  | EQUIPMENT<br>reservoirs<br>diffusers                       |
| H-13 | <p>Holley, E R<br/> <b>UNIFIED VIEW OF DIFFUSION AND DISPERSION</b><br/>         Proc ASCE v 95 n HY 2 Mar 1969<br/>         Diffusion and dispersion are basically convective transport mechanisms. The method chosen for representing the convection in a mass balance equation is the determining factor in deciding whether diffusion or dispersion must be included in the conservation equation for a given flow. This principle is illustrated for molecular diffusion, turbulent diffusion, and longitudinal dispersion. In a given flow, the relative importance of diffusion or dispersion</p>   | GENERAL<br>terms   |

## H—Continued

in different transport problems depends on the steepness of the concentration gradient. It is proposed that the term "diffusion" be reserved for transport that is associated primarily with time-averaged velocity fluctuations and that "dispersion" be used for transport associated primarily with the spatial average of velocity variations

- H-14    Holley, E R  
SOME DATA ON DIFFUSION AND TURBULENCE IN  
RELATION TO REAERATION  
Research Report No 21 Water Resources Center Univ of Illinois July 1969  
Heat was used as a tracer to determine diffusion rates immediately below the free surface both in the "film" region and in the remainder of the water in a mixing vessel. The results tend to indicate that model can be used to represent the downward transport of a substance which is being absorbed at the free surface. Apparently, the diffusion coefficient in the "film" can be either equal to or greater than the molecular coefficient depending on the amount of mixing at the free surface. Hot film anemometry was used to determine turbulence characteristics from 1 to 0.006 inch below the free surface of a laboratory open-channel flow. The energy spectra indicate no significant changes in the turbulence in this region. Thus, apparently turbulence exists right up to the free surface and in the "film" region. The amount of reliable data that was obtained was very limited.
- H-15    Hooper, Frank F Ball, Robert C Tanner, Howard A  
AN EXPERIMENT IN THE ARTIFICIAL CIRCULATION  
OF A SMALL MICHIGAN LAKE  
Trans American Fisheries Soc v 82 1952 p 222  
Attempts to mix a stratified body of water using a gasoline-drive centrifugal pump on shore to withdraw water from the hypolimnion and discharging it on the surface of a barge
- H-16    Huckabay, H K Keller, A G  
AERATION ON AN INCLINED TRANSVERSELY CORRUGATED  
SOLID SURFACE  
J Water Pollution Control Federation v 42 n 5 pt 2 May 1970  
The "cascade board" aerates water by natural gravity flow down an inclined, transversely corrugated, solid surface. A study was carried out for angles of inclination of 5° to 30° from the horizontal. Flow rates of 0.02 to 0.08 mgd/ft of width (248 to 992 cu m/day/m of width), and temperatures of 83° to 108° F (28° to 42° C) were studied. Dissolved oxygen was measured by a microadaptation of the Winkler procedure. The mass transfer coefficient was correlated successfully in terms of flow rate and angle of inclination. The number of transfer units was found to be independent of flow rate and to correlate only with the angle of inclination. No optimum angle existed; however, the larger angles of inclination were more favorable to aeration
- H-17    Hughmark, G A  
HOLDUP AND MASS TRANSFER IN BUBBLE COLUMNS  
Ind and Eng Chem—Process Design and Development v 6 n 2 Apr 1967  
p 218-220  
Correlation for gas holdup in bubble columns predicts values with average absolute deviation of about 11 percent from experimental holdups; recent correlation for mass transfer from single gas bubbles in liquids is applicable to swarm data for bubble columns; illustrative problem is solved. 9 refs (E1 1967)
- BASIC STUDIES  
streams  
experimental  
reaeration
- EQUIPMENT  
reservoirs  
pumps
- EQUIPMENT  
streams  
cascades
- BASIC STUDIES  
bubbles  
experimental

## H—Continued

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|------|--|--|
| H-18 | <p>Hull, C H J<br/> <b>OXYGENATION OF BALTIMORE HARBOR BY PLANKTONIC ALGAE</b><br/> J Water Pollution Control Federation v 35 May 1963 p 587-606</p>   | <p><b>BASIC STUDIES</b><br/> experimental<br/> photosynthesis</p>  |
| H-19 | <p>Hull, C H J<br/> <b>PHOTOSYNTHESIS AS A FACTOR IN THE OXYGEN BALANCE OF RESERVOIRS</b><br/> U S Dept Health Education Welfare Symposium on Streamflow Regulation for Quality Control Public Health Service Pub No 999-WP-30 Jun 1965 p 77-96<br/> Describes studies on photosynthetic oxygenation in streams, estuaries and impoundments, and significance in controlling oxygen balance</p>  | <p><b>BASIC STUDIES</b><br/> reservoirs<br/> experimental<br/> photosynthesis</p>                                |
| H-20 | <p>Hull, C H J<br/> <b>PHOTOSYNTHETIC OXYGENATION OF A POLLUTED ESTUARY</b><br/> Advances in Water Pollution Res v 3<br/> E. A. Pearson (ed), Proc International Conf on Water Pollution Res London, England Sep 3-7 1962 Pergamon Press London England 1964 p 347-374<br/> disc on p 391-395<br/> Abstract in: London Conf Abstracts<br/> JWPCF v 34 Mar 1962 p 275-276</p>   | <p><b>BASIC STUDIES</b><br/> estuaries<br/> experimental<br/> photosynthesis</p>                                 |
| H-21 | <p>Humphrey, W H<br/> <b>REMOVAL OF AGGRESSIVE CARBON DIOXIDE FROM POTABLE WATERS</b><br/> Water and Water Eng v 68 n 822 Aug 1964 p 324-327<br/> Removal of CO<sub>2</sub> in excess of that required to maintain CaCO<sub>3</sub>/H<sub>2</sub>CO<sub>3</sub> equilibrium from water by aeration, marble, magnesite, lime, and dolomite filter methods; determination with aid of Tillmans graph, yielding aggressive CO<sub>2</sub> and probable pH values from free CO<sub>2</sub> and CaCO<sub>3</sub> concentrations; example of corrosiveness of aggressive CO<sub>2</sub> on water systems (EI 1965)</p>   | <p><b>BASIC STUDIES</b><br/> experimental</p>  |
| H-22 | <p>Hunter, H M Potter, W J Lyons, E T<br/> <b>PROGRESS REPORT—AN INVESTIGATION OF THE EFFECT OF ENGINEERING STRUCTURES UPON THE DISSOLVED OXYGEN CONTENT OF STREAMS AND RESERVOIRS</b><br/> USBR Denver Colo Report No CH-103 Apr 1961<br/> Presents and discusses (1) analytical data obtained in preliminary investigations of (a) the dissolved oxygen content of streams and reservoirs on the Colorado—Big Thompson Project, and (b) chemical methods of determining the dissolved oxygen content of water samples; (2) recommendations for future investigative work in this field. Includes a bibliography with 348 references, many dealing with instrumentation and chemical analysis for determination of dissolved oxygen</p> | <p><b>BASIC STUDIES</b><br/> streams<br/> reservoirs<br/> experimental<br/> DO ANALYSIS<br/> instrumentation</p> |
| H-23 | <p>Hurwitz, E Nogaj, R U Roeber, J A<br/> <b>PERFORMANCE OF SURFACE AERATORS UNDER WIDELY VARYING LOADINGS IN ACTIVATED SLUDGE SYSTEM</b><br/> Water and Sewage Works v 112 Nov 1965 p R-209-212 214-216 218<br/> Dixon, Ill. sewage treatment plant was used to test performance of surface aerators under several process applications of activated sludge system; performance and operating data of plant and sludge processes; empirical formulas developed from studies are summarized; plant was operated as conventional activated sludge plant at conventional loadings; contact</p>   | <p><b>EQUIPMENT</b><br/> waste treatment<br/> mechanical<br/> aerators</p>                                       |



## H--Continued

stabilization plant at conventional loadings; contact stabilization plant at extended aeration loadings; and high rate activated sludge plant (EI 1966)

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|------|--|--|
| H-24 | Hutchinson Sherwood<br>LIQUID FILM IN GAS ABSORPTION<br>Ind and Eng Chem Jun 1937 p 836  | BASIC STUDIES<br>theoretical<br>experimental<br>reaeration |
| H-25 | Hutchison, G E<br>A TREATISE ON LIMNOLOGY, VOL. I, GEOGRAPHY, PHYSICS<br>AND CHEMISTRY<br>John Wiley and Sons Inc New York N Y 1957<br>Discusses the formation and persistence of stratification in reservoirs | GENERAL  |

# I

- I-1 Iberall, A S Cardon, S Z  
AERATION MASS TRANSFER RELATED TO REYNOLDS  
NUMBER  
J Applied Chem v 16 n 2 Feb 1966 p 64-72  
Study of aeration rate data for streams and laboratory channels shows that aeration rate can be correlated with Reynolds number and Schmidt number by suitable dimensionless mass-transfer parameter which varies only slowly over wide range of Reynolds number; this parameter, analog to similar correlations in heat- and mass-transfer fields, has two different near-constant levels, one in low Reynolds number regime corresponding to molecular diffusivity, and another in high Reynolds number regime corresponding to eddy diffusivity (EI 1966)
- BASIC STUDIES  
streams  
experimental  
reaeration
- I-2 Ignjatovic, L R  
EFFECTS OF PHOTOSYNTHESIS ON OXYGEN SATURATION  
J Water Pollution Control Federation v 40 n 5 May 1968 p R151
- BASIC STUDIES  
experimental  
photosynthesis
- I-3 Imhoff Grabbe Albrecht  
ERPROBUNG VERSCHIEDENER VERFAHREN ZUN  
KUNSTLICHEN GEWASSERBELUFTUNG (Testing of  
Various Methods to Artificially Aerate Water)  
Vom Wasser 1968 Band XXXV In German
- EQUIPMENT
- I-4 Imhoff, K R  
UEBER DIE REINIGUNGSLEISTUNG DER RUHRSTAUSEEN  
Gas- u Wasserfach v 106 n 46 Nov 1965 p 1264-1267  
On purification capacity of impounded reservoirs of Ruhr River; 100 treatment plants of region for purifying drinking water are successfully increased by four Ruhr reservoirs paying for themselves by hydroelectric power generation; 1960 to 1964 chemical-biological laboratory tests of reservoir waters are tabulated, and results show that free-flowing river self-purification recovery distance is shortened by 3.2 to 3.7 higher purification values/river km by flowing through reservoirs. 24 refs In German (EI 1966)
- BASIC STUDIES  
streams  
reservoirs  
experimental  
reaeration
- I-5 Imhoff, K R  
OXYGEN MANAGEMENT AND ARTIFICIAL REAERATION  
IN THE AREA OF BALDENEY LAKE AND THE  
LOWER RUHR RIVER  
Das Gas- und Wasserfach 109 Jahrg (1968) Heft 34 Seite 936-941  
(Wasser-Abwasser) in German  
The Ruhr River in Germany has presented a major pollution-control problem for a long time. Although only a small river, the equivalent of sewage from over 2 million population comes through the central area near the city of Essen. In addition to very strict control of effluents by waste treatment plants, the pollution control agency, the Ruhrverband, has applied instream aeration as a supplemental means. Three aeration methods have been used—by introducing air into hydraulic turbines, by diffusers (bubbling from submerged orifices), and by mechanical aerators. Technical analysis allows an economic comparison as follows. In order to remove organic pollution of one population equivalent, at times of low flow, the cost would amount to 0.81 DM for a mechanical aerator, and 0.22 DM with the turbine aerator, as compared to 4.0 DM for expansion of the treatment plant to achieve the same result. Other figures show the diffuser as much less economic than the
- EQUIPMENT  
streams  
reservoirs  
diffusers  
mechanical  
aerators  
turbine injection

## I—Continued

mechanical aerator, though part of the extra cost is due to certain special circumstances. This result is in accord with recent American findings that instream aeration is an economical means in severe pollution situations. (Whipple-Rutgers)

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| I-6  | <p>Ingols, R S<br/> <b>POLLUTIONAL EFFECTS OF HYDRAULIC POWER GENERATION</b><br/> Sewage and Ind Wastes v 29 1957 p 292-297<br/> Discusses positive and negative effects of impoundments on downstream water quality, including reduction of DO</p>   | <p><b>BASIC STUDIES</b><br/> reservoirs<br/> experimental</p>                     |
| I-7  | <p>Ingols, R S<br/> <b>EFFECT OF IMPOUNDMENT ON DOWNSTREAM WATER QUALITY, CATAWBA RIVER, S. C.</b><br/> J American Water Works Assoc v 51 n 1 Jan 1959 p 42-46<br/> Reports on conditions causing oxygen depletion in the hypolimnion of a reservoir and oxygen depletion in the Holsten River</p>  | <p><b>BASIC STUDIES</b><br/> reservoirs<br/> experimental<br/> oxidation</p>      |
| I-8  | <p>Ingols, R S<br/> <b>SHORT TERM BOD</b><br/> Water and Sewage Works v 115 1968 p 258</p>  | <p><b>BASIC STUDIES</b><br/> waste treatment<br/> experimental<br/> oxidation</p> |
| I-9  | <p>Irwin, William H Symons, James M Robeck, Gordon G<br/> <b>IMPOUNDMENT DESTRATIFICATION BY MECHANICAL PUMPING</b><br/> Federal Water Pollution Control Admin Cincinnati Mar 1966<br/> Mechanical pumping was used to break up thermal stratification in four lakes in southern Ohio during the summer of 1964. The lake volumes were 98, 100, 120, and 1,260 acre-ft. Each impoundment was thermally and chemically stratified before pumping began. The equipment was a float-mounted, axial-flow pump, 13-acre-ft-per-day capacity, driven by a gasoline engine. The pump drew water from the bottom and discharged it at the surface. Profiles of temperature, pH, and concentrations of dissolved oxygen and carbon dioxide were taken before and after pumping. Data presented show that this method was effective in destratifying these lakes. In addition, the data show that water quality was improved by artificial destratification and that an entire impoundment could be mixed with the pump located at a single position. Some data are presented on total work requirements, but these were found to be dependent on the efficiency of the mechanical equipment and the percentage of cold water in the impoundment before pumping</p> | <p><b>EQUIPMENT</b><br/> reservoirs<br/> pumps</p>                                |
| I-10 | <p>Isaacs, W P<br/> <b>ATMOSPHERIC OXYGENATION AND BIOLOGICAL DEOXYGENATION IN AN IDEALIZED STREAM FLOW MODEL</b><br/> Dissertation Abstracts v 28 n 12 1968 p 5052<br/> Chem Abstracts v 69 1968 p 7498</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> theoretical<br/> oxidation</p>          |
| I-11 | <p>Isaacs, W P Gaudy, A F Jr<br/> <b>ATMOSPHERIC OXYGENATION IN A SIMULATED STREAM</b><br/> Proc ASCE v 94 n SA 2 Apr 1968 p 319-344<br/> A simulated stream channel was used in laboratory investigations to determine a rational expression relating stream variables and fluid properties</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> reaeration</p>        |

## I--Continued

which define the reaeration rate constant,  $K_2$ . Direct measurement of the reaeration coefficient at controlled depths and stream velocities enabled the development of a dimensionally homogeneous expression for  $K_2$ . The developed expression accounts for variations in  $K_2$  due to changes in temperature as well as changes in fluid flow conditions. For the rectangular cross section employed in these studies, the reaeration rate constant,  $K_2$ , was found to be directly proportional to average stream velocity, and inversely proportional to the average stream depth raised to the  $3/2$  power. The constant of proportionality was found to be 3.053. When the same analytical approach was applied to the best available natural stream data, the proportionality constant obtained was 3.739. Both analyses yielded highly acceptable correlation coefficients. It is believed that the difference in the values of the proportionality constant is due primarily to differences in channel geometry, i.e., smooth rectangular laboratory channel versus irregular-shaped natural river channels

## J

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|-----|---|--|
| J-1 | <p>Jackson, D F<br/> <b>EFFECTS OF ALGAE ON WATER QUALITY</b><br/>         N Y State Dept Health—Water Quality Res Symposium 1st—Proc Feb 1964<br/>         p 2-23<br/>         Certain changes in water quality which are associated with dynamics of algae metabolism were studied; theoretical equation to evaluate phytoplankton dynamics is presented; factors of light and temperature are integrated to provide foundation for physiological process of photosynthesis; incident solar radiation, as well as compensation point of light, may be determined by means of submarine photometer; review of literature on investigations of effects and dynamics of algae. 53 refs (EI 1966)</p>   | <p><b>BASIC STUDIES</b><br/>         theoretical<br/>         photosynthesis</p>                   |
| J-2 | <p>Jackson, M L Collins, W D<br/> <b>SCALE-UP OF VENTURI AERATOR</b><br/>         Ind and Eng Chem—Process Design and Development v 3 n 4 Oct 1964<br/>         p 386-393<br/>         Energy losses and oxygen transfer characteristics of two sizes of Venturi devices, designed for air aspiration by liquid, were compared; in large-scale system, transfer factors for water and for very dilute sulfite solutions, corresponding to falling and constant driving force conditions, were essentially equal (EI 1965)</p>   | <p><b>EQUIPMENT</b><br/>         Venturis</p>  |
| J-3 | <p>Jackson, R Bradney, L Bragstad, R E<br/> <b>SHORT-TERM AERATION SOLVES ACTIVATED SLUDGE<br/>         EXPANSION PROBLEMS AT SIOUX FALLS</b><br/>         J Water Pollution Control Federation v 37 n 2 Feb 1965 p 255-261<br/>         Operation of sewage treatment plant for treatment of waste water at Sioux Falls, S. Dak., that is complicated by high-strength industrial meat waste and receiving stream which at times measures nearly zero flow; based on pilot plant studies, full-scale short-term aeration system was designed and installed; eight aerators were installed in each of three passes of existing aeration tank; impellers used are flat-blade turbines; aeration tanks were modified to provide for cross-flow feeding; plant was designed to operate activated sludge portion according to efficiency of trickling filters (EI 1965)</p> | <p><b>EQUIPMENT</b><br/>         waste treatment<br/>         mechanical<br/>         aerators</p> |
| J-4 | <p>Jameson, G J Kupferberg, A<br/> <b>PRESSURE BEHIND BUBBLE ACCELERATING FROM<br/>         REST—SIMPLE THEORY AND APPLICATIONS</b><br/>         Chem Eng Sci v 22 n 7 Jul 1967 p 1053-1055<br/>         When gas bubble is formed at point in relatively inviscid liquid, its initial motion is determined by balance between buoyancy and inertia; bubble breaks off when its base reaches gas supply point and accelerates away from source; in its wake, bubble leaves distinct pressure field; it is suggested that this pressure, whose approximate magnitude can be calculated by potential flow theory, is responsible for phenomenon of dumping or weeping on sieve trays; it may also have important effects in other situations involving accelerating bubbles such as fluidized beds and in nucleate boiling. 7 refs (EI 1968)</p>                          | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         theoretical</p>                          |
| J-5 | <p>Jawonski, Nonhert A Weber, Walter J Deininger, Roolf A<br/> <b>OPTIMAL RELEASE SEQUENCES FOR WATER QUALITY<br/>         CONTROL IN MULTIPLE-RESERVOIR SYSTEMS</b><br/>         Michigan U (sets T-68-1) Apr 1968</p>   | <p><b>GENERAL</b></p>  |

## J—Continued

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| J-6  | <p>Jayne, T D Sedlacek, R J<br/> DEVELOPMENT AND CONSTRUCTION OF AN INSTRUMENT<br/> FOR MEASUREMENT OF STREAM AERATION RATE<br/> Public Health Service Contract No. PH-86-64-14 Rand Development Corp Cleveland<br/> 1964</p>  | DO ANALYSIS<br>instrumentation             |
| J-7  | <p>Jenks, J H<br/> HIGH-RATE PONDING SYSTEM SOLVES SEASONAL HIGH<br/> LOAD PROBLEM FOR HAYWARD, CALIFORNIA<br/> Water and Waste Eng v 3 n 11 Nov 1966 p 50-53<br/> Feature of program of waste water treatment and disposal is use of high-rate<br/> recirculation and aeration ponding system; to meet initial treatment needs for<br/> 19 mgd of combined sanitary sewage and seasonal high-strength wastes<br/> associated with local food processing industry; single "Inka" grid installed in<br/> high-rate pond was operated at submergence of 28 in.; air was generally<br/> supplied to grid at rate of 500 cfm; at that rate, blower power requipment<br/> was 5 hp; full-scale ponds are divided into four separate units, each with its<br/> own recirculation and aeration system (EI 1967)</p>   | EQUIPMENT<br>waste treatment<br>diffusers  |
| J-8  | <p>Johnson, A I Besik, F Hamielec, A E<br/> MASS TRANSFER FROM A SINGLE RISING BUBBLE<br/> Canadian J of Chem Eng v 47 n 6 Dec 1969 p 559<br/> Describes water column experiments to determine bubble sizes and transfer<br/> rates of carbon dioxide, ethylene, and butene. Results are compared with<br/> previous investigations and an empirical equation is presented</p>   | BASIC STUDIES<br>bubbles<br>experimental   |
| J-9  | <p>Johnson, V E Jr<br/> CAVITATION IN HYDRAULIC STRUCTURES: MECHANICS<br/> OF CAVITATION<br/> Proc ASCE v 89 n HY 3 May 1963 p 251-275<br/> A summary review of the knowledge related to the mechanism of cavitation is<br/> presented. Stability criteria for a spherical gas nucleus as well as the possible<br/> origins of such nuclei are examined. The critical pressure for cavity instability<br/> depends on the type and size of nuclei present in the flow. This critical<br/> pressure in large hydraulic structures may usually be taken as the liquid vapor<br/> pressure, but for small models tested in laboratory facilities, the critical<br/> pressure can be much less than vapor pressure. For streamlined bodies with<br/> unseparated boundary layers, the conditions for cavitation inception may be<br/> predicted by setting the minimum boundary pressure equal to the critical<br/> pressure. This method is usually inadequate for the case of bodies with<br/> separated flows; however, a method of conservatively estimating the<br/> conditions for cavitation inception in separated flows is presented. The<br/> dynamics of a collapsing cavity are examined, and the influence of the<br/> boundary layer on the types of cavities formed and the resulting damage is<br/> also reviewed. The "scale effects" suggested by the mechanics of the<br/> cavitation process are presented</p> | CAVITATION                                 |
| J-10 | <p>Juliano, David W<br/> REAERATION MEASUREMENTS IN AN ESTUARY<br/> Proc ASCE v 95 n SA 6 Dec 1969 p 1165-1178<br/> Measurements of surface reaeration are presented for the Sacramento-San<br/> Joaquin Delta. Estimates of reaeration were computed from observed diurnal<br/> dissolved oxygen changes in the estuary. The reaeration constants computed<br/> in this manner varied between 0.16 and 3.91 grams per cu m per hr at</p>  | BASIC STUDIES<br>estuaries<br>experimental |

## **J—Continued**

0-percent saturation. Independent in situ measurements using gasometric and disturbed equilibrium methods were conducted for comparison. Reaeration constants varied from 0.64 to 2.84 gm per cu m per hr using the gasometric method. The disturbed equilibrium method yielded reaeration constants between 0.62 and 1.70 gm per cu m per hr. The independent methods showed reaeration constants to be highly variable. Surface turbulence proved to be the most important mechanism controlling reaeration constants in the estuary. Wind velocity was the singularly most significant parameter in causing surface turbulence

## K

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| K-1 | <p>Kalinske, A A<br/> <b>ECONOMIC EVALUATION OF AERATOR SYSTEMS</b><br/>         Environmental Sci Tech v 3 1969 p 229-234<br/>         In an illustrated article the author discusses the principles of design and operation of aerators and aeration systems, and describes methods for evaluating performance. (Water Pollution Abstracts)</p>   | <p><b>EQUIPMENT</b><br/>         economics</p>  |
| K-2 | <p>Kalinske, A A<br/> <b>EVALUATION OF OXYGENATION CAPACITY OF LOCALIZED AERATORS</b><br/>         J Water Pollution Control Federation v 37 n 11 Nov 1965 p 1521-1529<br/>         Theoretical bases for techniques used to evaluate performance of aeration equipment are indicated, and conditions and limitations specified; it is shown that general theory that was developed for absorption of oxygen from air bubbles diffused into aeration basins is based on uniform conditions throughout any liquid volume under consideration; such conditions are not always obtained with localized aerators; therefore, relationships developed for uniform conditions must be used with care (EI 1966)</p>                                  | <p><b>EQUIPMENT</b><br/>         waste treatment<br/>         diffusers</p>   |
| K-3 | <p>Kalinske, A A<br/> <b>SURFACE "AERATORS" FOR ABSORPTION AND DESORPTION OF GASES INTO WATER AND LIQUID WASTES</b><br/>         Water and Sewage Works v 115 n 1 Jan 1968 p 33-37<br/>         Problem of supplying oxygen and removal of carbon dioxide or hydrogen sulfide from water and waste water is discussed and several solutions are detailed; methods for calculation of necessary size of surface aerators, and retention times; aeration of flowing stream and removal of CO<sub>2</sub> from fixed volume of liquid and from flowing liquid (EI 1968)</p>  | <p><b>EQUIPMENT</b><br/>         streams<br/>         waste treatment<br/>         mechanical<br/>         aerators</p> |
| K-4 | <p>Kalinske, A A Shell, G L Lash, L D<br/> <b>HYDRAULICS OF MECHANICAL SURFACE AERATORS</b><br/>         Water and Wastes Eng v 5 n 4 1968 p 65</p>   | <p><b>EQUIPMENT</b><br/>         mechanical<br/>         aerators</p>   |
| K-5 | <p>Kalman, L<br/> <b>ELECTROCHEMICAL MEASUREMENT OF THE OXYGEN CONTENT IN WATER, WASTE WATER, AND SLUDGE</b><br/>         Schweiz Z Hydrol v 31 n 1 1969 p 141-149<br/>         A newly developed apparatus for measuring oxygen concentrations is described. The apparatus works without any membrane, and no maintenance and readjustment is necessary even if it is used in activated sludge. The readings are only slightly affected by salt concentrations and pH of the medium. Practical experience with the use of the apparatus at the Horgen sewage treatment plant is reported. The application of the apparatus for continuous control of oxygen transfer in aeration basins by using different aeration systems is mentioned</p> | <p><b>DO ANALYSIS</b><br/>         instrumentation</p>  |
| K-6 | <p>Kaplovsky, A J Walters, W R Sosewitz, B<br/> <b>ARTIFICIAL AERATION OF CANALS IN CHICAGO</b><br/>         J Water Pollution Control Federation v 36 n 4 Apr 1964 p 463</p>   | <p><b>EQUIPMENT</b><br/>         streams</p>  |



## K—Continued

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| K-7  | <p>Kaplovsky, A Joel<br/> discussion of <b>CHANGES IN WASTE ASSIMILATION<br/> CAPACITY RESULTING FROM STREAMFLOW REGULATION</b><br/> by R. A. Vanderhoof<br/> U S Dept Health Education Welfare Symposium on Streamflow Regulation for<br/> Quality Control Public Health Service Pub No 999-WP-30 Jun 1965<br/> p 146-151<br/> Gives a concise definition of assimilative capacity and questions the generally<br/> accepted concept that increased flow improves water quality; the important<br/> question is whether the loss of stabilization time within a given estuarine<br/> segment is sufficiently compensated by the <i>lower concentration buildup level</i><br/> induced by an increase in flow</p> | <p><b>BASIC STUDIES</b><br/> streams</p>  |
| K-8  | <p>Kehr, Robert W<br/> <b>MEASURE OF NATURAL OXIDATION IN POLLUTED<br/> STREAMS. IV. Effect of Sewage on Atmospheric<br/> Reaeration Rates under Flow Conditions</b><br/> Sewage Works J v 10 n 2 1938 p 228-240</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> reaeration<br/> oxidation</p> |
| K-9  | <p>Kerri, K D<br/> <b>A DYNAMIC MODEL FOR WATER QUALITY CONTROL</b><br/> J Water Pollution Control Federation<br/> v 39 n 5 May 1967 p 772</p>  | <p><b>GENERAL</b></p>   |
| K-10 | <p>King, D L<br/> <b>HYDRAULICS OF STRATIFIED FLOW—SECOND PROGRESS<br/> REPORT—SELECTIVE WITHDRAWAL FROM RESERVOIRS</b><br/> USBR Denver Colo Report No Hyd-595 Sep 1969</p>  | <p><b>BASIC STUDIES</b><br/> reservoirs<br/> theoretical<br/> experimental</p>            |
| K-11 | <p>King, H R<br/> <b>DESIGN OF AIR DISTRIBUTION SYSTEMS FOR<br/> ACTIVATED SLUDGE PLANTS</b><br/> Water Works and Sewage v 91 1944</p>  | <p><b>EQUIPMENT</b><br/> waste treatment</p>  |
| K-12 | <p>King, Henry R<br/> <b>MECHANICS OF OXYGEN ABSORPTION IN SPIRAL<br/> FLOW AERATION TANKS, EXPERIMENTAL WORK</b><br/> Sewage and Ind Wastes v 27 n 9 1955 p 1007-1026</p>  | <p><b>EQUIPMENT</b><br/> waste treatment<br/> diffusers</p>                               |
| K-13 | <p>Kishinevski, M<br/> <b>TWO APPROACHES TO THE THEORETICAL ASPECTS<br/> OF GAS ABSORPTION</b><br/> J of Applied Chem USSR Sep 1955 p 881 In Russian</p>  | <p><b>BASIC STUDIES</b><br/> theoretical<br/> reaeration</p>                              |
| K-14 | <p>Kitrell, F W<br/> <b>EFFECTS OF IMPOUNDMENTS ON DISSOLVED OXYGEN<br/> RESOURCES</b><br/> Sewage and Ind Wastes v 31 n 9 Sep 1959 p 1065-1078<br/> Discusses the formation and persistence of stratification in reservoirs.<br/> Discusses stratification in impounded water, effects on dissolved oxygen, and<br/> theoretical energy requirements for mixing stratified reservoirs 1 to 25<br/> kwhr/ac of surface per year. 30,000 acres, 1,500,000 acre-ft \$5,850/yr</p>   | <p><b>BASIC STUDIES</b><br/> reservoirs<br/> theoretical</p>                              |

## K—Continued

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| K-15 | <p>Kitrell, F W<br/> <b>THERMAL STRATIFICATION IN RESERVOIRS</b><br/>         U S Dept Health Education Welfare Symposium on Streamflow Regulation for<br/>         Quality Control Public Health Service Pub No 999-WP-30 Jun 1965<br/>         p 57-76<br/>         Discusses temperature stratification in reservoirs, patterns of summer and<br/>         winter stratification, and current tilted thermoclines</p>  | <p><b>BASIC STUDIES</b><br/>         reservoirs</p>  |
| K-16 | <p>Kleijn, H F W<br/> <b>OXYGEN DEMAND NUMBER—NEW TOOL IN ESTIMATION<br/>         OF OXYGEN DEMAND OF INDUSTRIAL AND<br/>         DOMESTIC WASTE WATER</b><br/>         Air and Water Pollution v 10 n 8 Aug 1966 p 521-535<br/>         New system is evolved for calculation of theoretical oxygen demand that is<br/>         particularly suited for evaluation of industrial waste water, but is valid as well<br/>         in judgment of domestic waste and polluted water; amount of organic<br/>         substances and in general oxidizable substances is expressed in carbon<br/>         g-equivalent, which are so defined that elements nitrogen, sulfur, and<br/>         phosphorus are equivalent with carbon; oxygen demand number of substance<br/>         is number of g-equivalent oxygen needed for complete oxidation of one<br/>         carbon g-equivalent of substance; this is derived from elemental composition.<br/>         24 refs (EI-1967)</p> | <p><b>BASIC STUDIES</b><br/>         waste treatment<br/>         theoretical<br/>         experimental<br/>         oxidation</p> |
| K-17 | <p>Knight, W E<br/> <b>IMPROVEMENT OF THE QUALITY OF RESERVOIR<br/>         DISCHARGES THROUGH CONTROL OF DISCHARGE<br/>         ELEVATION</b><br/>         U S Dept Health Education Welfare Symposium on Streamflow Regulation for<br/>         Quality Control Public Health Service Pub No 999-WP-30 Jun 1965<br/>         p 279-298<br/>         Discusses the concentration of dissolved oxygen in water discharged from a<br/>         reservoir and selective level withdrawals from John H. Kerr Dam, Gaston<br/>         Dam, and Roanoke Rapids Dam on the Roanoke River</p>   | <p><b>BASIC STUDIES</b><br/>         reservoirs<br/>         experimental</p>  |
| K-18 | <p>Koberg, G E<br/> <b>ELIMINATION OF THERMAL STRATIFICATION BY<br/>         AIR-BUBBLING TECHNIQUE IN LAKE WOHLFORD,<br/>         CALIFORNIA</b><br/>         U S Geological Survey—Professional Paper 501-D 1964 p 190-192<br/>         Use of experimental air-bubbling system at Lake Wohlford, Calif., resulted in<br/>         elimination of thermal stratification, definite improvement in taste and odor<br/>         of water, and net reduction in evaporation of 35 acre-ft (5 percent) in 1962<br/>         (EI-1962)</p>   | <p><b>EQUIPMENT</b><br/>         reservoirs<br/>         diffusers</p>   |
| K-19 | <p>Koberg, G E Ford, M E Jr<br/> <b>ELIMINATION OF THERMAL STRATIFICATION IN<br/>         RESERVOIRS AND THE RESULTING BENEFITS</b><br/>         Geological Survey Water—Supply Paper 1809-M 1965<br/>         The use of air bubbling to artificially induce mixing in a lake has been<br/>         successful in several investigations reported in the literature. A detailed study<br/>         of this technique in Lake Wohlford in collaboration with the Escondido<br/>         Mutual Water Co. of Escondido, Calif., is presented.</p>  | <p><b>EQUIPMENT</b><br/>         reservoirs<br/>         diffusers</p>   |

## K—Continued

The results of the Lake Wohlford study indicate that the air-bubbling system is economically feasible to remove undesirable taste and odors from the water used for domestic purposes and to increase the dissolved-oxygen concentration in the hypolimnion of the lake. The results also indicate that the elimination of thermal stratification can reduce evaporation. The elimination of thermal stratification in Lake Wohlford during May, June, and July reduced the evaporation 15 percent. Although the evaporation was increased 9 percent in September, October, and November, the net reduction for the 6 months was about 6 percent.

The Lake Wohlford study and other tests cited have not presented enough data to define criteria for design of an air-bubbling system for a thermally stratified reservoir of a given capacity. Further studies are needed on larger reservoirs before design criteria can be established

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| K-20 | <p>Kolbe, F F<br/> <b>ARTIFICIAL OXYGEN REGENERATION AT GOREANGAB DAM</b><br/>           The Civil Engr of So Africa v 6 1964<br/>           Reports on use of air bubble gun to mix a reservoir to increase oxygen content</p>   | <p><b>EQUIPMENT</b><br/>           reservoirs<br/>           hydraulic guns</p>   |
| K-21 | <p>Kothandaraman, V Ewing, B B<br/> <b>A PROBABILISTIC ANALYSIS OF DISSOLVED OXYGEN—<br/>           BIOCHEMICAL OXYGEN DEMAND RELATIONSHIP IN<br/>           STREAMS</b><br/>           J Water Pollution Control Federation v 41 1969 p R73-R90<br/>           Statistical analysis of the relation between dissolved oxygen and BOD in streams has shown that variations in the values of the deoxygenation and reaeration coefficients have a significant effect on the prediction of dissolved-oxygen level in polluted streams, and the error caused by the variations in these coefficients increases with increase in temperature. The most probable value for the oxygen deficit predicted by the probabilistic model using the Monte Carlo simulation techniques was found to be a better estimate than the values predicted by the conventional deterministic methods</p> | <p><b>BASIC STUDIES</b><br/>           streams<br/>           experimental<br/>           reaeration<br/>           oxidation</p>   |
| K-22 | <p>Krenkel, P A<br/> <b>TURBULENT DIFFUSION AND THE KINETICS OF<br/>           OXYGEN ABSORPTION</b><br/>           PhD Thesis U of Calif 1960</p>  | <p><b>BASIC STUDIES</b><br/>           streams<br/>           theoretical<br/>           experimental<br/>           reaeration</p> |
| K-23 | <p>Krenkel, Peter A Orlob, Gerald T<br/> <b>TURBULENT DIFFUSION AND THE REAERATION<br/>           COEFFICIENT</b><br/>           Proc ASCE v 88 n SA 2 Mar 1962 p 53-83<br/>           Reports on study of oxygen absorption as related to concepts of turbulent flow, explanation of mechanism causing transfer of oxygen into water, and development of a practical method of estimating oxygen transfer rates in open channel flow using easily obtained hydraulic parameters. Experimental reaeration coefficient and longitudinal mixing coefficient show a direct correlation between parameters when depth of flow is taken as a measure of eddy size. Transfer of oxygen molecules into a liquid is explained by the kinetic gas theory assuming only oxygen molecules with sufficient activation energy would be absorbed by the liquid</p>                                | <p><b>BASIC STUDIES</b><br/>           streams<br/>           theoretical<br/>           experimental<br/>           reaeration</p> |

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| K-24 | <p>Krenkel, P A Williams, H E<br/> discussion to PREDICTION OF STREAM REAERATION<br/> RATES by M. A. Churchill<br/> Proc ASCE J Sanitary Eng Div Apr 1963</p>  | <p>BASIC STUDIES<br/> streams<br/> experimental<br/> reaeration</p>                                  |
| K-25 | <p>Krenkel, Peter A Cawley, William A Minch, Virgil A<br/> THE EFFECT OF IMPOUNDING RESERVOIRS ON RIVER<br/> WASTE ASSIMILATIVE CAPACITY<br/> J Water Pollution Control Federation Sep 1965 p 1203-1217<br/> Reduction of the waste assimilative capacity of reservoirs is mainly caused by<br/> inherent low DO in reservoirs, peaking power operations, and stratified flow<br/> conditions induced by cooling water discharge from a steam electrical<br/> generating plant. Studies were conducted on Coosa River, Ga. at the Georgia<br/> Kraft Mill, Mayos Bar, Weiss Reservoir, and Allatoona Reservoir</p> | <p>BASIC STUDIES<br/> reservoirs<br/> experimental</p>   |
| K-26 | <p>Krenkel, P A Thackston, E L Parker, F L<br/> THE INFLUENCE OF IMPOUNDMENTS ON WASTE<br/> ASSIMILATIVE CAPACITY<br/> Proc of the Speciality Conf on Current Res into the Effects of Reservoirs on<br/> Water Quality ASCE Portland Oreg Jan 1968</p>   | <p>BASIC STUDIES<br/> reservoirs<br/> streams<br/> theoretical<br/> experimental<br/> reaeration</p> |
| K-27 | <p>Krishnamurthi, S Kumar, R Kuloor, N R<br/> FORMATION OF BUBBLES<br/> Chem and Process Eng v 49 n 1 Jan 1968 p 91-97, 100<br/> Many operations, particularly distillation, require knowledge of sizes of<br/> bubbles; classical studies and models of bubble formation under constant<br/> flow conditions are examined, and new model is developed from empirical<br/> considerations, showing bubble volume (EI 1968)</p>   | <p>BASIC STUDIES<br/> bubbles<br/> experimental</p>  |

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| L-1 | <p>Lackey, Robert T<br/> <b>EFFECTS OF ARTIFICIAL DESTRATIFICATION ON<br/>         PARVIN LAKE, COLORADO</b><br/>         Progress Report Project F-46-R-1 Colorado State University May 1970<br/>         Reports use of "Helixor" device for destratification of small lake to prevent<br/>         winterkill of fish</p>  | <p><b>EQUIPMENT</b><br/>         reservoirs<br/>         diffusers</p>                             |
| L-2 | <p>Lamb, M<br/>         discussion of <b>MECHANISM OF GAS ABSORPTION BY<br/>         TURBULENT LIQUIDS</b> by W. E. Dobbins<br/>         Proc 1st International Conf Water Pollution Res Pergamon Press Ltd London<br/>         England v 2 1964 p 78<br/>         Contains description of transfer from bubbles originating from porous or<br/>         nozzle diffusers. Shows efficiency advantage of porous type over nozzle type.<br/>         Describes full-scale laboratory tests in which diffuser locations were varied</p>   | <p><b>EQUIPMENT</b><br/>         diffusers</p>   |
| L-3 | <p>Langbein, W B Durum, W H<br/> <b>THE AERATION CAPACITY OF STREAMS</b><br/>         U S Geological Survey Circular No. 542 1967<br/>         Examines the variations in the coefficient of reaeration due to velocity,<br/>         depth, and discharge of rivers; computations are made for the tons of oxygen<br/>         per day that could be absorbed by the river for each unit of oxygen less than<br/>         the saturation value</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p> |
| L-4 | <p>Landberg, G G Graulich, B P Kipple, W H<br/> <b>EXPERIMENTAL PROBLEMS ASSOCIATED WITH THE<br/>         TESTING OF SURFACE AERATION EQUIPMENT</b><br/>         Water Res v 3 n 6 Jun 1969<br/>         The method of testing surface aerators by unsteady-state reaeration of water<br/>         at low or zero oxygen concentration is discussed and the assumptions made in<br/>         applying the usual differential equation to calculate the mass-transfer<br/>         coefficient are queried. Possible errors caused by the use of added chemicals<br/>         to reduce the oxygen level, the existence of microscopically entrained gas<br/>         bubbles, and the transport of gas bubbles to regions of significant hydrostatic<br/>         pressures in deep tanks are pointed out. Test data obtained in various<br/>         environmental conditions are described and discussed in relation to published<br/>         work</p> | <p><b>EQUIPMENT</b><br/>         mechanical<br/>         aerators</p>                              |
| L-5 | <p>Laughlin, J E<br/> <b>STUDIES IN FORCE MAIN AERATION</b><br/>         Proc ASCE v 90 n SA 6 Dec 1964 p 13-24<br/>         Studies of an existing system showed air injection into a force main was an<br/>         effective, economical, and reliable measure for controlling sulfides generation.<br/>         Additional benefits included some degree of BOD reduction and removal of<br/>         friction-producing bacterial filaments. Air at the force main outlet was not<br/>         odorous, and contained only trace amounts of hydrogen sulfide. Generation<br/>         of sulfides returned to normal levels a few days after aeration ceased.<br/>         Analytical techniques used may apply elsewhere. The design rationale may be<br/>         of value in other installations in which general conditions are similar</p>  | <p><b>EQUIPMENT</b><br/>         waste treatment<br/>         misc equipment</p>                   |
| L-6 | <p>Leach, L E Duffer, W R Harlin, C C Jr<br/> <b>PILOT STUDY OF DYNAMICS OF RESERVOIR<br/>         DESTRATIFICATION</b><br/>         Robert S. Kerr Water Res Center Ada Okla 1968</p>  | <p><b>BASIC STUDIES</b><br/>         reservoirs<br/>         experimental</p>                      |

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| L-7  | <p>Leary, R D Ernest, L A Katz, W J<br/> <b>EFFECT OF OXYGEN TRANSFER CAPABILITIES AND<br/> WASTE WATER TREATMENT PLANT PERFORMANCE</b><br/> J Water Pollution Control Federation v 40 n 7 Jul 1968 p 1298-1310<br/> Performance of Jones Island Waste Water Treatment Plants, Milwaukee, Wis.,<br/> were reduced because of inadequate oxygen transfer capabilities at one plant<br/> and because of introduction of poor waste-activated sludge from the plant<br/> into another plant. The spiral-flow aeration basin gave the lowest oxygen<br/> transfer of seven patterns tested; the ridge-and-furrow placement was the<br/> most efficient oxygen diffuser system</p> | <p><b>EQUIPMENT</b><br/> waste treatment<br/> diffusers</p>                               |
| L-8  | <p>Le Bosquet, M Jr<br/> discussion of <b>THE OXYGEN SAG AND DO RELATIONSHIPS<br/> IN STREAMS</b> by H. W. Streeter<br/> Oxygen Relationships in Streams Tech Report W58-2 Robert A Taft Sanitary Eng<br/> Eng Center U S Public Health Service</p>   | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> reaeration<br/> oxidation</p> |
| L-9  | <p>Lee, W S<br/> discussion of <b>IMPROVEMENT OF THE QUALITY OF<br/> RESERVOIR DISCHARGES THROUGH TURBINE OR<br/> TAILRACE AERATION</b><br/> U S Dept Health Education Welfare Symposium on Streamflow Regulation for<br/> Quality Control Public Health Service Pub No 999-WP-30 Jun 1965<br/> p 308-312<br/> Cites aeration experiments with Francis turbines at the Wylie Station plant on<br/> the Catawba River, S. C.; reaeration effectiveness depends upon the turbine<br/> characteristics, load being carried, the setting of the wheel above tailwater<br/> elevation, vacuum-breaker arrangement, and the shape and dimensions of the<br/> draft tube</p>         | <p><b>EQUIPMENT</b><br/> streams<br/> turbine injection</p>                               |
| L-10 | <p>Lemke, A A<br/> <b>FLOW OF AIR IN PIPES</b><br/> Sewage and Ind Wastes v 24 1952 p 24</p>  | <p><b>EQUIPMENT</b></p>   |
| L-11 | <p>Lewis Whitman<br/> <b>PRINCIPLES OF GAS ABSORPTION</b><br/> Ind Eng Chem v 16 1924 p 1215-1220<br/> Describes film theory of mass transfer</p>   | <p><b>BASIC STUDIES</b><br/> theoretical<br/> reaeration</p>                              |
| L-12 | <p>Li, P S West, F B Vance, W H Moulton, R W<br/> <b>UNSTEADY STATE MASS TRANSFER FROM GAS<br/> BUBBLES--LIQUID PHASE RESISTANCE</b><br/> AIChE J v 11 n 4 Jul 1965 p 581-587<br/> Theoretical basis for mass transfer from gas bubbles is important for<br/> predicting distillation and absorption efficiencies; liquid-phase, mass-transfer<br/> coefficients were determined for streams of bubbles in water, gases used were<br/> pure oxygen, 10 percent carbon dioxide in air, and 10 percent chlorine in air.<br/> 31 refs (EI 1965)</p>  | <p><b>BASIC STUDIES</b><br/> bubbles<br/> theoretical<br/> experimental</p>               |
| L-13 | <p>Li, W H<br/> <b>UNSTEADY DISSOLVED-OXYGEN SAG IN STREAM</b><br/> Proc ASCE v 88 n SA 3 May 1962 p 75-85<br/> Solution is obtained for distribution of dissolved oxygen in polluted water of<br/> stream in which volume and velocity of flow are steady at any cross section,</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> theoretical<br/> reaeration</p>                 |

## L--Continued

but not necessarily uniform at all cross sections; solution can account for added discharge and pollution along course of streams; in addition, unsteady distribution of dissolved oxygen due to unsteady initial oxygen content and BOD load can be computed (EI 1962)

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| L-14 | <p>Liebman, J C Lynn, W R<br/> <b>THE OPTIMAL ALLOCATION OF STREAM DISSOLVED OXYGEN</b><br/>         Water Resources Res v 2 1966 p 581<br/>         Chem Abstracts v 66 1967 p 1359</p>   | <p><b>BASIC STUDIES</b><br/>         streams</p>   |
| L-15 | <p>Lin, T J Donnelly, H G<br/> <b>GAS BUBBLE ENTRAINMENT BY PLUNGING LAMINAR LIQUID JETS</b><br/>         AIChE J v 12 n 3 May 1966 p 563-571<br/>         Investigation of factors affecting air entrainment process of free, liquid jet plunging into pool of same liquid; entrainment only occurs when average jet velocity exceeds certain value called minimum entrainment velocity; correlation of Weber numbers and Reynolds numbers which permits prediction of minimum entrainment velocity was developed; relevant to pouring of molten glass or polymer solutions, and paint, food, detergent, cosmetics, and pharmaceutical industries. 14 refs (EI 1966)</p>  | <p><b>EQUIPMENT</b><br/>         cascades</p>  |
| L-16 | <p>Londong, D<br/> <b>FLUBWASSERBELUFTUNGEN AN DER LIPPE (River Water Aeration on the Lippe)</b><br/>         Gewässerschutz-Wasser-Abwasser Band 1 Aachen 1968</p>  | <p><b>EQUIPMENT</b><br/>         streams</p>   |
| L-17 | <p>Loucks, D P Lynn, W R<br/> <b>PROBABILISTIC MODELS FOR PREDICTING STREAM QUALITY</b><br/>         Water Resources Res v 2 1966 p 593<br/>         Chem Abstracts v 66 1967 p 1359</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         theoretical</p>  |
| L-18 | <p>Loucks, D P Revelle, C S Lynn, W R<br/> <b>LINEAR PROGRAMMING MODELS FOR WATER POLLUTION CONTROL</b><br/>         Management Sci v 14 n 4 Dec 1967 p B-166-81<br/>         Two linear programming models are presented for determining amount of waste water treatment required to achieve at minimum cost any particular set of stream dissolved oxygen standards within river basin; derived from generalized Streeter-Phelps differential equations used to describe rates of dissolved oxygen depletion and recovery of streams, these models are adaptable to any river basin configuration; they can be used not only in determining system costs for various quality standards but also for measuring cost sensitivity to changes in stream and waste-water flows and treatment facility location; example illustrates use of these models (EI 1968)</p> | <p><b>BASIC STUDIES</b><br/>         streams<br/>         theoretical<br/>         reaeration<br/>         oxidation</p> |
| L-19 | <p>Love, S K<br/> <b>RELATIONSHIP OF IMPOUNDMENT TO WATER QUALITY</b><br/>         J American Water Works Assoc v 53 n 5 May 1961 p 559-568<br/>         Describes oxygen depletion conditions in the hypolimnion of a reservoir</p>   | <p><b>BASIC STUDIES</b><br/>         reservoirs<br/>         experimental<br/>         oxidation</p>                     |

## **L—Continued**

- L-20** Love, S K Slack, K V  
**CONTROLS ON SOLUTION AND PRECIPITATION IN  
RESERVOIRS**  
U S Dept Health Education Welfare Symposium on Streamflow Regulation for  
Quality Control Public Health Service Pub No 999-WP-30 Jun 1965  
p 97-128  
Examines the environmental events bringing about encounters with water and  
new solid phases or between unlike water masses in reservoirs with a detailed  
discussion of the resulting chemical reactions
- L-21** Lueck, B F Wiley, A J Scott, R H Wisniewski, T F  
**DETERMINATION OF STREAM PURIFICATION CAPACITY**  
Sewage and Ind Waste v 29 Sept 1957 p 1054
- BASIC STUDIES**  
reservoirs
- BASIC STUDIES**  
streams  
experimental  
reaeration



## M

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| M-1 | <p>Mackenthun, K M</p> <p><b>THE EFFECTS OF NUTRIENTS ON PHOTOSYNTHETIC OXYGEN PRODUCTION IN LAKES AND RESERVOIRS</b></p> <p>U S Dept Health Education Welfare Symposium on Streamflow Regulation for Quality Control Public Health Service Pub No 999-WP-30 Jun 1965 p 205-220</p> <p>Biological activity influences chemical parameters including dissolved oxygen; it is governed by temperature and stimulated by nutrients</p>  | <p><b>BASIC STUDIES</b></p> <p>reservoirs</p> <p>experimental</p> <p>photosynthesis</p>           |
| M-2 | <p>Malz, F Bischofsberger</p> <p><b>UEBER DIE ANWENDUNG POROESER PASTIKMATERIALIEN ALS BELUEFTUNGSKOERPER IN BELEBUNGSANLAGEN</b></p> <p>Gas- u Wasserfach v 102 n 44 Nov 1961 p 1197-1199</p> <p>Use of porous plastic materials as aerators in activated sludge tanks; efficiency of porous polyvinylchloride or polyester foil in aeration of sewage water; data on loss of pressure depending on velocity of airflow; data on amount of introduced oxygen; plastic aerators can be easily cleaned; this is advantage as compared to ceramic aerators In German (EI 1962)</p>   | <p><b>EQUIPMENT</b></p> <p>waste treatment</p> <p>diffusers</p>                                   |
| M-3 | <p>Mancy, K H Okun, D A</p> <p><b>EFFECTS OF SURFACE ACTIVE AGENTS ON AERATION</b></p> <p>Water Pollution Control Federation J v 37 n 2 Feb 1965 p 212-227</p> <p>Study was conducted to analyze theoretically and experimentally effect of surface active agents (SAA) on oxygen transfer kinetics; effect of SAA on oxygen transfer from air to water was studied in aeration vessels of different geometry in which water was stirred at various speeds; gas transfer was postulated as encountering total resistance composed of sum of two main resistances in series, liquid surface resistance and liquid bulk resistance; resistance to gas transfer was defined as being equal to reciprocal of rate constant. 36 refs (EI 1965)</p>  | <p><b>BASIC STUDIES</b></p> <p>waste treatment</p> <p>experimental</p> <p>reaeration</p>          |
| M-4 | <p>Manczak, H</p> <p><b>VERBESSERUNG DER SAUERSTOFFVERHALTNISSE EINES GEBIRGSBACHES MITTELS SOHLENABSTAFFELUNG</b></p> <p>(Improving the Oxygen Content of a Mountain Stream by Means of Steps in the Bed)</p> <p>Osterreichische Wasserwirtschaft 1964 Heft 9/10 In German</p>  | <p><b>EQUIPMENT</b></p> <p>streams</p> <p>cascades</p>  |
| M-5 | <p>Manzack, H</p> <p><b>THE COURSE OF SELF-PURIFICATION PROCESS OF CANALIZED HIGHLY POLLUTED RIVERS</b></p> <p>Water Res v 2 n 1 Jan 1968 p 3-4</p> <p>A study to establish the capacity of self-purification in channeled and unchanneled sections of Odra River, Poland is described. Hydrographic, hydrometric, chemical, and biological measurements in the river showed: (1) ice cover reduced the biochemical processes; (2) the coefficient of oxygen utilization in polluted water was about half that from unpolluted water; (3) this coefficient decreased sharply during the navigable period; (4) the reaeration process was much lower in channeled section of the river than in unchanneled sections; (5) the self-purification capacity was relatively high in unchanneled sections, without ice; (6) the self-purification coefficient decreased in polluted water during summer and autumn only in the areas with high initial BOD values. It is concluded that canalization of Odra River has positive and negative features, of which the weirs which increase the amount</p> | <p><b>BASIC STUDIES</b></p> <p>streams</p> <p>experimental</p> <p>reaeration</p> <p>oxidation</p> |

## M—Continued

of dissolved oxygen is the most important. The channel has negative effects such as accumulation of bottom sediment, hydrogen sulphide, and occurrence of oxygen deficiency

- M-6 Marrucci, G Nicodemo, L  
COALESCENCE OF GAS BUBBLES IN AQUEOUS SOLUTIONS  
OF INORGANIC ELECTROLYTES  
Chem Eng Sci v 22 n 9 Sep 1967 p 1257-1265  
Measurements of average bubble size in bubble column have been taken by means of photographic method; liquid phase consisted of aqueous solution of electrolyte and distributor was porous plate; number of different electrolytes were used, and superficial gas velocity was varied between 0.1 and 1.5 cm/sec; coalescence phenomena which occur near distributor; proposed correlation relates average bubble diameter to gas flow rate and to group of electrolyte properties. 38 refs (EI 1968)
- M-7 Maxworthy, T  
NOTE ON EXISTENCE OF WAKES BEHIND LARGE,  
RISING BUBBLES  
J Fluid Mechanics v 27 pt 2 Feb 1967 p 367-368  
Using simple flow-visualization techniques, it was observed that as large volume of air rises through quiescent liquid it produced well-defined wake and that drag on bubble appears as momentum defect within this wake (EI 1967)
- M-8 McCloy, D  
CAVITATION AND AERATION—EFFECT ON VALVES AND  
SYSTEMS  
Hydraulic Pneumatic Power v 12 n 133-134 Jan 1966 p 32-37 Feb 1966  
p 100-105  
Conditions that give rise to cavitation and aeration and effects of their presence in hydraulic systems are discussed; orifice cavitation and cavitation erosion in valves are studied; theoretical analysis of cavitation occurrence in actuators during step and frequency responses is supported by experimental results (EI 1966)
- M-9 McDonnell, A J Hall, S D  
EFFECT OF ENVIRONMENTAL FACTORS ON BENTHAL  
OXYGEN UPTAKE  
Water Pollution Abstracts Proc 22nd Ind Waste Conf Purdue U  
Eng Extn Ser No 127 1967 p 414-428  
Preliminary results of laboratory experiments on the effect of various factors on the oxygen demand of benthic deposits collected from Spring Creek, a highly eutrophic stream in Pennsylvania, confirmed that the rate of oxygen uptake is dependent on oxygen concentration and independent of sample depth. The presence of measureable densities of macroinvertebrates also has a marked effect, and an attempt was made by a relatively simple procedure to approximate the demands associated with microbial and invertebrate respiration to determine the relative importance of each
- BASIC STUDIES  
bubbles  
experimental
- BASIC STUDIES  
bubbles  
experimental
- CAVITATION
- BASIC STUDIES  
streams  
experimental  
oxidation

## M—Continued

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| M-10 | <p>McDonnell, Archie J Kountz, R Rupert<br/> <b>ALGAL RESPIRATION IN A EUTROPHIC ENVIRONMENT</b><br/>         J Water Pollution Control Federation v 38 n 5 May 1966 p 841-857<br/>         Present-day community development, especially in small watersheds, such as Spring Creek, Penn., has compounded problems of stream pollution criteria. In many stream situations, depletion of dissolved oxygen resources is a result not only of BOD but also of the effect of community respiration. Exactly how much effect each of these factors has on the dissolved oxygen level of the stream is difficult to evaluate. With statistical methods of regression and variance analysis, it was possible to define the BOD parameter as one of secondary engineering significance and to evaluate quantitatively the nocturnal oxygen demands of a heterogeneous stream flora. Community plant respiration varies directly with stream temperature and inversely with streamflow. Chemical analysis of contributing sources indicated nutrient concentrations sufficient to induce and maintain a eutrophic environment. On this basis, where population-to-receiving water resource ratio is high, analysis for significance of parameters other than BOD should be made and the findings manifested in the treatment process. The solution appears to lie in the removal of nitrogen and phosphorus from the waste water treatment plant effluent before it enters the creek waters, which practically implies total exclusion (Jones-Wis) W69-10159</p> | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         respiration</p> |
| M-11 | <p>McKinney, R E Benjes, H H Jr<br/> <b>EVALUATION OF TWO AERATED LAGOONS</b><br/>         Proc ASCE v 91 n SA 6 Dec 1965 p 43-55<br/>         Field studies of two aerated lagoons treating domestic sewage over 2-yr period yielded 63 percent BOD reduction with 1.7 days aeration and 78 percent BOD reduction with 7.1 days aeration; use of oxidation ponds after using aerated lagoons increased BOD reductions to 85 and 88 percent; it appeared that mechanical aerators-mixers could produce complete mixing with from 1/5 to 1/4 hp/1,000 cu ft aeration volume; bacterial cells were primarily responsible for effluent BOD from aerated lagoon; algae were responsible for effluent BOD from oxidation ponds (EI 1966)</p>   | <p><b>EQUIPMENT</b><br/>         waste treatment<br/>         mechanical<br/>         aerators</p>  |
| M-12 | <p>McWhirter, J R<br/> <b>FUNDAMENTAL ASPECTS OF SURFACE AERATOR PERFORMANCE AND DESIGN</b><br/>         Purdue U—Eng Extn Ser 118 1965 p 75-92<br/>         Discussion of several methods for determination of oxygenation; unsteady-state reaeration is most widely used and accepted method; steady-state technique gives results about 10 percent higher than unsteady-state technique; sulfite oxidation data shows higher oxygen uptake rates than steady-state data with different temperature variation and significant variation in oxygen uptake rate with different catalysts. 24 refs (EI 1967)</p>   | <p><b>EQUIPMENT</b><br/>         mechanical<br/>         aerators</p>                               |
| M-13 | <p>Mercier, P Perret, J<br/> <b>AERATION STATION OF LAKE BRET</b><br/>         Monatsbull Schweiz Ver Gas- u Wasserfachm v 29 1949 p 25<br/>         Water Pollution Abstracts v 40 1950 p 533<br/>         Attempts to aerate a stratified lake by withdrawing water, aerating, and returning to the same depth</p>  | <p><b>EQUIPMENT</b><br/>         reservoirs<br/>         misc equipment</p>                         |

## M—Continued

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| M-14 | <p>Mercier, P    Gay, S<br/> <b>EFFECTS OF ARTIFICIAL AERATION ON WATERS OF LAKE BRET</b><br/> Rev Suisse d'Hydrologie v 16 1954 p 2<br/> Reports on aerating water in a stratified lake by withdrawing water, aerating, and returning to same depth</p>   | <p><b>EQUIPMENT</b><br/> reservoirs<br/> misc equipment</p>                |
| M-15 | <p>Metzger, I    Dobbins, W E<br/> <b>THE ROLE OF FLUID PROPERTIES IN GAS TRANSFER</b><br/> Environmental Sci and Tech v 1 1967 p 57</p>   | <p><b>BASIC STUDIES</b><br/> reaeration</p>                                |
| M-16 | <p>Metzger, I<br/> <b>SURFACE EFFECTS IN GAS ABSORPTION</b><br/> Environmental Sci and Tech v 2 1968 p 784</p>   | <p><b>BASIC STUDIES</b><br/> reaeration</p>                                |
| M-17 | <p>Metzger, Ivan<br/> <b>EFFECTS OF TEMPERATURE ON STREAM AERATION</b><br/> Proc ASCE v 94 n SA 6 Dec 1968 p 1153-1159<br/> The effect of temperature on the aeration of receiving waters is often described by an equation of the form <math>K_T = K_{20} \theta^{(T-20)}</math> where <math>K_{20}</math> is the <math>20^\circ</math> value of the absorption coefficient and <math>K_T</math> is the value at some other temperature, T. In the past, <math>\theta</math> has been considered to be a constant with various values assigned to it by different investigators. It is shown that <math>\theta</math> is not a constant but depends on the level of turbulence and temperature. Values of <math>\theta</math> appropriate for streams are determined by using the film penetration model and experimental results. These values are compared with values reported in the literature</p>   | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> reaeration</p> |
| M-18 | <p>Miyamoto, S<br/> <b>A THEORY OF THE RATE OF SOLUTION OF GAS INTO LIQUID</b><br/> Bull Chem Society of Japan v 7 n 1 1932 v 7 n 12 Dec 1932 v 5 n 4 Apr 1930</p>   | <p><b>BASIC STUDIES</b><br/> theoretical<br/> reaeration</p>               |
| M-19 | <p>Morgan, P F<br/> <b>MAINTENANCE OF FINE BUBBLE DIFFUSION</b><br/> Proc ASCE v 84 n SA 2 Apr 1958<br/> As a result of a 2-year laboratory study at the State University of Iowa, it has been confirmed that diffuser media can be clogged externally by a number of specific materials in the tank liquor, and internally by particulate matter in the air supply. Further, it was found that all forms of external clogging are aggravated by particulate matter in the air supply.<br/><br/> Corrective measures are proposed for each of the causes of clogging but because particulate matter is the most important it is recommended that it be corrected first. The commonly accepted standard for air quality of 0.5 mg/1,000 cu ft is shown to be unsatisfactory under certain conditions. A new standard of 0.1 mg/1,000 cu ft is proposed. Plant operating records are presented to show that a clogging problem was eliminated after the installation of precoated bag filters producing air meeting this standard. The corrective measures for other specific causes of clogging can be effectively applied only after the air supply is adequately filtered</p> | <p><b>EQUIPMENT</b><br/> waste treatment<br/> diffusers</p>                |

## M—Continued

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| M-20 | <p>Morgan P F Bewtra, J K<br/> <b>AIR DIFFUSER EFFICIENCIES</b><br/> J Water Pollution Control Federation v 32 n 10 1960 p 1047</p>  | <p><b>EQUIPMENT</b><br/> diffusers</p>                                     |
| M-21 | <p>Morgan, P F Bewtra, J K<br/> <b>DIFFUSED AIR OXYGEN TRANSFER EFFICIENCIES</b><br/> paper presented at Conference on Biological Waste Treatment Manhattan College<br/> 1960</p>  | <p><b>EQUIPMENT</b><br/> waste treatment<br/> diffusers</p>                |
| M-22 | <p>Morgan, P F Bewtra, J K<br/> <b>DETERMINATION OF OXYGEN UPTAKE RATE BY<br/> POLAROGRAPH METHOD</b><br/> J Water Pollution Control Federation v 34 1962</p>  | <p><b>DO ANALYSIS</b><br/> instrumentation</p>                             |
| M-23 | <p>Morris, James S Krenkel, P A Thackston, E L<br/> <b>INVESTIGATIONS ON TURBULENT DIFFUSION IN<br/> INLAND WATERWAYS</b><br/> Tech Report No. 14 Sanitary and Water Res Eng Vanderbilt U Nashville Tenn<br/> 1966</p>   | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental</p>                 |
| M-24 | <p>Morris, J V McGill, L H Rutherford, C C<br/> <b>MECHANICAL AERATORS TESTED AT LONDON'S<br/> "GREENWAY" POLLUTION CONTROL CENTRE</b><br/> Water and Pollution Control v 106 n 1 Jan 1968 p 30-32<br/> Paper summarizes results of program of acceptance tests of mechanical<br/> aerators supplied at London, Ontario, sewage treatment facilities; work<br/> involved reconstruction and renovation of existing primary, aeration and final<br/> tanks to bring their capacity to 7 mgd; economic analysis indicated<br/> desirability of employing mechanical aerators to supply oxygen necessary for<br/> new activated-sludge secondary-treatment plant which would operate as third,<br/> parallel section of total works (EI 1968)</p> | <p><b>EQUIPMENT</b><br/> waste treatment<br/> mechanical<br/> aerators</p> |
| M-25 | <p>Morris, R M<br/> <b>MASS TRANSFER AND BUBBLE SIZES IN<br/> SOLID-LIQUID-GAS SYSTEMS</b><br/> Chem and Ind n 44 Oct 1964 p 1836-1837<br/> Contacting of gas and liquid with suspended solids in vessel with rotating<br/> impeller; applicability to fermentation processes such as yeast and antibiotics<br/> manufacture, aeration of activated sewage sludge, and catalytic<br/> hydrogenation and chlorination reactions; of specific industrial interest is<br/> scrubbing of flue gases (10 percent CO<sub>2</sub>) by means of calcium hydroxide<br/> slurry in agitated vessel, and precipitation of whiting for plastics and paint<br/> industries (EI 1965)</p>  | <p><b>EQUIPMENT</b><br/> waste treatment<br/> misc equipment</p>           |
| M-26 | <p>Mortimer, C H<br/> <b>THE EXCHANGE OF DISSOLVED SUBSTANCES BETWEEN<br/> MUD AND WATER IN LAKES</b><br/> J Ecol v 29 1941 p 280-329; v 30 1942 p 147-201</p>   | <p><b>BASIC STUDIES</b><br/> reservoirs<br/> experimental</p>              |
| M-27 | <p>Muenz, K Marchello, J M<br/> <b>SURFACE MOTION AND GAS ABSORPTION</b><br/> A I Ch E J v 12 n 2 Mar 1966 p 249-253<br/> Influence of small waves on mass transfer from pure gases into water is<br/> investigated; small-amplitude progressive two-dimensional waves are</p>   | <p><b>BASIC STUDIES</b><br/> experimental<br/> reaeration</p>              |

## M—Continued

mechanically generated at liquid surface for wave studies; control experiments with nonwaved surfaces are also conducted; effect of surface motion arising from Marangoni instability is considered for nonwaved surface; effective diffusivity is used to correlate data (EI 1966)

- M-28 Murphy, G I  
EFFECT OF MIXING DEPTH AND TURBIDITY ON THE  
PRODUCTIVITY OF FRESH-WATER IMPOUNDMENTS  
Trans American Fisheries Society v 91 n 1 1962 p 69-76

BASIC STUDIES  
reservoirs

# N

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| N-1 | <p>Nems, E I Tokmakov, V I Chigareva, T S<br/> O ZAVISIMOSTI FORMY POVERKHNOSTNYKH PUZYR'KOV<br/> (KAPEL) OF IKH RAZMERA<br/> Akademiya Nauk Izvestiya Energetika i Transport n 2 Mar-Apr 1967<br/> p 146-149<br/> Shape of surface bubbles as dependent on their size; change of shape of bubbles during growth was studied; it is shown that base of growing bubble first crawls apart but later contracts until onset of breakoff. In Russian (EI 1968)</p>  | <p>BASIC STUDIES<br/> bubbles<br/> experimental</p>                 |
| N-2 | <p>Nesmeyanov, S-A<br/> DONNYE OTLOZHENIYA I KILORODNYI REZHIM VODOEMOV<br/> (Benthic Deposits and the Oxygen Regime of Reservoirs)<br/> Izd-vo Akad Med Nauk USSR Moscow 1950 157 p In Russian</p>   | <p>BASIC STUDIES<br/> reservoirs<br/> oxidation</p>                 |
| N-3 | <p>Nicholas, W R Bewtra, J K<br/> EFFECT OF SUBMERGENCE ON AERATION DEVICES IN<br/> OXGENATION IN AERATION TANKS<br/> presented at the 35th Annual Meeting of the Central States Water Pollution<br/> Control Assoc Duluth 1962</p>   | <p>EQUIPMENT<br/> waste treatment</p>                               |
| N-4 | <p>Nicholas, W R<br/> AERATION SYSTEM DESIGN<br/> presented to the Sanitary Eng Inst U of Wis Madison Wis 1965</p>  | <p>EQUIPMENT<br/> waste treatment<br/> diffusers</p>                |
| N-5 | <p>Novak, R G<br/> TECHNIQUES AND FACTORS INVOLVED IN AERATOR<br/> SELECTION AND EVALUATION<br/> J Water Pollution Control Federation v 40 n 3 pt 1 Mar 1968 p 452-463<br/> Methods, results, and data reliability obtained during in-place, steady-state<br/> evaluation of two different types of aeration equipment for chemical wastes<br/> are presented; oxygen transfer efficiency of installed system of mechanical<br/> aerators was estimated by measuring oxygen uptake and power; COD, BOD,<br/> sludge volume index, suspended solids, and mixed liquor velocity were<br/> evaluated (EI 1968)</p> | <p>EQUIPMENT<br/> waste treatment<br/> mechanical<br/> aerators</p> |
| N-6 | <p>Novotny, V<br/> ON THE DIFFUSION PHENOMENON IN BOUNDARY LAYERS<br/> OF TURBULENT FLOW AND ITS INFLUENCE ON THE<br/> COURSE OF SELF-PURIFICATION OF SMALL STREAMS<br/> Water Res v 2 n 6 1968</p>   | <p>BASIC STUDIES<br/> streams<br/> reaeration</p>                   |

# O

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| <p>O-1 O'Connell, R L Thomas, N A<br/>EFFECT OF BENTHIC ALGAE ON STREAM DISSOLVED OXYGEN<br/>Proc ASCE v 91 n SA 3 Jun 1965 p 1-16<br/>The effects of respiratory oxygen uptake by photosynthetic benthos on the water quality of streams is examined. Methods for evaluating these effects are given together with results obtained in a survey of the Truckee River. The significance of daily minimum dissolved oxygen concentrations in streams is considered and techniques for prediction of this value incorporating benthic algal effects are described</p>  | <p>BASIC STUDIES<br/>streams<br/>experimental<br/>respiration</p>   |
| <p>O-2 O'Connor, D J Dobbins, W E<br/>THE MECHANISM OF REAERATION IN NATURAL STREAMS<br/>Proc ASCE v 82 n SA 6 1956 p 1115<br/><i>Develops a theoretical model for reaeration of a turbulent system</i></p>  | <p>BASIC STUDIES<br/>streams<br/>theoretical</p>                    |
| <p>O-3 O'Connor, D J<br/>THE MEASUREMENT AND CALCULATION OF STREAM REAERATION RATIO<br/>Oxygen Relationships in Streams Tech Report No. W-58-2 Taft Sanitary Eng Center 1958</p>   | <p>BASIC STUDIES<br/>streams<br/>experimental<br/>reaeration</p>    |
| <p>O-4 O'Connor, D J<br/>OXYGEN BALANCE OF AN ESTUARY<br/>Proc ASCE v 86 n SA 3 May 1960<br/>The net seaward movement of organic impurities in estuaries is due to the displacement by the land runoff and to the longitudinal diffusion of the tidal action. The dissolved-oxygen profile depends on the concentration of the organic materials, its rate of oxidation, and the resulting rate of reaeration. The interrelationship among these geophysical and biochemical factors is described by a differential equation under a steady-state condition. The assumption of constant coefficients in the equation is confirmed by the field data from estuarine surveys of the Delaware and the James Rivers. Dissolved-oxygen profiles are calculated from the integrated equation and compared to the measured dissolved-oxygen concentrations. The turbulent diffusion coefficient and the deoxygenation rate are determined from an analysis of survey data and are used in the calculation of the oxygen profiles. The agreement between the calculated profiles and the observed values is sufficiently close to justify the use of the equations for the conditions assumed in the development</p> | <p>BASIC STUDIES<br/>estuaries<br/>theoretical<br/>experimental</p> |
| <p>O-5 O'Connor, D J<br/>TEMPORAL AND SPATIAL DISTRIBUTION OF DISSOLVED OXYGEN IN STREAMS<br/>Water Resources Res v 3 n 1 First Quarter 1967 p 65-79<br/>Geophysical characteristics of drainage basin and biochemical and physical environment of river affect concentration of dissolved oxygen, these factors are embodied in fundamental equation of continuity that describes oxygen balance, variation of fresh-water flow and cross-sectional area is included, as well as various sources and sinks of oxygen—natural and artificial aeration, photosynthetic contribution, bacterial and algae respiration, carbonaceous and nitrogenous oxidation, and benthic deposits (EI 1967)</p>  | <p>BASIC STUDIES<br/>streams<br/>reaeration<br/>oxidation</p>       |



## O—Continued

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| O-6  | <p>Ogunrombi, J A<br/> <b>THE EFFECTS OF BENTHAL DEPOSITS ON THE OXYGEN RESOURCES OF NATURAL STREAMS</b><br/>         Water Pollution Abstracts thesis New York U 1968<br/>         Dissertation Abstracts v 29 n B 1969 p 3343<br/>         Benthaf deposits are known to exert oxygen demands on the overlying water, and it is suggested that this occurs in two ways—by addition of organic matter from the deposits, to the water, thus increasing the BOD of the water; and by the removal of dissolved oxygen from the water to satisfy both the BOD of organic matter in the top aerobic layer and the intermediate COD of products of anaerobic decomposition which diffuse to the aerobic zone from the deeper layers. Laboratory experiments were carried out to verify the existence of these processes and the results indicated that the rate of transfer of organic matter from the benthaf deposits to the supernatant water is smaller than the rate at which dissolved oxygen is abstracted from the water by the deposits. For any sludge depth, the total oxygen demand of the deposit is less than the potential aerobic demand of the sludge</p> | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         oxidation</p>  |
| O-7  | <p>Oldaker, W H Burgun, A A Pahren, H R<br/> <b>PILOT-PLANT STUDY OF BENTHIC OXYGEN DEMAND OF RIVER BOTTOM SEDIMENTS</b><br/>         J Water Pollution Control Federation v 40 n 10 Oct 1968 p 1688</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         oxidation</p>                            |
| O-8  | <p>Orlob, G T<br/> <b>EDDY DIFFUSION IN HOMOGENEOUS TURBULENCE</b><br/>         Proc ASCE v 85 n HY 9 Sept 1959 p 75-103</p>   | <p><b>BASIC STUDIES</b><br/>         streams</p>   |
| O-9  | <p>Owens, M Edwards, R W Gibbs, J W<br/> <b>SOME REAERATION STUDIES IN STREAMS</b><br/>         Air and Water Pollution v 8 n 8-9 Sept 1964 p 469-486<br/>         Reaeration coefficients of several reaches of lowland and lake district streams were determined and correlated with some of hydraulic characteristics of streams to see if observed reaeration coefficients agree with those calculated from equations proposed by previous workers; empirical equation is derived from which it is possible to predict reaeration rate which could be expected in rivers from their mean velocities and depths, provided these are within experimentally observed ranges. 27 refs (EI 1965)</p>  | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p> |
| O-10 | <p>Owens, M Knowles, G<br/> <b>THE PREDICTION OF THE DISTRIBUTION OF DISSOLVED OXYGEN IN RIVERS</b><br/>         Water Res v 2 1968 p 20</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         reaeration</p>                           |

## P

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| P-1 | <p>Palladino, A J<br/> <b>INVESTIGATION OF METHODS OF STREAM IMPROVEMENT</b><br/> <i>Ind Water and Wastes</i> v 6 n 3 1961 p 87</p> <p>Includes evaluation of turbine venting and diffusers for reaeration of Kalamazoo River in Michigan. The stream is heavily polluted with paper mill wastes. Turbine venting added 2 lb/kwhr, with initial DO less than 1 mg/l. 0.5 mg/l was added through venting. Vent noise indicated undersizing. Drilled pipe diffusers resulted in 1 mg/l pickup with airflow of 570 cfm, or 0.6 mg/l at 325 cfm. Efficiency thus was 1.6 to 1.7 percent, or about 0.5 lb/kwhr. Initial DO was 2 to 3 mg/l</p>   | <p>EQUIPMENT<br/> streams<br/> turbine injection<br/> diffusers</p> |
| P-2 | <p>Panaioti, S S<br/> <b>VLIYANIE RASTVORENNOGO V ZHIDKOSTI GAZA NA KAVITATSIONNYE KHARAKTERISTIKI</b><br/> <i>Izvestiya Vysshikh Uchebnykh Zavedenii Mashinostroyeniya</i> n 4 1968 p 95-100</p> <p>Influence of gas dissolved in liquid upon cavitation characteristics; cavitating flows around cylindrical profile were examined for cases of water-air and water-carbon-dioxide systems; it was found that variations of gas content in water have no practical effect on values of characteristic coefficients of cavitation; applicable to cavitation in pumps. In Russian (EI 1968)</p>   | <p>CAVITATION</p>   |
| P-3 | <p>Parker, Frank L<br/> <b>EDDY DIFFUSION IN RESERVOIRS AND PIPELINES</b><br/> <i>Proc ASCE</i> v 87 n HY 3 May 1961 p 151-171</p> <p>Ocean eddy current diffusion coefficient is a function of eddy size, which is confirmed by reservoir tests with radioactive tracers. Tests of eddy diffusion in pipelines are compared with Taylor's solution; pipeline coefficients are greater because of obstructions and curved sections in the pipe</p>  | <p>BASIC STUDIES<br/> reservoirs<br/> experimental</p>              |
| P-4 | <p>Pasveer, A<br/> <b>A STUDY OF THE AERATION OF WATER</b><br/> <i>Res on Activated Sludge I Sewage and Ind Wastes</i> v 25 n 11 Nov 1953 p 1253</p>  | <p>EQUIPMENT<br/> waste treatment</p>                               |
| P-5 | <p>Pasveer, A Sweeris, S<br/> <b>NEW DEVELOPMENT IN DIFFUSED AIR AERATION</b><br/> <i>J Water Pollution Control Federation</i> v 37 n 9 Sept 1965 p 1267-1274</p> <p>Application of study on oxidation-ditch system for purification of smaller quantities of domestic and industrial wastes to investigate whether it is possible to use diffused-air system in horizontal flow of mixed liquor, steel ring-shaped aeration tank was constructed in which it was possible to achieve horizontal flow by paddle-wheel arrangement; experiments were performed at various velocities of horizontal flow; quantity of oxygen taken up per 100 cm of water-column was determined as percentage from weight of oxygen introduced with air (EI 1966)</p> | <p>EQUIPMENT<br/> waste treatment<br/> diffusers</p>                |
| P-6 | <p>Pasveer, A<br/> <b>CONSIDERATIONS ON EFFICIENCY OF AERATION PROCESS</b><br/> <i>Air and Water Pollution</i> v 10 n 8 Aug 1966 p 477-493</p> <p>Possibility of achieving higher efficiencies in aeration processes than are achieved in practice is considered; according to theory of aeration, besides creation of large interface of water and air, rapid renewal of this interface is also of great importance; it is found that in methods of diffused air aeration, only 10 percent of gross energy expended is used for surface creation and surface renewal; improvement in diffused air efficiency could be achieved by</p>  | <p>EQUIPMENT<br/> waste treatment<br/> diffusers</p>                |

## P--Continued

avoiding "spiral flow" and "ridge and furrow" systems by means of "horizontal flow" system and by using smaller air bubbles. 26 refs (EI 1967)

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|------|--|---|
| P-7  | Patriarche, Mercer H<br><b>AIR-INDUCED WINTER CIRCULATION OF TWO SHALLOW MICHIGAN LAKES</b><br>J Wildlife Management v 26 1961 p 289   | <b>EQUIPMENT</b><br>reservoirs<br>diffusers                   |
| P-8  | Patterson, Calvin C Gloyna, Earnest F<br><b>DISPERSION MEASUREMENT IN OPEN CHANNELS</b><br>Proc ASCE v 91 n SA 3 Jun 1965  | <b>BASIC STUDIES</b><br>streams<br>experimental               |
| P-9  | Pence, G D Jeglie, J M Thomann, R V<br><b>TIME-VARYING DISSOLVED OXYGEN MODEL</b><br>Proc ASCE v 94 n SA 2 1968 p 381  | <b>BASIC STUDIES</b><br>streams<br>reaeration                 |
| P-10 | Pearson, E A<br>discussion of THE MEASUREMENT AND CALCULATION OF STREAM REAERATION RATIO by D. J. O'Connor<br>Oxygen Relationships in Streams Tech Report No. W-58-a2 Taft Sanitary Eng Center 1958  | <b>BASIC STUDIES</b><br>streams<br>experimental<br>reaeration |
| P-11 | Peskin, R L<br><b>LAWS OF DISPERSION</b><br>Water Resources Research Institute Report Rutgers Univ Oct 1969<br>Two problems on the laws of dispersion for materials such as small particles and gas bubbles in turbulent streams are considered. After discussing the mechanisms of single-particle dispersion, a statistical approximation model is used to calculate two-particle dispersion. Specifically, the Eulerian fluid velocity which appears in the equation of motion of a small particle is replaced by a random best estimate. This estimate is obtained by prediction techniques using specified statistical properties of the turbulence field. The second problem considered is that of gas bubble dispersion. An approximate analysis is used to estimate the spread of bubbles from a line source of bubbles. Buoyancy and turbulence inhomogeneity effects, which result in a bubble size segregation, are evaluated | <b>BASIC STUDIES</b><br>theoretical<br>reaeration             |
| P-12 | Pfeffer, John T<br><b>EVALUATION OF AERATOR CAPABILITIES FOR WASTE WATER TREATMENT</b><br>Tappi v 52 n 9 1969 p 1652-1655<br>Studies of aeration systems have shown a need for evaluation of aeration equipment operating under field conditions. Procedures have been developed for rating aerators, by using clean water as standard test conditions. Studies of the effects of waste water characteristics have shown that the oxygen transfer capacity of an aeration system can be significantly changed from the rated capacity. These effects are discussed and related to industrial waste water flows, particularly pulp and paper. Techniques for evaluation of systems operating under field conditions have been developed. These techniques are discussed and results of field studies are presented. Procedures for the determination of correction factors are given  | <b>EQUIPMENT</b><br>waste treatment                           |

## P—Continued

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| P-13 | <p>Pfeffer, J T Hart, F C Schmid, L A<br/> <b>FIELD EVALUATION OF AERATORS IN ACTIVATED<br/>         SLUDGE SYSTEMS</b><br/>         Water and Sewage Works v 115 1968 p 520</p>   | <p><b>EQUIPMENT</b><br/>         waste treatment</p>                      |
| P-14 | <p>Phelps, E B<br/> <b>STREAM SANITATION</b><br/>         John Wiley and Sons, Inc New York N Y 1944</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         reaeration</p>  |
| P-15 | <p>Plateau, J A F<br/> <b>STATIQUE DES LIQUIDS</b><br/>         Paris 1873 v 1 c 5<br/>         Presents the laws of bubble geometry based on minimizing surface area of liquid films; the laws are: 3, and only 3, foam lamellae meet at an edge—the 3 coplanar angles at which they are inclined to each other are all equal, each is 120° In French</p>   | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         theoretical</p> |
| P-16 | <p>Poon, C P C<br/> <b>THEORETICAL CONCEPT OF OXYGEN TRANSFER IN<br/>         GAS BUBBLE AERATION SYSTEM</b><br/>         Water and Sewage Works v 113 Nov 30 1966 p R200-202 204-205<br/>         Proposed theory and mathematical treatment of gas transfer process is presented with statistics of molecular motion and turbulent diffusion; single gas-liquid boundary layer is considered instead of two films which have been generally accepted as controlling factors; readily soluble gas is one which as high <math>\alpha</math>-value, specifying fraction of gas molecules striking bubble wall and condense; therefore thickness of liquid film—turbulent diffusion zone in this theory, controls rate of absorption since it will be slower step; on the other hand, less soluble gas will be limited by thickness of gas-film, <math>\alpha</math>-value in theory, and not by liquid film; proposed theory is more direct and easier to be followed (EI 1967)</p> | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         theoretical</p> |
| P-17 | <p>Poon, C P C Campbell, H<br/> <b>DIFFUSED AERATION IN POLLUTED WATER</b><br/>         Water and Sewage Works v 114 n 12 Dec 1967 p 461-463<br/>         Effect of dissolved chemicals in water on transfer process was studied in series of experiments; pyrex column of 5-1/2 in ID was built 12 feet high measured from top of diffusers to top of column; fritted glass diffusers were installed at bottom of column; temperature of water in column for all experiments was automatically held constant using thermostat with immersion heater; experiments were run at water depth of 7.0 ft above top of diffuser and rate of airflow was maintained at constant of 300 cc/min; temperature was held constant at 20° C or otherwise diffusion coefficient was corrected to 20° C. 10 refs (EI 1968)</p>  | <p><b>EQUIPMENT</b><br/>         diffusers</p>                            |
| P-18 | <p>Poon, C P C Lee, F<br/> <b>SURFACE AERATION BY MECHANICAL AGITATION</b><br/>         Water and Sewage Works v 116 n 7 Jul 1969 p 262<br/>         In experiments with mechanical aeration in laboratory-scale circular tanks, various factors affecting the oxygen absorption coefficient were studied, including the degree of submergence of the rotor blades, rotor speed, and water depth. The overall oxygen absorption coefficient increase significantly with increasing rotor size at high speeds</p>   | <p><b>EQUIPMENT</b><br/>         mechanical<br/>         aerators</p>     |

## P—Continued

- P-19 Poston, H W Ownbey, C R  
THE GREAT LAKES WATER RESOURCE  
J American Water Works Assoc v 60 n 1 Jan 1968 p 15-20  
The problems of eutrophication, increase of chemicals, and oxygen depletion are discussed. Measures presently being taken are presented, including Federal grants. Legally, the judicial process has been inadequate to resolve the problems created by the conflicting interest for the use of the water. The Great Lakes belong to all the people of the United States and Canada, but the problem is who should be the custodian of these waters. A Board of Directors, similar to that governing the Tennessee Valley Authority, is proposed. The representation of the states bordering the Great Lakes, the Province of Ontario, and the Governments of the United States and Canada is discussed
- P-20 Purdy, R W  
WHAT DO WE KNOW ABOUT NATURAL PURIFICATION?  
Proc ASCE v 94 n SA 1 Feb 1968 p 1-11  
It is possible to predict effect of stabilization of oxidizable substances on DO content of stream; time of flow can be calculated on basis of displacement of occupied channel volume but calculations should be checked by observing time of passage with fluorescent dye; effect of sludge deposits, biological extraction and accumulation, and oxidation of nitrogenous substances on DO balance in stream can be evaluated and examples of such evaluations are presented. 11 refs (EI 1968)
- GENERAL
- BASIC STUDIES  
streams  
reaeration

## Q

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|-----|---|---|
| Q-1 | <p><b>Quigley, J T</b><br/> <b>EFFECTIVENESS AND COSTS OF VARIOUS TYPES OF MECHANICAL REAERATION FOR RIVERS AND IMPOUNDMENTS</b><br/>         Unpublished paper presented to the Seminar in Water Resources Planning<br/>         U of Wis Madison Wis Apr 1969<br/>         Describes problem of generalizing four alternative aeration systems for purposes of cost comparison: (1) porous diffuser system, (2) perforated tubing system, (3) mechanical surface aerator, and (4) hydraulic turbine injection</p>   | <p><b>EQUIPMENT</b><br/>         streams<br/>         reservoirs<br/>         turbine injection<br/>         diffusers<br/>         mechanical aerators<br/>         economics</p>                      |
| Q-2 | <p><b>Quirk, T P Eder, L J</b><br/> <b>EVALUATION OF ALTERNATIVE SOLUTIONS FOR ACHIEVEMENT OF RIVER STANDARDS</b><br/>         J Water Pollution Control Federation v 42 n 2 pt 1 1970 p 272<br/>         A river of approximately 170 miles (274 km) in length and 3,500 sq miles (9,965 sq km) in drainage area is studied. The purpose of the study was to: determine the physical characteristics, develop a mathematical simulation model to predict BOD and DO profiles under any condition of flow, temperature, or waste discharge, and application of the model to investigate BOD assimilation capacity under critical weather and flow conditions. The effects of sludge deposits, hydroturbine venting, and flow augmentation are determined. The model also was used to determine the comparative economics of alternative solutions for the achievement of proposed water-quality standards. The effects of channel geometry, sludge composition, location, depth, oxygen uptake rates, point aeration, riverflow, and seiche wave effect were plugged into the model. Seven solution components were analyzed and the results, used by regulatory personnel and industry, culminated in the establishment of a common basis for interpretation of the financial requirements and practical capability of achieving various levels of water quality improvement</p> | <p><b>BASIC STUDIES</b><br/>         streams<br/>         theoretical<br/>         experimental<br/>         reaeration<br/>         oxidation<br/> <b>EQUIPMENT</b><br/>         turbine injection</p> |

## R

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|-----|--|---|
| R-1 | <p>Ragone, Stanley Peters, B J<br/> <b>WATER QUALITY MONITORING FOR WATER QUALITY CONTROL</b><br/>         U S Dept Health Education Welfare Symposium on Streamflow Regulation for Quality Control Public Health Service Pub No 999-WP-30 1965<br/>         Describes submerged weirs at Gaston Dam and Roanoke Rapids Dam designed to prevent discharge of cold, oxygen-deficient water; weirs skim off oxygen-rich surface layers of water and prevent density currents from entering intakes</p>   | <p><b>BASIC STUDIES</b><br/>         reservoirs<br/>         experimental</p>                 |
| R-2 | <p>Rasmussen, D H<br/> <b>PREVENTING A WINTERKILL BY USE OF A COMPRESSED AIR SYSTEM</b><br/>         Progressive Fish Culture v 24 1960 p 185<br/>         Reports on compressed air mixing of lakes to prevent fish winterkill when the lake freezes over and cuts off the oxygen supply</p>  | <p><b>EQUIPMENT</b><br/>         reservoirs<br/>         diffusers<br/>         misc uses</p> |
| R-3 | <p>Redfield, J A Houghton, G<br/> <b>MASS TRANSFER AND DRAG COEFFICIENTS FOR SINGLE BUBBLES AT REYNOLDS NUMBERS OF 0.02-5000</b><br/>         Chem Eng Sci v 20 n 2 Feb 1965 p 131-139<br/>         Simultaneous dilatometric and photoelectric determinations of mass transfer and velocity of rise, respectively, have been made for a single bubbles of CO<sub>2</sub> rising in pure water and aqueous solutions of dextrose; although boundary layer and potential flow models predict orders of magnitude and general trends for drag and mass-transfer coefficients at Re greater than 1, detailed comparison is masked by changes in shape and motion of bubbles as well as presence of turbulence in wake. 35 refs (EI 1965)</p>  | <p><b>BASIC STUDIES</b><br/>         bubbles<br/>         experimental</p>                    |
| R-4 | <p>Reid, L C Jr<br/> <b>AERATED SEWAGE LAGOON IN ARCTIC ALASKA</b><br/>         Western Canada Water and Sewage Conf 17th Annual Convention—Papers Sep 15-17 1965 p 101-113<br/>         Observations and results of study conducted by Arctic Health Research Center, with cooperation of Air Force of Alaskan Air Command, during winter of 1964-65 on aerated sewage pond receiving settled domestic sewage at Eielson Air Force Base; pond is located 25 miles from Fairbanks, in central valley of Alaska area which ordinarily experiences coldest winter temperatures in United States; Air-Aqua System provides aeration and lagoon operates on extended aeration principle; rising action of air bubbles divides lagoon into 15 individual cells which are continually being mixed; activated sludge agglomerates until particles are too large to remain in suspension, whereupon it settles and digests on lagoon floor (EI 1967)</p> | <p><b>EQUIPMENT</b><br/>         waste treatment<br/>         diffusers</p>                   |
| R-5 | <p>Revelle, C S Loucks, D P Lynn, W R<br/> <b>LINEAR PROGRAMMING APPLIED TO WATER QUALITY MANAGEMENT</b><br/>         Water Resources Res v 4 n 1 1968 p 1</p>   | <p><b>GENERAL</b></p>   |
| R-6 | <p>Revelle, C S Loucks, D P Lynn, W R<br/> <b>A MANAGEMENT MODEL FOR WATER QUALITY CONTROL</b><br/>         J Water Pollution Control Federation v 39 n 7 Jul 1967 p 1164</p>  | <p><b>GENERAL</b></p>   |

## R—Continued

- R-7 Riddick, Thomas M  
FORCED CIRCULATION OF RESERVOIR WATERS  
Water and Sewage Works v 104 n 6 1957 p 231-237  
Compressed air mixing of 246 acre-ft reservoir at Ossining, N. Y. completely destratified and recirculated the water almost twice a day
- R-8 Rincke, G Moeller, U  
MESS- UND VERFAHRENSTECHNISCHE MOEGLICHKEITEN  
FUER EINE AUTOMATISCHE REGELUNG DER  
SAUERSTOFFZUFUHR IN BELUEFTUNGSBECKEN  
Vom Wasser v 34 1967 p 297-333  
Measurement and technical process possibilities for automatic control of oxygen supply to aeration basins; literature review of devices for analysis of oxygen contents in aeration basins; first continuous analyzer and controller by G. Stracke is described; effects of various parameters on devices sensitivity, accuracy of commercial-scale tests, and results. 38 refs. In German (EI 1968)
- R-9 Robertson, J M  
CAVITATION IN HYDRAULIC STRUCTURES: SCALE  
EFFECTS INVOLVED IN CAVITATION EXPERIMENTS  
Proc ASCE v 89 n HY 3 May 1963 p 167-180  
The general nature and purpose of experimental studies of cavitation-susceptible hydraulic structures is reviewed. Scale effects are defined as deviations in the cavitation occurrences from the simple concept of cavitation in a liquid of given density and vapor pressure, resulting from other fluid properties and occurrences. For simple bodies, known scale effects are shown to be characterized sometimes by the Reynolds number and sometimes by a dimensional parameter  $V\sqrt{d}$ . The effects of protuberances or roughnesses in terms of boundary-layer thickness and location on the body are indicated as potential sources of large effects. Possible effects of air content on cavitation scaling are also noted
- R-10 Roe, F C  
THE INSTALLATION AND SERVICING OF AIR  
DIFFUSER MEDIUMS  
Water and Sewage Works v 81 1934 p 450
- R-11 Rolley, H L J Owens, M  
OXYGEN CONSUMPTION RATES AND SOME CHEMICAL  
PROPERTIES OF RIVER MUDS  
Water Res v 1 1968 p 759  
Rates of oxygen consumption varying from 0.006 to 0.41 g/m<sup>2</sup>/hr were obtained during an investigation of sediments collected from 74 sites in 12 river systems during January-February and July-August 1966. The distribution of these rates was similar in both surveys and no correlation was found between rates of oxygen consumption and any chemical property of the mud. Strong correlations were obtained between all the chemical properties examined: permanganate value, loss on ignition, and contents of humic acid, org. C, and Kjeldahl N. Deposits in reaches below outfalls from sewage-treatment works operating percolating filters to a nominal effluent standard of 30 mg/l suspended solids and 20 mg/l BOD were not found to differ significantly from those in unpolluted reaches. However, both were significantly different from deposits downstream of outfalls from works using the activated sludge process
- EQUIPMENT  
reservoirs  
diffusers
- DO ANALYSIS  
instrumentation
- CAVITATION
- EQUIPMENT  
diffusers
- BASIC STUDIES  
streams  
experimental  
oxidation



## R—Continued

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|------|---|--|
| R-12 | <p>Ross, Sydney<br/> <b>BUBBLES AND FOAM</b><br/> <i>Ind and Eng Chem</i> v 61 n 10 Oct 1969 p 48-55<br/>                     The general law of bubble geometry takes into account the minimizing of surface area required to contain a given amount of gas at a given temperature and given pressure</p>  | <p><b>BASIC STUDIES</b><br/>                     bubbles<br/>                     theoretical</p>    |
| R-13 | <p>Rozen, A M<br/> <b>PROBLEMY TEORII I INZHENERNOGO RASCHETA<br/>                     PROTESSESOV MASSOOBMENA</b><br/> <i>Khimicheskaya Promyshlennost</i> n 2 Feb 1965 p 5-11<br/>                     Problems of theoretical studies and engineering calculations of mass exchange processes; development of theory of mass exchange; measurements and calculations of contact surface in liquid-gas and liquid-liquid systems; theory of scalar transitions concerned with transversal irregularity in large-diameter apparatus. In Russian (EI 1966)</p>  | <p><b>BASIC STUDIES</b><br/>                     theoretical<br/>                     reaeration</p> |
| R-14 | <p>Ruckenstein, E<br/> <b>A GENERALIZED PENETRATION THEORY FOR UNSTEADY<br/>                     CONVECTIVE MASS TRANSFER</b><br/> <i>Chem Eng Soc (Brit)</i> v 23 n 4 1968 p 363</p>   | <p><b>BASIC STUDIES</b><br/>                     theoretical<br/>                     reaeration</p> |
| R-15 | <p>Ryder, Robert A<br/> <b>DISSOLVED OXYGEN CONTROL IN ACTIVATED SLUDGE</b><br/> <i>Ind Water Eng</i> v 6 n 9 1969 p 43-45<br/>                     The control of the dissolved oxygen concentrations in activated sludge to <math>\pm 0.2</math> percent mg/l results in a continuous response to changing oxygen demands, reduced power consumption, and suppression of filamentous organism growth (sludge bulking). The volume of air directed to three aeration tanks and a post-aeration tank was regulated by butterfly valves responsive to both waste and dissolved oxygen content. The aeration pattern was varied to match the desired aeration profile by adjusting the number of diffusers on each swing header. Sludge bulking was decreased when the dissolved oxygen levels were kept at 0.75 to 1.0 and 0 mg/l in the aeration and sedimentation tanks, respectively. Rohm and Haas (C-7) polyelectrolyte increased the zone settling rate by a factor of 10 in the laboratory and afforded immediate relief to sludge bulking until a stable sludge was obtained by dissolved oxygen control</p> | <p><b>EQUIPMENT</b><br/>                     waste treatment<br/>                     diffusers</p>  |

# S

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|-----|---|--|
| S-1 | Schade, W F Wirts, J J<br>DIFFUSER PLATE CLEANING VERSUS COMPRESSED AIR<br>COST<br>Sewage Works J v 14 1942 p 81  | EQUIPMENT<br>diffusers<br>economics                      |
| S-2 | Schmitz, William R Hasler, Arthur D<br>ARTIFICIALLY INDUCED CIRCULATION OF LAKES BY<br>MEANS OF COMPRESSED AIR<br>Sci v 128 1958 p 1088   | EQUIPMENT<br>reservoirs<br>diffusers                     |
| S-3 | Schrock, V E Perrais, J P<br>DYNAMICS OF BUBBLES IN KNOWN TEMPERATURE<br>DISTRIBUTION<br>Heat Transfer and Fluid Mechanics Inst 19th—Proc Jun 22-24 1966 p 122-147<br>Experimental investigation of bubble growth rates and shapes was conducted using system in which thermal environment is known; this was accomplished by viewing from two directions those bubbles which were first nucleated on transiently heated surface; to vary thickness of superheated liquid layer and steepness of temperature profile at time of nucleation, subcooling, pool pressure, and heating schedule were varied appropriately; this produced superheat thicknesses ranging from 2 to 12 mils while maximum bubble size ranged from 12 to over 110 mils; shape factors were defined and determined over bubble lifetime. 24 refs (EI 1967) | BASIC STUDIES<br>bubbles<br>experimental                 |
| S-4 | Scott, W Foley, A L<br>A METHOD OF DIRECT AERATION OF STORED WATERS<br>Reprinted from Proceedings of the Indiana Academy of Science for 1919, Aug 1921<br>Describes very early application of diffusers to reaeration of a small reservoir  | EQUIPMENT<br>reservoirs<br>diffusers                     |
| S-5 | Scott, R H Wisniewski, T F<br>HYDRO-TURBINE AERATION OF RIVERS WITH SUPPLEMENTAL<br>DATA ON CASCADES AERATION<br>Pulp Paper Mag Canada v 61 Feb 1960 p T45<br>In addition to discussion of turbine venting efficiencies covered in other references by these authors, the paper briefly discusses the determination of true power loss. Although power output is reduced, water is also saved for later generation, thus partially offsetting the cost of power loss. Also discusses aeration by cascades   | EQUIPMENT<br>streams<br>turbine injection<br>cascades    |
| S-6 | Scott, R H Wisniewski, T F Lueck, B F Wiley, A J<br>AERATION OF STREAM FLOW AT POWER TURBINES<br>Sewage and Ind Wastes v 30 n 12 Dec 1958 p 1496-1505<br>Describes results of turbine venting at Pixley Dam on Flambeau River, Wis. in June and July of 1957. Indicated gross gain of 525 to 9,471 lb/day-1,000 cfs. Maximum absorption efficiency of 37.3 percent. Maximum DO gain was 4.87 lb/kwhr of power loss. Injection was in annular space between runner ring and conically shaped part of draft chest which surrounds the runner ring. Turbines were double-runner horizontal type  | EQUIPMENT<br>streams<br>turbine injection                |
| S-7 | Shapiro, J<br>THE CAUSE OF A METALIMNETIC MINIMUM OF<br>DISSOLVED OXYGEN<br>Limnol and Oceanog v 5 n 2 1960 p 216-227   | BASIC STUDIES<br>reservoirs<br>experimental<br>oxidation |

## S—Continued

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| S-8  | <p>Shastry, J S Fan, L T Erickson, L E Yao, Kuan M<br/> discussion of REAERATION PREDICTION IN NATURAL STREAMS<br/> by Edward L. Thackston and Peter A. Krenkel<br/> Proc ASCE v 95 n SA 6 Feb 1969 p 1186-1202</p>   | <p>BASIC STUDIES<br/> streams<br/> reaeration</p> |
| S-9  | <p>Shaver, J W Canter, L W Rowe, D R<br/> PERFORMANCE STUDY OF MUNICIPAL EXTENDED<br/> AERATION PLANT<br/> Pub Works v 99 n 3 Mar 1968 p 85-87 148<br/> Study involved comprehensive examination of performance of extended<br/> aeration modification of activated sludge process in plant treating domestic<br/> waste water from Harahan, La.; plant performance was evaluated by<br/> examining coliform reduction, aeration tank oxygenation resulting from two<br/> air-flow rates, and overall BOD and suspended solids removal efficiencies (EI<br/> 1968)</p>  | <p>EQUIPMENT<br/> waste treatment</p>             |
| S-10 | <p>Sibiryakov, M A<br/> SANITARNAYA KHARSKTERISTIKA, ETC<br/> (Sanitary Characteristics of Reservoirs)<br/> Kizucheniyyu kislorodnogo rezhima vodoemov Sb (Towards the analysis of<br/> the oxygen regime of reservoirs Coll)<br/> Trudy AMN SSSR v 10 1951 p 14-43 In Russian</p>  | <p>BASIC STUDIES<br/> reservoirs</p>              |
| S-11 | <p>Sideman, S Hortacsu, O Fulton, J W<br/> MASS TRANSFER IN GAS-LIQUID CONTACTING SYSTEMS<br/> Ind and Eng Chem v 48 n 7 Jul 1966 p 32-47<br/> Available studies on mass transfer in gas-liquid contacting systems have been<br/> critically reviewed; primary weakness in these studies is fact that their<br/> correlations are limited to their particular pieces of equipment and ranges of<br/> operating conditions; therefore, attempt has been made to organize<br/> information into general framework in order to give better insight and<br/> understanding to subject; ranges of applicability of these studies have been<br/> pointed out, and general correlations have been suggested. 54 refs (EI 1967)</p> | <p>GENERAL<br/> reviews</p>                       |
| S-12 | <p>Simonsen, R N<br/> AIR FLOTATION DEOILS SOHIO EFFLUENT<br/> Oil and Gas J v 60 n 21 May 21 1962 p 146-148 152-154<br/> Air flotation in combination with chemical flocculation cuts oil in effluent to<br/> less than 10 ppm; at one location packaged unit of total pressurization type<br/> guards plant effluent discharging to city sewer; at another refinery two-stage<br/> API separator was redesigned to provide air flotation unit of recycle type<br/> with 3,000 gpm capacity; third installation was made to prevent visible oil<br/> films on receiving stream passing through residential and rural areas (EI 1962)</p>   | <p>EQUIPMENT<br/> misc uses</p>                   |
| S-13 | <p>Simonsen, R N<br/> REMOVE OIL BY AIR FLOTATION<br/> Hydrocarbon Processing and Petroleum Refineries v 41 n 5 May 1962 p 145-148<br/> Three refineries have dissolved air flotation units of different types in<br/> operation; air flotation was selected over more conventional flocculation and<br/> sedimentation process for secondary oil removal because of anticipated<br/> smaller equipment sizes and costs, ability to handle varying feed without<br/> upsets, and easier sludge disposal; principles of air flotation; conversion of<br/> API-type converter to air flotation process; summary of performance (EI<br/> 1962)</p>   | <p>EQUIPMENT<br/> misc uses</p>                   |

## S—Continued

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|------|---|--|
| S-14 | Sinkoff, M D Geilker, C D Rennerfelt, J G<br>AN ANALOG COMPUTER FOR THE OXYGEN SAG CURVE<br>Proc ASCE v 84 n SA6 Nov 1958<br>Presents a theory for application of the analog computer to stream pollution problems  | BASIC STUDIES<br>streams<br>theoretical                |
| S-15 | Smirnov, D N Kuz'min, A A Saiti, R N<br>AUTOMATIC CONTROL OF THE AMOUNT OF DISSOLVED<br>OXYGEN IN WASTE WATERS<br>Vodosnabzh Sanit Tekh v 5 1960 p 18-24<br>The apparatus employs the polarographic method and its probe consists of two solid electrodes, Au and Zn, protected by the gas-permeable membranes. The electroelectrolyte between electrodes is 0.1N NaOAc solution with agar agar. Diffusion of oxygen through the membrane causes depolarization of the indicating electrolyte and flow of current in the circuit of the cell. The apparatus can be used in the laboratory as well as under industrial conditions<br>In Russian  | DO ANALYSIS<br>instrumentation                         |
| S-16 | Smith, A<br>SURFACE AERATORS SPIN TO COMEBACK<br>Water and Wastes Eng v 3 n 12 Dec 1966 p 54-56<br>Economical method for mixing and furnishing oxygen to wastes in tanks and lagoons; selection of aeration units should not be based on oxygen transfer alone; mixing and tank geometry must also be considered; example of activated sludge plant designed to operate at 15° C with 2 mg of dissolved oxygen per liter of mixed liquor; oxygen requirements are 100 lb/hr (EI 1967)   | EQUIPMENT<br>waste treatment<br>mechanical<br>aerators |
| S-17 | Smith, A R<br>TESTING AND RATING SURFACE AERATORS<br>Water and Sewage Works 1964 P R264-268   | EQUIPMENT<br>mechanical<br>aerators                    |
| S-18 | Smith, H L<br>BABINE LAKE BUBBLER SYSTEM<br>Eng J v 51 n 3 Mar 1968 p 39-45<br>Adaption of air bubbling system for melting lake ice in winter is described; system was installed toward north end of lake in British Columbia; air required is supplied by unperforated galvanized steel pipe to drop-off point of western bench; distance is some 1,595 ft from west shore, at which point depth is 161 ft; connection between two 50-ft lengths of polyethylene pipe is made with galvanized steel insert coupling to which pipe ends are clamped with two stainless steel straps; lake area is subjected to winter conditions with lowest ambient temperature of -47° F, and average winter snowfall amounted to 87 in. EIC-68-CIV 3 (EI 1968) | EQUIPMENT<br>reservoirs<br>diffusers<br>misc uses      |
| S-19 | Smutek, Rados Rudis, Miroslav<br>DIFFUSION OF OXYGEN THROUGH THE FREE SURFACE<br>OF A TURBULENT OPEN CHANNEL FLOW<br>(Ceskoslov. Akad. Ved, Prague, Czech.) Acta Tech (Prague) v 14 n 3 1969 p 326-351<br>The transfer rate, K, of oxygen from an oxygen-nitrogen mixture into water flowing under turbulent conditions was studied to determine the mechanism of transfer of oxygen from air into water. To prevent desorption, Na <sub>2</sub> SO <sub>3</sub> was used to bond the oxygen in the water through formation of Na <sub>2</sub> SO <sub>4</sub> . At 18° and surface-active agent (SAA) concentrations of 0.1 mg/l, the  | BASIC STUDIES<br>streams<br>experimental<br>reaeration |

## S—Continued

mass-transfer coefficient for oxygen,  $K_L$ , was  $Au^{0.683}$ , where  $u$  is the flow velocity and  $A$  is a coefficient depending on the surface roughness of the channel. For a smooth surface,  $A = 0.00396$  and increases with increasing roughness. At low SAA level,  $K_L$  is related to  $u$  and to the SAA concentrations by  $K_L = 0.00214 u^{0.76} C_{SAA}^{-0.15}$ . There is a limiting concentration, however, beyond which no further effect exists. It was not possible to construct a physical model for the transfer process in Czech

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| S-20 | <p>Sooky, Attila A<br/> <b>LONGITUDINAL DISPERSION IN OPEN CHANNELS</b><br/> Proc ASCE v 95 n HY 4 Jul 1969 p 1327-1346</p> <p>The effects of cross-sectional geometry and velocity distribution on the dispersion process in straight, uniform open channels with large width-to-depth ratio are investigated. The method of investigation follows Taylor's approach; results apply after the elapse of an initial period during which a constant dispersion coefficient has developed. Under the assumed conditions, the longitudinal dispersion coefficient can be described by a general expression in which the hydraulic radius and the shear velocity are variables. Dispersion varies significantly with cross-sectional shape, width-to-hydraulic radius ratio, and the Reynolds number. The calculated values and pattern of variation are compared to available data for open channels with irregular cross section. 28 refs</p> | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental</p>                 |
| S-21 | <p>Speece, R E<br/> <b>STREAM OXYGENATION WITH THE U-TUBE</b><br/> Proc 7th Annual Sanitary and Water Resources Engineering Conf Vanderbilt Univ May 1968</p>   | <p><b>EQUIPMENT</b><br/> streams<br/> U-tubes</p>                          |
| S-22 | <p>Speece, R E<br/> <b>THE USE OF PURE OXYGEN IN RIVER AND IMPOUNDMENT AERATION</b><br/> Paper 24th Purdue Ind Waste Conf May 1969</p> <p>In many situations, using pure oxygen offers an economically competitive alternative for artificial aeration of rivers and impoundments. Proper design of the oxygen injection system can make using pure oxygen very advantageous and achieve efficient absorption. The judicious selection of an oxygen injection system can result in side benefits and flexibility not possible when using air. The application of pure oxygen is economically competitive with air when attempting to aerate water that is about 50 percent saturated with dissolved oxygen or when attempting to achieve near-saturation concentrations in the effluent. Nitrogen concentration can present a serious problem when fish are involved, but can be alleviated by using pure oxygen</p>                        | <p><b>EQUIPMENT</b><br/> streams<br/> reservoirs<br/> molecular oxygen</p> |
| S-23 | <p>Speece, R E<br/> <b>U-TUBE STREAM RE-AERATION</b><br/> Public Works N Y v 100 n 8 1969 pp 111-113</p> <p>The uses of the U-tube system for aerating streams, its operating characteristics, and a modification using dispersed air injection (see also Wat. Pollut. Abstr., 1969, 42, Abstr. No. 894) are discussed, and arrangements for U-tube aeration at a low dam using the cascade to entrain air and at the discharge point of a stratified reservoir to aerate the waters of the hypolimnion are described</p>   | <p><b>EQUIPMENT</b><br/> streams<br/> U-tubes</p>                          |

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| S-24 | <p>Speece, Richard E Adams, Jack L<br/> <b>U-TUBE OXYGENATION OPERATING CHARACTERISTICS</b><br/> N. Mex. State U Eng Exp Sta Tech Report No. 45 Las Cruces May 1968<br/> Gives oxygen transfer equation and advantages of U-tube aeration. Results are given for an experimental U-tube system; the system favors depths of 40 ft or more, nominal water velocities greater than 6 fps, and minimum diffuser depths in most cases where air is injected</p>  | <b>EQUIPMENT</b><br>U-tubes                                   |
| S-25 | <p>Speece, Richard E Adams, Jack L Wooldridge, Carolyn B<br/> <b>U-TUBE AERATION OPERATING CHARACTERISTICS</b><br/> Proc ASCE v 95 n SA 3 Jun 1969 p 563-574<br/> A modification of U-tube aeration, using low-pressure air injection, was studied on a pilot scale. The pilot U-tube system was made of 4-inch-diameter pipe. Depths of 10, 20, 30, and 40 ft were studied at flow rates up to about 300 gpm. Air injection rates of 5, 10, 15, and 20 percent at different depths were studied. The data were subjected to dimensional analysis and equations were derived for predicting prototype results. The effects of air injection depth, U-tube depth, and nominal water velocity on oxygen transfer economy were evaluated. The results show that water containing zero DO can be 100 percent saturated after one pass through a 40-ft-deep U-tube with 20 percent air injection. In the process of completely saturating water, the U-tube oxygen transfer economy (<math>\#O_2/HP-hr</math>) is about the same as conventional aeration systems transferring oxygen to water with zero DO</p> | <b>EQUIPMENT</b><br>U-tubes                                   |
| S-26 | <p>Speece, R E Orosco, R<br/> <b>DESIGN OF U-TUBE AERATION SYSTEMS</b><br/> Proc ASCE v 96 n SA 3 Jun 1970<br/> Four independent parameters were studied in the design of U-tube aeration systems: (1) Air-water ratio; (2) inlet dissolved oxygen concentration; (3) depth; and (4) water velocity. Each different combination of parameters will result in different capital and operating costs. Outlet dissolved oxygen concentration is reported in this study for the following range of independent parameters: (1) Air-water ratio = 5 to 25 percent; (2) inlet dissolved oxygen = 0 to 100 percent saturation; (3) depth = 20 to 40 ft; and (4) water velocity = 3.6 to 9.2 ft per sec. A computer model of the gas transfer equation, adapted to the U-tube aerator was used to evaluate the reaeration coefficient, <math>K_2</math>. Transfer of gases other than oxygen is analyzed.</p>  | <b>EQUIPMENT</b><br>U-tubes                                   |
| S-27 | <p>Stalman, V<br/> <b>DIE BSK-TURBINE—EIN NEUES HOCHLEISTUNGS—<br/> BELUEFTUNGSSYSGEM DER ABWASSERTECHNIK</b><br/> Gas- u Wasserfach v 106 n 22 Jun 4 1965 p 613-617<br/> BSK turbine, new and highly efficient aeration system for sewage treatment; performance of economic and improved oxygen entrainment of new, Swiss-designed, aerator are presented in form of tabulated data and graphs on sewage and clean water tests; applicability for smaller plants is pointed out; special features are simplicity of installation obviating complicated blower system, no clogging assuring plant safety, extensive foam destruction and easy adaptability to changing and sudden rise in contamination and density level of sewage to be treated In German (EI 1966)</p>   | <b>EQUIPMENT</b><br>waste treatment<br>mechanical<br>aerators |

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| S-28 | <p>Stefan, M J et al<br/> <b>UBER DIE DIFFUSION DER KOHLENSAURE DURCH<br/> WASSER UND ALKOHOL</b><br/> Class II Vienna 1878 p 371 In German</p>  | <p><b>BASIC STUDIES</b><br/> reaeration</p>                 |
| S-29 | <p>Stefan, M J et al<br/> <b>UBER DIE DIFFUSION DER FLUSSIGKEITEN</b><br/> v 79 1879 p 161<br/> This and preceding reference show development of solution to Fick's second law of diffusion In German</p>  | <p><b>BASIC STUDIES</b><br/> reaeration</p>                 |
| S-30 | <p>Steller, K<br/> <b>ZASYSANIE POWIETRZA PRZESZ TURBINE WODNA</b><br/> Polska Adademia Nauk—Prace Instytutu Maszyn Przeplywowych n 33 1966<br/> p 49-63<br/> Air suction by water turbine; results of experiments with model turbines inducing air by leakage and from free surface vortices confirm adverse effect of air contained in water on turbine characteristics; presence of air causes not only drop of efficiency and flow disturbances in rotor and in suction pipe, but also deformation of power characteristics of tested model; vortex and water hammer phenomena observed prove that presence of air influences rise and development of cavitation; observations may be useful for quantitative evaluation of hydraulic losses due to definite amount of air inducted into water flowing through turbine In Polish (EI 1967)</p> | <p><b>EQUIPMENT</b><br/> turbine injection</p>              |
| S-31 | <p>Storch, B<br/> <b>THE DESIGN, CONSTRUCTION, AND OPERATION OF<br/> EXTENDED AERATION PLANTS</b><br/> Water Pollution Control London v 68 1969 p 40-50<br/> The author discusses the design, construction, and operation of extended aeration plants with diffused-air aeration, and stresses the importance of ease of maintenance and control to ensure that the plant will be operated correctly (WPA 1383 Jul 1969)</p>   | <p><b>EQUIPMENT</b><br/> waste treatment<br/> diffusers</p> |
| S-32 | <p>Stratton, F E<br/> <b>NITRIFICATION EFFECTS ON OXYGEN RESOURCES IN<br/> STREAMS</b><br/> Dissertation Abstracts v B27 1967 p 3551<br/> Chem Abstracts v 67 1967 p 7997</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> oxidation</p>     |
| S-33 | <p>Stratton, F E McCarty, P L<br/> <b>PREDICTION OF NITRIFICATION EFFECTS ON DISSOLVED<br/> OXYGEN BALANCE OF STREAMS</b><br/> Environmental Sci and Tech v 1 n 5 May 1967 p 405-410<br/> Method for prediction of dissolved oxygen demand due to biochemical oxidation of inorganic reduced nitrogen compounds utilizes digital computer to estimate nitrifying rate parameters for two-step nitrification process, including kinetic rate constants and initial concentration of nitrifying bacteria; variation of rate constants with temperature is discussed and method for evaluating decay of viable nitriteoxidizing bacteria in absence of its specific substrate is presented; examples comparing predicted and measured nitrogen changes are shown (EI 1967)</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> oxidation</p>     |

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| S-34 | <p>Streeter, H W<br/> <b>MEASURES OF NATURAL OXIDATION IN POLLUTED STREAMS II THE REAERATION FACTOR AND OXYGEN BALANCE</b><br/> Sewage Works J v 7 n 3 May 1935 p 534</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> reaeration</p> |
| S-35 | <p>Streeter, H W Wright, C T Kehr, R W<br/> <b>MEASURES OF NATURAL OXIDATION IN POLLUTED STREAMS, III, AN EXPERIMENTAL STUDY OF ATMOSPHERIC REAERATION UNDER STREAM FLOW CONDITIONS</b><br/> Sewage Works J March 1936 p 282</p>   | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> reaeration</p> |
| S-36 | <p>Streeter, H W<br/> <b>THE OXYGEN SAG AND DISSOLVED OXYGEN RELATIONSHIPS IN STREAMS</b><br/> Oxygen Relationships in Streams Tech Report No. W-58-2 Taft Sanitary Eng Center 1958</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> reaeration<br/> oxidation</p>    |
| S-37 | <p>Streeter, H W Phelps, E B<br/> <b>A STUDY OF THE POLLUTION AND NATURAL PURIFICATION OF THE OHIO RIVER III FACTORS CONCERNED IN THE PHENOMENA OF OXIDATION AND REAERATION</b><br/> Public Health Bull No. 146 U S Public Health Service Washington D C 1925<br/> Reprinted 1958</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> reaeration<br/> oxidation</p>    |
| S-38 | <p>Streif, Abraham<br/> <b>COMPRESSED AIR VERSUS DROUGHT</b><br/> Compressed Air Magazine v 60 1955 p 232<br/> Proposes using compressed air for artificial turnover to reduce summer evaporation losses by bringing cold bottom water to the surface</p>  | <p><b>EQUIPMENT</b><br/> reservoirs<br/> diffusers<br/> misc uses</p>      |
| S-39 | <p>Sullivan, S L Jr Hardy, B W Holland, C D<br/> <b>FORMATION OF AIR BUBBLES AT ORIFICES SUBMERGED BENEATH LIQUIDS</b><br/> A I Ch E J v 10 n 6 Nov 1964 p 848-854<br/> Air bubbles were formed at orifices submerged beneath each of 14 liquids, at various angles of inclination; effect of liquid velocity past horizontal, submerged orifice on formation of air bubbles was determined; bubble formation was correlated with physical variables of system by use of Newton's second law of motion; several chemical processes depend upon contacting liquid as continuous phase with gas as dispersed phase (EI 1966)</p> | <p><b>BASIC STUDIES</b><br/> bubbles<br/> experimental</p>                 |
| S-40 | <p>Susag, R H Polta, R C Schroepfer, G J<br/> <b>MECHANICAL SURFACE AERATION OF RECEIVING WATERS</b><br/> J Water Pollution Control Federation Jan 1966</p>  | <p><b>EQUIPMENT</b><br/> streams<br/> mechanical<br/> aerators</p>         |
| S-41 | <p>Susag, Russell H Robins, Maurice L Schroepfer, George J<br/> <b>IMPROVING RIVER AERATION AT AN UNDERFLOW DAM</b><br/> Proc ASCE v 93 n SA 6 Dec 1967 p 133-144<br/> The aeration occurring in flow through dams can be a significant contribution to the dissolved oxygen resources of a river receiving the oxygen consuming</p>   | <p><b>EQUIPMENT</b><br/> streams<br/> cascades</p>                         |



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organic material of waste waters. Changes in physical or operational characteristics of a dam can affect the rate of aeration. The aeration rate at Lock and Dam No. 2 on the Mississippi River near Hastings, Minn., had been reduced by a factor of three by an increase in tailwater elevation resulting from the construction of another dam downstream. Conversion of the underflow gate structure to an overflow condition by the installation of bulkheads and increasing downstream turbulence almost restored the lost aeration capacity. This study demonstrates that aeration at dams can be improved through changes in operation and indicates that the contribution of dams to river-dissolved oxygen resources should be included in the consideration of dam design and operation

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| S-42 | <p>Symons, J M<br/> <b>WATER QUALITY BEHAVIOR IN RESERVOIRS</b><br/>         Public Health Service Bureau of Water Hygiene Cincinnati Ohio 1969</p>  | <p><b>BASIC STUDIES</b><br/>         reservoirs</p>                    |
| S-43 | <p>Symons, J M Irwin, W H Robinson, E L Robeck, G G<br/> <b>IMPOUNDMENT DESTRATIFICATION FOR RAW WATER<br/>         QUALITY CONTROL USING EITHER MECHANICAL- OR<br/>         DIFFUSED-AIR PUMPING</b><br/>         J American Water Works Assoc Oct 1967</p> <p>Two methods of artificially destratifying lakes and reservoirs are compared; comparisons are based on water quality improvement and hydraulic performance; results of experiments showed that mechanical- and diffused-air pumping broke up thermal stratification patterns in study lake successfully and improved water quality; dissolved oxygen was added to water and sulfides, reduced iron and manganese were oxidized; although some nitrogen and phosphorous was transported to surface layers during mixing, excessive algal growths did not develop in either case. 19 refs</p> | <p><b>EQUIPMENT</b><br/>         reservoirs<br/>         diffusers</p> |
| S-44 | <p>Symons, J M Robeck, G G<br/> <b>IMPOUNDMENT RESEARCH—1, 2</b><br/>         Water and Wastes Eng (formerly Water Works and Wastes Eng) v 3 n 1, 2<br/>         Jan 1966 p 42-44; Feb 1966 p 66-68</p> <p>Results of study conducted on streamflow regulation projects using method of water quality control in which good-quality stored water is added to stream at times of deteriorating stream water quality; experimental equipment used in studies is reported; studies include artificial destratification and biological transformation of nitrogen. 22 refs (EI 1966)</p>   | <p><b>BASIC STUDIES</b><br/>         reservoirs</p>                    |
| S-45 | <p>Symons, J M Weibel, S R Robeck, G G<br/> <b>INFLUENCE OF IMPOUNDMENTS ON WATER QUALITY</b><br/>         U S Public Health Service—Environmental Health Ser Water Supply and Pollution Control—Publ 999-WP-18 Oct 1964</p> <p>Since streamflow regulation is considered as method of water quality control in impoundments, changes in water quality that occur during storage in given environment must be understood and predicted; to aid such study and further research needs, selected references in sanitary engineering and limnology are reviewed with additional section on impoundment releases on downstream water quality as well as operations research for water quality management. 147 refs (EI 1966)</p>   | <p><b>BASIC STUDIES</b><br/>         reservoirs</p>                    |

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| S-46 | <p>Symons, James M Irwin, William H Clark, Robert M Robeck, Gordon G<br/> <b>MANAGEMENT AND MEASUREMENT OF DO IN IMPOUNDMENTS</b><br/> Proc ASCE v 93 n SA 6 proc paper 5688 Dec 1967 p 181-209</p> <p>A basis for the comparison of various mechanical devices used for artificially destratifying impoundments by calculating their hydraulic performance based on impoundment stability is recommended. Three problems with this calculation are discussed to avoid misinterpretation, influence of size and geometry on stability, natural changes in stability with time, and the basic hydraulic inefficiency of spring mixing if cold water is raised. Also, a mathematical model is developed for studying the DO budget in impoundments. A solution to the model is presented, using specially designed DO probe equipment. Finally, data are presented on the destratification of a 2,930-acre-ft impoundment in northern Kentucky by pumping. The hydraulic performance of the pump is calculated and the influence of the mixing on the reduced substances and the DO resources in the impoundment is shown. The most favorable time for destratification is also discussed. A bibliography on artificial destratification is included</p> | <p><b>BASIC STUDIES</b><br/> reservoirs<br/> <b>EQUIPMENT</b><br/> reservoirs<br/> diffusers<br/> pumps</p> |
| S-47 | <p>Symons, J M Irwin, W A Robeck, G G<br/> <b>VERBESSERUNG DER WASSERQUALITAET VON TALSPERREN<br/> DURCH KUENSTLICHE UMSCHICHTUNG</b><br/> Vom Wasser v 34 1967 p 158-174</p> <p>Improvement of reservoir water quality by artificial destratification; commercial-scale experiments on two impoundments, one under study and other undisturbed for comparison purposes, showed high improvement of water quality, due to water destratification by means of pumping and aeration; curves of temperature, oxygen concentration, sulfide and Mn ions concentrations, and phytoplankton, concentration vs time (24 wk) were plotted for depth from 1.5 to 15 m; oxygenation capacity factor and destratification efficiency were used to compute capacity of aeration installation. 15 refs. In German (EI 1968)</p>   | <p><b>BASIC STUDIES</b><br/> reservoirs</p>   |
| S-48 | <p>Symons, James M Irwin, William H Robeck, Gordon G<br/> <b>IMPOUNDMENT WATER QUALITY CHANGES CAUSED BY<br/> MIXING</b><br/> Federal Water Pollution Control Admin Cincinnati Apr 1966</p> <p>Mechanical pumping was used to artificially destratify a 2,380-acre-ft lake in northern Kentucky. The pump drew water from the bottom and discharged it at the surface. Analysis of samples taken weekly, from May 14 to October 29, 1965, throughout the depth of the lake, showed the influence of mixing on water quality. A nearby lake of nearly equal volume, sampled similarly, was the control. Results showed a warming and oxygenating of the lower layers of the test lake that resulted in the precipitation of manganese and the oxidation of sulfide. Mixing neither increased the concentration of any nitrogen form, or the total hydrolyzable phosphorous, nor decreased the clarity in the surface. There was no increase in algal densities. Some data on work requirements and efficiencies are also given</p>  | <p><b>BASIC STUDIES</b><br/> reservoirs</p>   |
| S-49 | <p>Symons, J M Carswell, J K Robeck, G G<br/> <b>MIXING OF WATER SUPPLY RESERVOIRS FOR QUALITY<br/> CONTROL</b><br/> J American Water Works Assoc v 62 n 5 May 1970 p 322-334</p> <p>Describes test destratification of relatively small reservoirs (up to 2,900 acre-ft) using either mechanical or diffused air pumping. Dissolved oxygen in</p>   | <p><b>EQUIPMENT</b><br/> reservoirs<br/> diffusers</p>  |

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the hypolimnion was increased and associated water quality problems were alleviated. Results from one of the test lakes showed reoxygenation efficiencies of 0.7 lb/kwhr for mechanical pumping and 1.7 lb/kwhr for diffused air pumping. Guidelines are given for design and equipment performance evaluation. Includes a summary of water purveyor experience in destratification at 17 reservoirs.

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| T-1 | <p>Takahashi, T Fan, L T<br/> <b>SEVERAL DIFFERENT GAS-LIQUID CONTACTORS<br/>         UTILIZING CENTRIFUGAL FORCE</b><br/>         Kans State U Inst for Systems Design and Optimization Report No. 10<br/>         Dec 19 1968 Manhattan Kans</p> <p>Describes the features of several centrifugal contactors; these contactors are coming into use but as yet there is no literature on design features and fundamental studies. Centrifugal contactors are expected to be widely used because of favorable mass-transfer characteristics</p>  | EQUIPMENT<br>misc equipment                           |
| T-2 | <p>Tarassov, Victor J Perlis, Harlan J Davidson, Burton<br/> <b>OPTIMIZATION OF A CLASS OF RIVER AERATION<br/>         PROBLEMS BY THE USE OF MULTIVARIABLE<br/>         DISTRIBUTED PARAMETER CONTROL THEORY</b><br/>         Water Resources Res v 5 n 3 Jun 1969 p 563-573</p> <p>Mathematical programming methods applied to water pollution problems have been highly successful, especially in cases where hypothetical models were used. In many applications, linear programming, dynamic programming, or Pontryagin's Maximum Principle methods have been demonstrated, using steady-state Streeter-Phelps system equations at some stage in the optimization study. The application of the Sirazetdinov-Tarassov-Perlis theory of optimal control to the artificial instream aeration problem in polluted rivers is examined. The main concern of the study is to show how artificial instream aeration can be controlled, minimizing the relative cost of operation for several competing design criteria. The economic aspects of cost minimization of this process have important theoretical implications and potential applications to specific water pollution problems. 19 refs</p> | BASIC STUDIES<br>streams<br>theoretical<br>reaeration |
| T-3 | <p>Technical Practice Committee Subcommittee on Aeration in Wastewater Treatment<br/> <b>AERATION IN WASTEWATER TREATMENT—MOP 5</b><br/>         J Water Pollution Control Federation v 41 n 11 Nov 1969 p 1863 v 41 n 12 Dec 1969 p 2026</p> <p>"Aeration in Wastewater Treatment" is the revised edition of the original Manual of Practice No. 5, "Air Diffusion in Sewage Works," published in 1952. The manual is intended to provide designers, operators, and maintenance personnel of wastewater treatment facilities with the fundamental theory and operational aspects of aeration. First and second installments</p>   | EQUIPMENT<br>waste treatment                          |
| T-4 | <p>Technical Practice Committee Subcommittee on Aeration in Wastewater Treatment<br/> <b>AERATION IN WASTEWATER TREATMENT—MOP 5</b><br/>         J Water Pollution Control Federation v 42 n 1 Jan 1970 p 51</p> <p>Third of three installments. Discussion of operation and maintenance of aeration systems, with emphasis on diffusers. Includes short discussion of air blowers</p>   | EQUIPMENT<br>waste treatment                          |
| T-5 | <p>Teerink, John R Martin, Cecil V<br/> <b>ARTIFICIAL DESTRATIFICATION IN RESERVOIRS OF THE<br/>         CALIFORNIA STATE WATER PROJECT</b><br/>         J American Water Works Assoc v 61 n 9 Sep 1969 p 436-440</p> <p>Destratification and aeration in Calif. reservoirs are accomplished by air injection and multiple-level outlet structures. Mixing returns nutrients to the</p>  | EQUIPMENT<br>reservoirs<br>diffusers<br>economics     |

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photosynthetic zone for use by organisms, and oxidizes iron and manganese. The effects may be beneficial or detrimental to intended water uses. Evaporation is usually reduced because surface water temperatures are lowered. Dissolved oxygen is increased. Because artificial destratification can produce both benefits and detriments, a study should be made of priority of uses and the effects of mixing, and cost-benefit analyses should be made, placing a value on the various quality changes related to mixing. 16 refs (Knapp-USGS) W69-09883

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| T-6  | <p>Thackston, E L<br/> <b>APPLICATIONS OF ANALOG COMPUTERS IN SANITARY ENGINEERING</b><br/> Proc of the 3rd Annual Workshop American Assoc of Professors in Sanitary Eng<br/> Jun 1968 (Editor)</p>   | GENERAL                                |
| T-7  | <p>Thackston, E L<br/> discussion of <b>CONTROL OF IMPOUNDMENT WATER QUALITY BY ENGINEERING METHODS</b> by J. M. Symons, W. H. Irwin, G. G. Robeck<br/> ASCE Specialty Conf on Current Res into the Effects of Reservoirs on Water Quality Portland Jan 22-24 1968</p>  | BASIC STUDIES<br>reservoirs            |
| T-8  | <p>Thackston, E L<br/> discussion of <b>MANAGEMENT AND MEASUREMENT OF D.O. IN IMPOUNDMENTS</b> by J. M. Symons, W. H. Irwin, R. M. Clark and G. G. Robeck<br/> Proc ASCE v 94 n SA 4 Aug 1968 p 748-752</p>   | BASIC STUDIES<br>reservoirs            |
| T-9  | <p>Thackston, Edward L Hays, James R Krenkel, Peter A<br/> <b>LEAST SQUARES ESTIMATION OF MIXING COEFFICIENTS</b><br/> Proc ASCE v 93 n SA 3 Jun 1967 proc paper 5288 p 47-58<br/> The principle of least squares estimation of nonlinear parameters as a general tool in mathematical modeling can be shown to be applicable to many common problems in sanitary engineering. A digital computer program for accomplishing this procedure is explained, and the results are illustrated for the example of estimating mixing coefficients and mean travel times for measured time-concentration curves. A critical examination of existing estimation procedures shows them to be inaccurate and unreliable. The results of comparative fit of several methods to several hundred curves are presented. If a digital computer is not available, a simple, quick, trial-and-error procedure—outlined in the paper—can be used to produce results more reliable than those given by presently used methods</p> | BASIC STUDIES<br>streams               |
| T-10 | <p>Thackston, E L Krenkel, P A<br/> discussion of <b>BOD AND OXYGEN RELATIONSHIPS IN STREAMS</b> by William E. Dobbins<br/> Proc ASCE v 91 n SA 1 Feb 1965 proc paper 3949 p 84-88</p>  | BASIC STUDIES<br>streams<br>reaeration |
| T-11 | <p>Thackston, E L Krenkel, P A<br/> <b>LONGITUDINAL MIXING AND REAERATION IN NATURAL STREAMS</b><br/> Tech Report No. 7 in Sanitary and Water Resources Eng Vanderbilt U<br/> Nashville Tenn 1966</p>   | BASIC STUDIES<br>streams<br>reaeration |

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| T-12 | <p>Thackston, E L Krenkel, P A<br/> <b>LONGITUDINAL MIXING IN NATURAL STREAMS</b><br/> Proc ASCE v 93 n SA 5 Oct 1967 p 67-90</p> <p>Various models used to describe or predict longitudinal mixing coefficients are examined and the conditions under which they are expected to apply are elucidated. Several hundred coefficients, both in laboratory flumes and natural streams, were measured under two-dimensional, uniform-flow conditions. The coefficients measured in natural streams are shown to follow equations derived from flume data. The influence of dead zones in the stream on mixing is examined, and it is shown that measured coefficients are much closer to predicted values when the influence of mixing due to the dead zones is separated by the use of a new mixing model</p>   | <p><b>BASIC STUDIES</b><br/> streams</p>   |
| T-13 | <p>Thackston, Edward L Krenkel, Peter A<br/> <b>REAERATION PREDICTION IN NATURAL STREAMS</b><br/> Proc ASCE v 95 n SA 1 Feb 1969 p 65-94</p> <p>Reviews the predictive equations of O'Connor-Dobbins, Krenkel, Dobbins, Kalinske, and Churchill; proposes a new formula and gives field data for correlation</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> reaeration</p>   |
| T-14 | <p>Thackston, Edward L Krenkel, Peter A<br/> <b>TURBULENT DIFFUSION AND REAERATION</b><br/> Proc 14th So. Water Resources and Pollution Control Conf held at U of N C Chapel Hill N C Apr 1965 p 197-206</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> reaeration</p>   |
| T-15 | <p>Thackston, Edward L Speece, R E<br/> <b>REVIEW OF SUPPLEMENTAL REAERATION OF FLOWING STREAMS</b><br/> J Water Pollution Control Federation v 38 n 10 Oct 1966 p 1614-1622</p> <p>Diffused air, turbine aeration, weirs, surface aeration, pressure injection, and U-tubes are among methods of providing supplemental aeration in flowing streams; weirs are quite efficient and inexpensive; turbine aeration also appears to be inexpensive, whereas diffused-air and surface aeration are far more costly for same amount of oxygen transfer; pressure injection seems, from its limited use thus far, to be efficient; very effective U-tube process may be applicable to small streams. 20 refs</p>   | <p><b>GENERAL</b><br/> reviews<br/> <b>EQUIPMENT</b><br/> streams<br/> diffusers<br/> turbine injection<br/> cascades<br/> mechanical<br/> aerators<br/> pressure injection<br/> U-tubes</p> |
| T-16 | <p>Thackston, Edward L Speece, R E<br/> <b>SUPPLEMENTAL REAERATION OF LAKES AND RESERVOIRS</b><br/> J American Water Works Assoc v 58 n 10 Oct 1966 p 1317-1324</p> <p>Supplemental aeration and mixing of water in lakes and reservoirs is complicated by stratification and the tremendous volume of water to be moved. A method of oxygenation must provide for distributing oxygen throughout the impounded water, or the water must be mixed to bring it into contact with oxygen at the surface. Most methods of supplemental aeration of impounded waters rely on mixing alone and do not attempt to add oxygen directly. Mixing brings the oxygen-deficient hypolimnion into contact with the atmosphere where it absorbs oxygen and also breaks up the temperature stratification, enabling natural wind forces to cause further mixing action with resulting distribution of oxygen throughout the entire depth of water. Once stratification is broken, continuous pumping is unnecessary; usually intermittent operation will cause complete mixing throughout the season. The most successful attempts to destroy stratification have used compressed air. One of the more promising recent developments is the aerohydraulic gun,</p> | <p><b>GENERAL</b><br/> reviews<br/> <b>EQUIPMENT</b><br/> reservoirs<br/> diffusers<br/> hydraulic guns</p>  |

## T—Continued

or bubble gun, which shoots air bubbles to the surface from underwater tubes. Rising bubbles shatter as they leave the tube mouth and entrain considerably more water than actually flows through the tube. Other techniques for reaerating impounded water are discussed

- T-17 Thayer, Richard P Krutchkoff, Richard G  
**STOCHASTIC MODEL FOR BOD AND DO IN STREAMS**  
Proc ASCE v 93 n SA 3 Jun 1967 p 59-72  
A stochastic model for pollution and dissolved oxygen in streams is obtained. Given the stream parameters and the initial conditions, the model predicts not only the mean amounts of pollution and dissolved oxygen at any point downstream, but also their variability in time. One can determine the proportion of the time that pollution is above any given concentration or that dissolved oxygen is below any given concentration. The theoretical results are tested by comparing them with controlled laboratory experiments and with data from the Sacramento River. It is observed that the means of both pollution and dissolved oxygen follow the equations already obtained by Dobbins ("BOD and Oxygen Relationships in Streams," J of the Sanitary Eng Div, ASCE v 90 n SA 3 Jun 1964 proc paper 3949 p 53). A new and unexpected observation is that the greatest variability in dissolved oxygen occurs at the sag, where it is most critical
- T-18 Thomman, Robert V  
**MATHEMATICAL MODEL FOR DISSOLVED OXYGEN**  
Proc ASCE v 89 n SA 5 Oct 1963 p 1-30  
Discussion: Alex N Diachishin SA 3:Jun 64:137:3935; Donald J O'Connor and Dominic Di Toro SA 6:Dec 64:117:4171  
Closure: SA 6:Dec 64:122:4171  
The basic concepts of systems analysis and its application to DO are presented. The mathematical model is developed by viewing a particular body of water such as an estuary as composed of a number of finite segments each comprising a "system" in the classical mathematical sense. A dissolved oxygen balance equation can then be written for each system. A linear systems analysis technique is then used and the DO response resulting from the input forcing functions are derived
- T-19 Thomann, R V  
**RECENT RESULTS FROM MATHEMATICAL MODEL OF WATER POLLUTION CONTROL IN DELAWARE ESTUARY**  
Water Resources Res v 1 n 3 Third Quarter 1966 p 349-359  
Basic concepts of systems analysis and optimum (least-cost) water pollution control are presented; equations utilized to describe time and space variability of dissolved oxygen are presented in systems analysis context, and their usefulness in this form is discussed; application of mathematical model to control of dissolved oxygen in Delaware Estuary is given; recent computer solutions are illustrated, and sensitivity of least-cost dissolved oxygen improvement solutions to rate of atmospheric reaeration is presented (EI 1966)
- T-20 Thomann, R V  
**TIME-SERIES ANALYSIS OF WATER-QUALITY DATA**  
Proc ASCE v 93 n SA 1 Feb 1967 p 1-23  
The basic concepts of Fourier and power spectrum analyses are presented in terms of their application to dissolved oxygen and temperature data of the
- BASIC STUDIES**  
streams  
theoretical  
reaeration  
oxidation
- BASIC STUDIES**  
theoretical
- BASIC STUDIES**  
estuaries  
theoretical
- BASIC STUDIES**  
estuaries  
experimental

## T—Continued

Delaware Estuary. The results of Fourier analyses computations performed on hourly data from water-quality monitoring stations are presented. For temperature, more than 92 percent of the total variance is accounted for by the 365-day periodicity. For dissolved oxygen, more than 90 percent of the total variance is accounted for by the annual periodicity and the next four higher harmonics (semi-annual; tri-annual, etc.). The dissolved oxygen variability remaining after removal of the principal Fourier components was found to be approximately normally distributed with an average standard deviation of 0.85 mg per l. Power spectrum analyses of the 24-hr averaged DO residual seconds indicated a peak in the region of 30 to 60 days and for temperature a peak is dominant at 30 days. The analyses all indicate a predominance of low frequency (periods of from 7 days to 1 year and longer) types of phenomena. The implications of the results from a sampling and control point of view are evaluated

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| T-21 | Thomas, H A Jr<br>THE "SLOPE" METHOD OF EVALUATING THE CONSTANTS<br>OF THE FIRST-STAGE BIOCHEMICAL OXYGEN DEMAND<br>CURVE<br>Sewage Works J v 9 n 3 May 1937 p 425  | BASIC STUDIES<br>experimental<br>oxidation             |
| T-22 | Thomas, Ivor E<br>DISPERSION IN OPEN CHANNEL FLOW<br>PhD Thesis Northwestern U Evanston Ill 1958  | BASIC STUDIES<br>streams                               |
| T-23 | Toei, Ryoza Matsuno, Ryuichi Nishitani, Keiichi Hayashi, Hideo<br>Imamoto, Tsunehiko<br>GAS INTERCHANGE BETWEEN BUBBLE PHASE AND<br>CONTINUOUS PHASE IN GAS-SOLID FLUIDIZED BED<br>AT COALESCENCE<br>Chem Abstracts v 71 1969 p 134<br>The process of coalescence of bubbles was investigated from the viewpoint of<br>gas interchange (mass transfer) between the bubble phase and the continuous<br>phase. A two-dimensional fluidized bed was used to determine the gas<br>mass-transfer coefficient   | BASIC STUDIES<br>bubbles<br>experimental               |
| T-24 | Truesdale, G A<br>NEW SOLUBILITY DATA FOR OXYGEN<br>J of Applied Chem v 5 1955  | BASIC STUDIES<br>experimental<br>reaeration            |
| T-25 | Truesdale, G A Vandyke, K G<br>THE EFFECT OF TEMPERATURE ON THE AERATION<br>OF FLOWING WATER<br>Water and Waste Treatment J v 7 n 9 May-Jun 1958  | BASIC STUDIES<br>streams<br>experimental<br>reaeration |
| T-26 | Tsivoglou, E C<br>MODERN CONCEPTS OF BOD-DO RELATIONSHIPS<br>Ontario Ind Waste Conf 12th—Proc Jun 1965 p 147-157<br>Summary of more recent work at Robert A. Taft Sanitary Engineering Center<br>on factors involved in stream self-purification, with particular emphasis on<br>relationship of this work to disposal of industrial effluents; analysis of BOD<br>reaction kinetics, as determined on basis of observed BOD rate curves; it is<br>shown that waste treatment plants designed only on basis of 5-day BOD<br>determination will prove inadequate to meet desired DO objectives in<br>receiving streams (EI 1966) | BASIC STUDIES<br>streams<br>experimental<br>oxidation  |



## T—Continued

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| T-27 | <p>Tsivoglou, E C O'Connell, R L Walter, C M Godsil, P J Logsdon, G S<br/> <b>TRACER MEASUREMENTS OF ATMOSPHERIC REAERATION—I</b><br/> <b>LABORATORY STUDIES</b><br/>         J Water Pollution Control Federation v 37 n 10 Oct 1965 p 1343-1362<br/>         Evaluates atmospheric reaeration rates in turbulent systems by laboratory experiments using chemically inert radioactive tracer gases; results show Kr 85 and Rn 222 are suitable tracers for oxygen gas. Tests indicate reaeration in turbulent systems takes place in two separate consecutive steps—diffusion of gas across the liquid-air interface, and subsequent mixing and dispersion of the dissolved gas throughout the main body of water</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p> |
| T-28 | <p>Tisvoglou, E C<br/> <b>TRACER MEASUREMENT OF STREAM REAERATION</b><br/>         Federal Water Pollution Control Admin Div of Tech Services U S Dept Interior Washington D C 1967<br/>         Reports laboratory and field trials on tracer measurement of stream reaeration</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p> |
| T-29 | <p>Tsivoglou, E C Cohen, J B Shearer, S D Godsil, P J<br/> <b>TRACER MEASUREMENT OF STREAM REAERATION—II</b><br/> <b>FIELD STUDIES</b><br/>         J Water Pollution Control Federation Washington D C 20016 v 40 n 2 pt 1 Feb 1968 p 285-305<br/>         New method for accurate and independent direct measurement of gas transfer and reaeration capacity of natural streams is presented; fluorescent dye, dispersion indicator (tritium), and gaseous tracer (krypton-85) were released in main flow of Jackson River from Covington to Clifton Forge, Va.; results show that tracer method may be used in polluted or unpolluted rivers, regardless of sludge deposits, algae, and dissolved oxygen levels; method provides predictions in general range of values predicted by previous investigators. 10 refs</p> | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p> |
| T-30 | <p>Tsivoglou, E C Wallace, J R<br/> <b>HYDRAULIC PROPERTIES RELATED TO STREAM REAERATION</b><br/>         Georgia Inst of Tech Unnumbered Undated</p>   | <p><b>BASIC STUDIES</b><br/>         streams<br/>         experimental<br/>         reaeration</p> |
| T-31 | <p>Tullis, J P Skinner, M M<br/> <b>REDUCING CAVITATION IN VALVES</b><br/>         Proc ASCE v 94 n HY 6 Nov 1968 p 1475-1488<br/>         The variation of cavitation inception, with and without air injection and as a function of valve opening, are reported for a 12-in. ball valve in a 12-in. butterfly valve with water as the test fluid. Air is injected through the valve stem and side ports of the butterfly valve and through side ports in the ball valve. The water supply is approximately 38° F with an air content of about 70 percent of saturation. Air injection into the separation zone below the valves is shown to effectively eliminate or significantly reduce cavitation. (J. F. Lafferty Applied Mechanics Rev v 22 n 11 Nov 1969 rev 8870.)</p>   | <p><b>CAVITATION</b></p>   |
| T-32 | <p>Tullis, J P Marschner, B W<br/> <b>REVIEW OF CAVITATION RESEARCH ON VALVES</b><br/>         Proc ASCE v 94 n HY 1 Jan 1968 p 1-16<br/>         Critical cavitation indices are presented for 12-in. ball and 12-in. butterfly valve installed in closed conduit system with sudden expansion downstream</p>  | <p><b>CAVITATION</b></p>   |

## T—Continued

of valves; tests were conducted under normal operating conditions to find effect of injecting air and water at various locations on critical cavitation index; it was found that injecting water into sudden expansion below valves does not affect cavitation; injecting small quantities of air into separation zones below valves materially reduces cavitation intensity and critical cavitation index. 12 refs (EI 1968)

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| T-33 | Tyler, R<br>POLLUTED STREAMS CLEARED UP BY AERATION<br>Civil Eng v 16 1946 p 348-349   | EQUIPMENT<br>streams<br>diffusers |
| T-34 | Tyler, Richard G<br>ACCELERATED REAERATION<br>Sewage Works J v 14 n 4 Jul 1942 p 834-838<br>This paper contains one of the early proposals for the use of diffusers for supplemental reaeration of streams | EQUIPMENT<br>streams<br>diffusers |
| T-35 | Tyler, Richard G<br>STREAM POLLUTION, ACCELERATED REAERATION<br>Civil Eng (London) v 38 Jan 1943 p 7-9   | EQUIPMENT<br>streams              |

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No references

## V

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| V-1 | <p>Vanderhoof, R A</p> <p>CHANGES IN WASTE ASSIMILATION CAPACITY RESULTING FROM STREAMFLOW REGULATION</p> <p>US Dept Health Education Welfare Symposium on Streamflow Regulation for Quality Control Public Health Service Pub No 999-WP-30 Jun 1965</p> <p>Discusses dissolved oxygen changes in a reservoir and the control of waste assimilative capacity downstream by flow augmentation and peaking power discharges</p>   | <p>BASIC STUDIES</p> <p>streams</p> <p>reservoirs</p>                  |
| V-2 | <p>Van der Kroon, G T M</p> <p>EFFECT OF SUSPENDED COMPOUNDS ON THE RATE OF OXYGEN TRANSFER INTO WATER SOLUTIONS</p> <p>Vodni Hospodarstvi (Czech) v 6 1968 p 255</p> <p>THE INFLUENCE OF SUSPENDED SOLIDS ON THE RATE OF OXYGEN TRANSFER INTO AQUEOUS SOLUTIONS</p> <p>Water Res v 2 1968 p 26</p>   | <p>BASIC STUDIES</p> <p>experimental</p> <p>reaeration</p>             |
| V-3 | <p>Van Wijngaarden, L</p> <p>ON GROWTH OF SMALL CAVITATION BUBBLES BY CONVECTIVE DIFFUSION</p> <p>Int J Heat and Mass Transfer v 10 n 2 Feb 1967 p 127-134</p> <p>In calculation of bubble growth due to convective diffusion of gas (mainly air) by B. R. Parkin and R. W. Kermeen, vapor content of bubbles and surface tension were not taken into account; allowance is made for these effects; V. G. Levich's model is advanced for determination of mass flux in bubbles; growth results are compared with Parkin and Kermeen experimental data. 9 refs (EI 1967)</p> | <p>CAVITATION</p>  |
| V-4 | <p>Varma, M M DiGiano, F</p> <p>KINETICS OF OXYGEN UPTAKE BY DEAD ALGAE</p> <p>J Water Pollution Control Federation v 40 n 4 Apr 1968 p 613</p>   | <p>BASIC STUDIES</p> <p>experimental</p> <p>oxidation</p>              |
| V-5 | <p>Velz, C J</p> <p>DEOXYGENATION AND REOXYGENATION</p> <p>Trans ASCE v 104 1939 p 560</p> <p>Presents a nomograph for calculating atmospheric reaeration in turbulent systems</p>  | <p>BASIC STUDIES</p> <p>streams</p> <p>reaeration</p> <p>oxidation</p> |
| V-6 | <p>Velz, C J</p> <p>FACTORS INFLUENCING SELF-PURIFICATION AND THEIR RELATION TO POLLUTION ABATEMENT</p> <p>Sewage Works Journal v 19 n 4 1947</p>   | <p>BASIC STUDIES</p> <p>streams</p> <p>reaeration</p>                  |
| V-7 | <p>Velz, C J</p> <p>SIGNIFICANCE OF ORGANIC SLUDGE DEPOSITS</p> <p>Oxygen Relationships in Streams Tech Report W58-2 Robert A. Taft Sanitary Eng Center U S Public Health Service 1958</p>  | <p>BASIC STUDIES</p> <p>streams</p> <p>oxidation</p>                   |
| V-8 | <p>Verduin, Jacob</p> <p>discussion of PHOTOSYNTHESIS AS A FACTOR IN THE OXYGEN BALANCE OF RESERVOIRS by C.H.J. Hull</p> <p>US Dept Health Education Welfare Symposium on Streamflow Regulation for Quality Control Public Health Service Pub No. 999-WP-30 Jun 1965 p 91-94</p>  | <p>BASIC STUDIES</p> <p>reservoirs</p> <p>photosynthesis</p>           |

## V—Continued

Discusses establishing the ecological relationships in photosynthetic oxygenation rather than applications to sanitary engineering; gives a table showing amount of oxygen derived from natural phytoplankton communities

- V-9 Vinberg, G G  
ZHACHENIE FOTOSINTEZA JLYA OBOGASHCHENIYA VODY  
KISLORODOM PRI SAMOOCHISHCHENII ZAGRYAZNENNYKH VOD  
(Significance of Photosynthesis for Oxygen Enrichment of Water During  
Self-purification of Polluted Waters)  
Trudy Vsesoyuz Hidrobiol Obschestva v 6 1955 p 46-69 In Russian

BASIC STUDIES  
photosynthesis

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| W-1 | <p>Wagner, H<br/>         VOITH-FORSCHUNG UND KONSTRUKTION (Voith—Research<br/>         and Construction)<br/>         v 1 1955 p 1311 In German</p>   | EQUIPMENT<br>streams                                   |
| W-2 | <p>Wagner, H<br/>         THE ARTIFICIAL AERATION OF HARNESSSED STREAMS<br/>         Special Communications to the German Hydrological Year Book No. 15<br/>         Published by the Federal Office for Hydrology Coblenz (1956) In German</p>  | EQUIPMENT<br>streams<br>turbine injection              |
| W-3 | <p>Wagner, H<br/>         THE ARTIFICIAL AERATION OF CANALIZED RIVERS<br/>         Bes Mitt Dtsch Gewasserkundlichen J No. 15 1956<br/>         Water Pollution Abstracts (Brit) v 30 1957 p 2222 In German</p>  | EQUIPMENT<br>streams                                   |
| W-4 | <p>Wagner, H<br/>         EXPERIMENTS WITH ARTIFICIAL AERATION OF RIVER<br/>         WATER<br/>         Deutsche Gewasserkundliche Mitteilungen v 2 n 4 1958 p 73-79<br/>         Results of aeration experiments at the Poppenweiler Powerplant on the<br/>         Neckar, 1957 In German</p>  | EQUIPMENT<br>streams<br>turbine injection              |
| W-5 | <p>Walker, J D<br/>         CROSS-ROLL AERATION ELIMINATES SHORT CIRCUITING<br/>         Water and Wastes Eng (formerly Water Works and Wastes Eng) v 3 n 1 Jan 1966<br/>         p 57-59<br/>         Effects of cross-roll aeration method in long-period reaeration processes to<br/>         eliminate short circuiting so that progressive synthesis will take place and<br/>         finished sludge will be endogenous before reentry into contact are outlined;<br/>         how diffusers and air headers are arranged for cross-roll aeration; tests in<br/>         parallel tanks (EI 1966)</p>              | EQUIPMENT<br>waste treatment<br>diffusers              |
| W-6 | <p>Wallace, J R Reheis, H F<br/>         HYDRAULIC PROPERTIES OF THE SOUTH AND FLINT<br/>         RIVERS IN THE VICINITY OF ATLANTA, GEORGIA<br/>         Georgia Inst Technol Atlanta prepared for the FWPCA Washington D C<br/>         Feb 1969<br/>         Provides physical data for an investigation on stream reaeration capacity.<br/>         Physical characteristics of the streams are discharge, flow depth, stream<br/>         width, flow velocity, hydraulic radius, wetted perimeter, and stream slope.<br/>         Predictions of reaeration capacity are made from available predictive models</p> | BASIC STUDIES<br>streams<br>experimental<br>reaeration |
| W-7 | <p>Welch, P S<br/>         LIMNOLOGY, 2D ED<br/>         McGraw-Hill New York N Y 1952 528 p</p>   | GENERAL  |
| W-8 | <p>Weston, R F<br/>         STUDIES IN ENTRAINMENT AERATION<br/>         J Water Pollution Control Federation v 34 n 4 Apr 1962 p 342-353<br/>         Report of work undertaken to better define fundamentals of operation and<br/>         to determine effects of diameter, blade sizes, number of blades, speed of<br/>         rotation, submergence, and other variables on horsepower requirements and<br/>         oxygen transfer (EI 1962)</p>   | EQUIPMENT<br>mechanical<br>aerators                    |

## W—Continued

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| W-9  | <p>Wezenak, Chester T Gannon, John J<br/> <b>EVALUATION OF NITRIFICATION IN STREAMS</b><br/> Proc ASCE v 94 n SA 5 Oct 1968 p 883-895<br/> A simplified procedure for evaluating nitrification progression in a stream is given. Data are presented for the Clinton River between Pontiac and Rochester, Mich. which show rapid inorganic nitrogen oxidation in this section of the river. Graphical and analytical techniques for evaluating nitrification parameters and progression are described</p>   | <p><b>BASIC STUDIES</b><br/> streams<br/> experimental<br/> oxidation</p>                        |
| W-10 | <p>Whipple, W<br/> <b>ECONOMICS OF INDUCED RIVER AERATION</b><br/> Chemical Engineering Progress v 65 n 97 1969 (book review)</p>  | <p><b>EQUIPMENT</b><br/> streams<br/> economics</p>  |
| W-11 | <p>Whipple, W Jr Coughlan, F P Jr<br/> <b>INSTREAM AERATORS FOR POLLUTED RIVERS</b><br/> Reprint 1086 ASCE National Water Resources Meeting Memphis Tenn<br/> Jan 26-30 1970<br/> Describes field tests of instream use of mechanical aerator and diffuser. Comparison on basis of transfer efficiency and cost shows mechanical aerator to be superior. Efficiency of mechanical aerator was about 2 to 3 lbs oxygen/hp-hr; diffuser had efficiency about two-thirds that amount. Gives good example of cost analysis</p>   | <p><b>EQUIPMENT</b><br/> streams<br/> mechanical<br/> aerators<br/> diffusers<br/> economics</p> |
| W-12 | <p>Whipple, W Jr Hunter, J V Davison, B Dittman, F W Yu, Shaw L<br/> <b>IN-STREAM AERATION OF POLLUTED RIVERS</b><br/> Rutgers—The State U New Brunswick N J Water Resources Res Inst<br/> Mechanical and diffuser instream aerators were tested on the Upper Passaic River and proved a practical and economical method of adding dissolved oxygen to polluted streams. The tests were conducted in conjunction with research into photosynthesis, benthal oxygen demand, and mass balance of BOD in that river system. Systems of aerators were designed to provide for meeting water quality objectives of dissolved oxygen and cost estimates made. Alternative costs of meeting the same objectives by means of advanced effluent treatment alone appear to be several times as great. It is concluded that instream aeration may provide a feasible alternative to advanced waste treatment for polluted rivers, as a supplement to secondary waste treatment<br/> W69-09555</p> | <p><b>EQUIPMENT</b><br/> streams<br/> mechanical<br/> aerators<br/> diffusers</p>                |
| W-13 | <p>White, M T<br/> <b>SURFACE AERATION AS SECONDARY TREATMENT SYSTEM</b><br/> Tappi v 48 n 10 Oct 1965 p 128A-132A<br/> Fourteen 60-hp surface aerators were installed as secondary treatment system in one basin of existing two-basin retention lagoon; BOD is reduced by about 36 percent in passing through first basin; overall reduction for summer averaged 88 percent; oxygen transfer efficiency was 3.1 lb/hp-hr at design load range; installation and operating costs (EI 1966)</p>  | <p><b>EQUIPMENT</b><br/> waste treatment<br/> mechanical<br/> aerators</p>                       |
| W-14 | <p>Whitman, W G<br/> <b>TWO-FILM THEORY OF GAS ABSORPTION</b><br/> Chemical and Metallurgical Engineering v 29 1923 p 146</p>  | <p><b>BASIC STUDIES</b><br/> theoretical<br/> reaeration</p>                                     |

## W—Continued

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| W-15 | <p>Wiebe, A H<br/> THE EFFECT OF DENSITY CURRENTS UPON THE<br/> VERTICAL DISTRIBUTION OF TEMPERATURE AND<br/> DISSOLVED OXYGEN IN NORRIS RESERVOIR<br/> J Tenn Academy Sci v 15 1940 p 301-308</p>  | <p><b>BASIC STUDIES</b><br/> reservoirs</p>                 |
| W-16 | <p>Wiley, A J Lueck, B F Scott, R H Wisniewski, T F<br/> COOPERATIVE STATE-INDUSTRY STREAM STUDIES—LOWER<br/> FOX RIVER, WISCONSIN<br/> Sewage and Ind Wastes v 29 Jan 1957 p 76</p>  | <p><b>EQUIPMENT</b><br/> streams<br/> turbine injection</p> |
| W-17 | <p>Wiley, A J Lueck, B F Scott, R H Wisniewski, T F<br/> COMMERCIAL-SCALE OPERATION OF TURBINE AERATION<br/> ON WISCONSIN RIVERS<br/> Sewage and Ind Wastes v 32 n 2 Feb 1960 p 186</p>   | <p><b>EQUIPMENT</b><br/> streams<br/> turbine injection</p> |
| W-18 | <p>Wiley, A J Lueck, B F<br/> TURBINE AERATION AND OTHER METHODS OF<br/> REAERATING STREAMS<br/> Tappi v 43 1960 p 241</p>  | <p><b>EQUIPMENT</b><br/> streams<br/> turbine injection</p> |
| W-19 | <p>Wiley, A J Lueck, B F Scott, R H Wisniewski, T F<br/> COMMERCIAL-SCALE STREAM REAERATION<br/> J Water Pollution Control Federation v 34 n 4 Apr 1962 p 401<br/> Review of present status of commercial-scale stream aeration as means for<br/> accelerating recovery of oxygen-depleted waters and of increasing working<br/> capacity of rivers subjected to heavy loadings of biochemical and chemical<br/> oxygen demand</p>  | <p><b>EQUIPMENT</b><br/> streams<br/> turbine injection</p> |
| W-20 | <p>Wiley, A J Parkinson, L Gehm, H W Wisniewski, T F Bartsch, H F<br/> RIVER REAERATION<br/> Paper Trade J v 124 Mar 20 1947 p 123<br/> A method suggested by Professor Tyler of the University of Wash. consisting<br/> of diffusing compressed air beneath the surface of a river which has been<br/> polluted for the purpose of maintaining minimum levels of dissolved oxygen,<br/> has been tried in full scale on a Wis. river. The experimental setup consisted<br/> of an aerating station located at a power dam downstream from a sulphite<br/> mill at a point where a serious sag in dissolved oxygen occurred in the stream<br/> during low summer flows. Employing carborundum diffusers with a total area<br/> of 319 sq ft set at a depth of about 10 ft and fed by a compressor capable of<br/> supplying 1,550 cu ft of air per minute at 5 psi it was possible to add to the<br/> stream an average of close to 1.5 tons of oxygen per day at a flow of 800 cfs.<br/> This together with the immediate satisfaction of a portion of the BOD of the<br/> stream water, attributable to aeration, caused a marked movement upstream<br/> of the zone of recovery. Hence the process appears to be a useful tool in<br/> accelerating the recovery of a polluted stream shortening to a considerable<br/> degree the distance of passage required for oxidation of the waste and serves<br/> to prevent anerobic conditions and attending nuisance.</p> <p>Extensive test data collected during operation of the unit are summarized in<br/> this paper including biological observations with respect to stream flora and<br/> fauna. Recommendations with respect to application, requirements, design,<br/> and efficiency are included</p> | <p><b>EQUIPMENT</b><br/> streams<br/> diffusers</p>         |



## W—Continued

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| W-21 | <p>Winberg, G G Sivko, T N<br/> <b>SIGNIFICANCE OF PHOTOSYNTHETIC AERATION IN<br/> OXYGEN BALANCE OF POLLUTED WATERS</b><br/> Int J Air and Water Pollution v 6 May-Aug 1962 p 267-275<br/> Method of calculation of elements of oxygen balance; example calculations of<br/> atmospheric aeration oxygen consumption of riverbed and sessile vegetation<br/> and photosynthetic reaeration by fixed vegetation (EI 1962)</p>  | <p><b>BASIC STUDIES</b><br/> streams<br/> photosynthesis<br/> oxidation<br/> reaeration</p>   |
| W-22 | <p>Wirts, J J<br/> <b>CLEANING AIR DIFFUSION MEDIA</b><br/> Water and Sewage Works v 94 1947</p>   | <p><b>EQUIPMENT</b><br/> diffusers</p>  |
| W-23 | <p>Wisniewski, T F<br/> <b>IMPROVEMENT OF THE QUALITY OF RESERVOIR DISCHARGES<br/> THROUGH TURBINE OR TAILRACE AERATION</b><br/> U S Dept Health Education Welfare Symposium on Streamflow Regulation for<br/> Quality Control Public Health Service Pub No 999-WP-30 Jun 1965<br/> p 299-316<br/> Review the status of commercial-scale stream aeration on the Flambeau<br/> River, Fox River, and Wisconsin River; an evaluation of capital and operating<br/> costs is given for hydroturbine aeration</p>  | <p><b>EQUIPMENT</b><br/> streams<br/> turbine injection<br/> diffusers</p>  |
| W-24 | <p>Wolf, P<br/> <b>KORREFERAT ZU: IMHOFF, KUNSTLICHE BELUFTUNG<br/> FUR DEN BALDENEYSEE UND DIE UNTERE RUHR</b><br/> (Coreview of: Imhoff, Artificial Aeration for the Baldeney Lake and<br/> the Lower Ruhr)<br/> Gewasserschutz—Wasser—Abwasser Band 1 Aachen 1968</p>   | <p><b>EQUIPMENT</b><br/> streams<br/> reservoirs<br/> diffusers<br/> turbine injection<br/> mechanical<br/> aerators<br/> economics</p> |
| W-25 | <p>Wood, R<br/> <b>COMPARISON STUDIES OF WINKLER VS OXYGEN SENSOR</b><br/> J Water Pollution Control Federation v 41 n 12 Dec 1969 p 2002<br/> Determination of dissolved oxygen levels in waste water treatment and<br/> effluent disposal are of great use in a number of ways. In-plant laboratory<br/> studies of using a polarographic oxygen sensor in comparison with the more<br/> common Winkler method were conducted. Advantages found were: (a) the<br/> preparation and standardization of reagent solution are eliminated; (b) time<br/> spent in analysis is reduced; (c) the method is less tedious; and (d) correlation<br/> with the Winkler method is excellent. Laboratory experiences and data<br/> support these conclusions</p> | <p><b>DO ANALYSIS</b><br/> instrumentation</p>  |
| W-26 | <p>Wurtz, B<br/> <b>EFFECTS OF HEATED DISCHARGES ON AQUATIC LIFE<br/> AND WATER USE</b><br/> ASME—Paper 61-WA-142 for meeting Nov 26-Dec 1 1961<br/> Effects of heated discharges on biological structure of receiving stream; fish<br/> and bottom organisms discussed insofar as they are directly affected by heat;<br/> water uses that are temperature limited, also discussed, as are relationships<br/> between dissolved oxygen and temperature (EI 1962)</p>  | <p><b>BASIC STUDIES</b><br/> streams</p>  |

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discussion of OXYGEN TRANSFER FROM FALLING  
WATER DROPLETS by Charles E. Carver, Jr.  
Proc ASCE v 95 n SA 6 Apr 1969 p 1203-1205
- Y-2 Yotsukura, Nobuhiro Fiering, Myron B  
NUMERICAL SOLUTION TO A DISPERSION EQUATION  
Proc ASCE v 90 n HY 5 Sep 1964 p 83-104

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## Z

- Z-1**    Zierninski, S A    Caron, M M    Blackmore, R B  
**BEHAVIOR OF AIR BUBBLES IN DILUTE AQUEOUS SOLUTIONS**  
 Ind and Eng Chem—Fundamentals v 6 n 2 May 1967 p 233-242  
 Total transfer rate may be profoundly affected by some of investigated substances, e.g., heptanoic acid at concentration of 10 ppm increased rate of oxygen transfer by 180 percent; effects discussed in this report depend on air dispersing system; since principal action of substances appears to be in preventing coalescence of bubbles, their effectiveness will improve in systems where possibility of coalescence is greater; applicability to aeration systems, as used in fermentation processes and in treatment of sewage by bio-oxidation. 24 refs (EI 1967)
- Z-2**    Zierninski, Stefan A    Raymond, Delmar R  
**USE OF CHEMICAL ADDITIVES TO IMPROVE AERATION RATES: STUDY OF THE BEHAVIOR OF SINGLE BUBBLES—PROGRESS REPORT NO. 3a**  
 Federal Water Pollution Control Admin Report R 848-4 Washington D C 1967  
 This report consists of two parts. Part 1 deals with methods of measuring rates of volume change of a rising gas bubble, its surface area, velocity of rise, and the instantaneous mass-transfer coefficient. The principle of this method was discussed in Progress Report No. 2a (1966). However, because of the changes introduced and the reproducibility tests conducted, the method is discussed in this report in detail. Special attention is given to the method of bubble release that proved to be an important factor affecting the consistency of results. Part 2 discusses effects of a homologous series of normal alcohols on mass-transfer and drag coefficients of a carbon dioxide bubble. Carbon dioxide was used in the tests instead of air because of its higher solubility in water permitting greater accuracy of results. It may be expected that similar effects would take place in the case of air bubbles and thus help to better understand and possibly improve aeration systems. The study showed the depressing effect of an alcohol on  $K_L$  increases with its chain length and concentration. A similar consistency of effects was also noticed in the case of drag coefficient which increased with concentration and chain length of the alcohol. 55 refs
- Z-3**    Zierninski, Stefan A    Lessard, Richard R  
**USE OF CHEMICAL ADDITIVES TO IMPROVE AERATION RATES: STUDY OF MODELS OF AIR DISPERSERS—PROGRESS REPORT NO. 3b**  
 Federal Water Pollution Control Admin Report R 848-4 Washington D C 1967  
 The investigation presented in this report deals with a method for improving the rates of aeration. In order to achieve this objective small quantities of some organic substances are introduced in the zone of bubble formation. These additives decrease bubble coalescence and improve the rate of transfer because of the substantial increase in the interfacial surface area. The tests were conducted with n-octanol, 4-methyl-2-pentanol and heptanoic acid. At a concentration of 1 ppm the n-octanol and 4-methyl-2-pentanol showed an improvement in the rate of aeration of 70 percent over that in pure water. At a concentration of only 0.5 ppm n-octanol gave an improvement in the rate of transfer of 30 percent. Since the design of the aerator and the agent were not optimized, it may be expected that still better effect could be obtained in a large-scale installation. Federal Water Pollution Control Administration Grant WP-00562-04. 36 refs

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 experimental

**BASIC STUDIES**  
 bubbles  
 experimental  
 reaeration

**BASIC STUDIES**  
 bubbles  
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 reaeration

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- Z-4 Zieminski, S A Raymond, D R  
EXPERIMENTAL STUDY OF BEHAVIOR OF SINGLE BUBBLES  
Chem Eng Sci v 23 n 1 Jan 1968 p 17-28  
Method is described for measurements of rates of volume change of rising gas bubble, its surface area, velocity of rise, and instantaneous mass-transfer coefficient; principle of this method is to follow, by means of high-speed photography, motion of bubble simultaneously with changes in volume as indicated by capillary of dilatometer; in this way almost continuous record is obtained of bubble volume, shape, and oscillation, as related to height of bubble in liquid and time elapsed from moment of bubble release; relevant to operation of air lifts, mammoth pumps, and sulfur pumping in Frasch process. 31 refs (EI 1968)  
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- Z-5 Zhavoronkov, N M Romankov, P G  
OSNOVNYE NAPRAVLENIYA NAUCHNYKH ISSLEDOVANIY V  
OBLASTI MASSOObMENNYKH PROTESSOV KHIMICHESKOY  
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Khimicheskaya Promyshlennost n 2 Feb 1965 p 1-4  
Main trends in scientific research of mass-exchange processes in chemical technology; present state and future program of research concerned with studies of theoretical problems of physicochemical hydrodynamics and mass exchange; phase equilibria and constants in systems gas-liquid, vapor-liquid, and liquid-liquid, particularly in nonideal and multicomponent systems; calculations of basic processes of mass exchange; mathematical modeling and descriptions of technology of mass-exchange processes. In Russian (EI 1966)  
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# CONVERSION FACTORS--BRITISH TO METRIC UNITS OF MEASUREMENT

The following conversion factors adopted by the Bureau of Reclamation are those published by the American Society for Testing and Materials (ASTM Metric Practice Guide, E 380-68) except that additional factors (\*) commonly used in the Bureau have been added. Further discussion of definitions of quantities and units is given in the ASTM Metric Practice Guide.

The metric units and conversion factors adopted by the ASTM are based on the "International System of Units" (designated SI for Systeme International d'Unites), fixed by the International Committee for Weights and Measures; this system is also known as the Giorgi or MKSA (meter-kilogram (mass)-second-ampere) system. This system has been adopted by the International Organization for Standardization in ISO Recommendation R-31.

The metric technical unit of force is the kilogram-force; this is the force which, when applied to a body having a mass of 1 kg, gives it an acceleration of 9.80665 m/sec/sec, the standard acceleration of free fall toward the earth's center for sea level at 45 deg latitude. The metric unit of force in SI units is the newton (N), which is defined as that force which, when applied to a body having a mass of 1 kg, gives it an acceleration of 1 m/sec/sec. These units must be distinguished from the (inconstant) local weight of a body having a mass of 1 kg; that is, the weight of a body is that force with which a body is attracted to the earth and is equal to the mass of a body multiplied by the acceleration due to gravity. However, because it is general practice to use "pound" rather than the technically correct term "pound-force," the term "kilogram" (or derived mass unit) has been used in this guide instead of "kilogram-force" in expressing the conversion factors for forces. The newton unit of force will find increasing use, and is essential in SI units.

Where approximate or nominal English units are used to express a value or range of values, the converted metric units in parentheses are also approximate or nominal. Where precise English units are used, the converted metric units are expressed as equally significant values.

Table I

## QUANTITIES AND UNITS OF SPACE

Multiply	By	To obtain
<b>LENGTH</b>		
Mil. . . . .	25.4 (exactly). . . . .	Micron
Inches . . . . .	25.4 (exactly). . . . .	Millimeters
. . . . .	2.54 (exactly)*. . . . .	Centimeters
Feet . . . . .	30.48 (exactly). . . . .	Centimeters
. . . . .	0.3048 (exactly)*. . . . .	Meters
. . . . .	0.0003048 (exactly)*. . . . .	Kilometers
Yards . . . . .	0.9144 (exactly). . . . .	Meters
Miles (statute). . . . .	1,609.344 (exactly)*. . . . .	Meters
. . . . .	1.609344 (exactly). . . . .	Kilometers
<b>AREA</b>		
Square inches . . . . .	6.4516 (exactly). . . . .	Square centimeters
Square feet . . . . .	929.03*. . . . .	Square centimeters
. . . . .	0.092903 . . . . .	Square meters
Square yards . . . . .	0.836127 . . . . .	Square meters
Acres . . . . .	0.40469*. . . . .	Hectares
. . . . .	4,046.9*. . . . .	Square meters
. . . . .	0.0040469*. . . . .	Square kilometers
Square miles . . . . .	2.58999. . . . .	Square kilometers
<b>VOLUME</b>		
Cubic inches . . . . .	16.3871 . . . . .	Cubic centimeters
Cubic feet . . . . .	0.0283168. . . . .	Cubic meters
Cubic yards. . . . .	0.764555 . . . . .	Cubic meters
<b>CAPACITY</b>		
Fluid ounces (U.S.) . . . . .	29.5737 . . . . .	Cubic centimeters
. . . . .	29.5729 . . . . .	Milliliters
Liquid pints (U.S.) . . . . .	0.473179 . . . . .	Cubic decimeters
. . . . .	0.473166 . . . . .	Liters
Quarts (U.S.) . . . . .	946.358*. . . . .	Cubic centimeters
. . . . .	0.946331*. . . . .	Liters
Gallons (U.S.) . . . . .	3,785.43*. . . . .	Cubic centimeters
. . . . .	3.78543. . . . .	Cubic decimeters
. . . . .	3.78533. . . . .	Liters
. . . . .	0.00378543*. . . . .	Cubic meters
Gallons (U.K.) . . . . .	4.54609 . . . . .	Cubic decimeters
. . . . .	4.54596 . . . . .	Liters
Cubic feet. . . . .	28.3160 . . . . .	Liters
Cubic yards. . . . .	764.55*. . . . .	Liters
Acre-feet. . . . .	1,233.5*. . . . .	Cubic meters
. . . . .	1,233,500*. . . . .	Liters

Table II  
QUANTITIES AND UNITS OF MECHANICS

Multiply	By	To obtain
<b>MASS</b>		
Grains (1/7,000 lb) . . . . .	64.79891 (exactly) . . . . .	Milligrams
Troy ounces (480 grains). . . . .	31.1035 . . . . .	Grams
Ounces (avdp). . . . .	28.3495 . . . . .	Grams
Pounds (avdp). . . . .	0.45359237 (exactly). . . . .	Kilograms
Short tons (2,000 lb). . . . .	907.185 . . . . .	Kilograms
Long tons (2,240 lb). . . . .	0.907185 . . . . .	Metric tons
	1,016.05 . . . . .	Kilograms
<b>FORCE/AREA</b>		
Pounds per square inch . . . . .	0.070307 . . . . .	Kilograms per square centimeter
	0.689476 . . . . .	Newtons per square centimeter
Pounds per square foot . . . . .	4.88243 . . . . .	Kilograms per square meter
	47.8803 . . . . .	Newtons per square meter
<b>MASS/VOLUME (DENSITY)</b>		
Ounces per cubic inch . . . . .	1.72999 . . . . .	Grams per cubic centimeter
Pounds per cubic foot . . . . .	16.0135 . . . . .	Kilograms per cubic meter
	0.0160185 . . . . .	Grams per cubic centimeter
Tons (long) per cubic yard . . . . .	1.32894 . . . . .	Grams per cubic centimeter
<b>MASS/CAPACITY</b>		
Ounces per gallon (U.S.) . . . . .	7.4893 . . . . .	Grams per liter
Ounces per gallon (U.K.) . . . . .	6.2362 . . . . .	Grams per liter
Pounds per gallon (U.S.) . . . . .	119.829 . . . . .	Grams per liter
Pounds per gallon (U.K.) . . . . .	99.779 . . . . .	Grams per liter
<b>BENDING MOMENT OR TORQUE</b>		
Inch-pounds . . . . .	0.011521 . . . . .	Meter-kilograms
	1.12985 x 10 <sup>6</sup> . . . . .	Centimeter-dynes
Foot-pounds . . . . .	0.138255 . . . . .	Meter-kilograms
	1.35582 x 10 <sup>7</sup> . . . . .	Centimeter-dynes
Foot-pounds per inch . . . . .	5.4431 . . . . .	Centimeter-kilograms per centimeter
Ounce-inches . . . . .	72.008 . . . . .	Gram-centimeters
<b>VELOCITY</b>		
Feet per second. . . . .	30.48 (exactly). . . . .	Centimeters per second
	0.3048 (exactly)* . . . . .	Meters per second
Feet per year. . . . .	0.965873 x 10 <sup>-8</sup> * . . . . .	Centimeters per second
Miles per hour . . . . .	1.609344 (exactly). . . . .	Kilometers per hour
	0.44704 (exactly) . . . . .	Meters per second
<b>ACCELERATION*</b>		
Feet per second <sup>2</sup> . . . . .	0.3048* . . . . .	Meters per second <sup>2</sup>
<b>FLOW</b>		
Cubic feet per second (second-foot)	0.028317* . . . . .	Cubic meters per second
Cubic feet per minute . . . . .	0.4719 . . . . .	Liters per second
Gallons (U.S.) per minute . . . . .	0.06309 . . . . .	Liters per second
<b>FORCE*</b>		
Pounds. . . . .	0.453592* . . . . .	Kilograms
	4.4482* . . . . .	Newtons
	4.4482 x 10 <sup>-5</sup> * . . . . .	Dynes

Multiply	By	To obtain
<b>WORK AND ENERGY*</b>		
British thermal units (Btu). . . . .	0.252* . . . . .	Kilogram calories
	1,055.08 . . . . .	Joules
Btu per pound. . . . .	2.326 (exactly) . . . . .	Joules per gram
Foot-pounds . . . . .	1.35582* . . . . .	Joules
<b>POWER</b>		
Horsepower . . . . .	745.700 . . . . .	Watts
Btu per hour . . . . .	0.293071 . . . . .	Watts
Foot-pounds per second . . . . .	1.35582 . . . . .	Watts
<b>HEAT TRANSFER</b>		
Btu in./hr ft <sup>2</sup> deg F (k, thermal conductivity) . . . . .	1.442 . . . . .	Milliwatts/cm deg C
	0.1240 . . . . .	Kg cal/hr m deg C
Btu ft/hr ft <sup>2</sup> deg F . . . . .	1.4880* . . . . .	Kg cal m/hr m <sup>2</sup> deg C
Btu/hr ft <sup>2</sup> deg F (C, thermal conductance) . . . . .	0.568 . . . . .	Milliwatts/cm <sup>2</sup> deg C
	4.882 . . . . .	Kg cal/hr m <sup>2</sup> deg C
Deg F hr ft <sup>2</sup> /Btu (R, thermal resistance) . . . . .	1.761 . . . . .	Deg C cm <sup>2</sup> /milliwatt
Btu/lb deg F (c, heat capacity) . . . . .	4.1868 . . . . .	J/g deg C
Btu/lb deg F . . . . .	1.000* . . . . .	Cal/gram deg C
Ft <sup>2</sup> /hr (thermal diffusivity) . . . . .	0.2581 . . . . .	Cm <sup>2</sup> /sec
	0.09290* . . . . .	M <sup>2</sup> /hr
<b>WATER VAPOR TRANSMISSION</b>		
Grains/hr ft <sup>2</sup> (water vapor transmission) . . . . .	18.7 . . . . .	Grams/24 hr m <sup>2</sup>
Perms (permeance) . . . . .	0.859 . . . . .	Metric perms
Perm-inches (permeability) . . . . .	1.67 . . . . .	Metric perm-centimeters

Table III  
OTHER QUANTITIES AND UNITS

Multiply	By	To obtain
Cubic feet per square foot per day (seepage) . . . . .	304.8* . . . . .	Liters per square meter per day
Pound-seconds per square foot (viscosity) . . . . .	4.8824* . . . . .	Kilogram second per square meter
Square feet per second (viscosity). . . . .	0.092903* . . . . .	Square meters per second
Fahrenheit degrees (change)*. . . . .	5/9 exactly . . . . .	Celsius or Kelvin degrees (change)*
Volts per mil. . . . .	0.03937 . . . . .	Kilovolts per millimeter
Lumens per square foot (foot-candles) . . . . .	10.764 . . . . .	Lumens per square meter
Ohm-circular mils per foot . . . . .	0.001682 . . . . .	Ohm-square millimeters per meter
Milliampes per cubic foot . . . . .	35.3147* . . . . .	Milliampes per cubic meter
Milliamps per square foot . . . . .	10.7639* . . . . .	Milliamps per square meter
Gallons per square yard . . . . .	4.527219* . . . . .	Liters per square meter
Pounds per inch. . . . .	0.17858* . . . . .	Kilograms per centimeter

## ABSTRACT

Bureau of Reclamation responsibility for maintaining or enhancing the water quality associated with its projects has resulted in a comprehensive program of research in water quality and pollution control. A literature search and state-of-the-art review to determine the need for future research in reeration of streams and reservoirs revealed a large number of references concerning the application of aeration methods and equipment to waste treatment. Generally, the application of this technology to aeration of large volumes of water such as rivers and reservoirs remains to be developed, although several applicable references were found. Questions regarding atmospheric reaeration in streams remain unresolved. Research is also needed regarding the aeration capability of hydraulic structures and control devices, development of new methods and equipment, effects of dissolved air on cavitation, and comparative economics of various methods and equipment. Ecological effects of reaeration are being considered in a separate review.

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Bur Reclam Rep REC-OCE-70-55, Div Gen Res, Dec 1970. Bureau of Reclamation, Denver, 131 p, 2 fig, 7 tab, 448 ref

DESCRIPTORS--/ \*aeration/ \*streams/ \*reservoirs/ instrumentation/ oxygen sag/ mathematical analysis/ theory/ mass transfer/ equipment/ \*dissolved oxygen/ methodology/ industrial waste treatment/ sewage treatment/ water quality/ efficiencies/ economics/ \*bibliographies/ \*reviews/ cavitation/ biochemical oxygen demand/ \*reaeration/ oxygen requirements

IDENTIFIERS--/ cavitation control/ oxygen exchange/ empirical equations/ formulas

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